

(b) Specific Restrictions:

(1) Participation and cooperation **MUST NOT** directly or indirectly endorse, or selectively benefit, or favor, or appear to endorse, or selectively benefit, or favor any private individual, group, corporation (whether for profit or nonprofit), sect, quasireligious or ideological movement, fraternal organization, political organization, or commercial venture, or be associated with the solicitation of votes in a political election.

(2) Participation may not help commercial advertising, publicity or promotional activities, nor events that help or favor a commercial venture.

§ 837.14 Reimbursement for support.

(a) News media do not pay for Air Force stock AV material or location photography on Air Force facilities, when used for news projects.

(b) Other AV producers must pay standard research fees and all other costs of Air Force stock AV materials. This includes materials wanted for documentaries that are not regarded as news materials under a above.

(c) Assistance to nongovernment enterprises whose productions have potential positive benefit to the Air Force should be charged at the DOD-user rate. Other productions should pay the nongovernment user or government (non-DOD) user rate. Office of the Assistant Secretary of Defense, Public Affairs Office (OASD/PA) and SAF/PA determine the rate to be charged.

(d) The Air Force organization that owns the resources expended or equipment involved should present its bill or bills to the production company through the SAF/PA project officer.

§ 837.15 Pay for Air Force people.

Air Force people who appear in non-news AV productions must do so voluntarily whether on duty or off duty.

(a) If they are performing normal duties, during the time of the AV production, the people are said to be on-duty and cannot be paid by the producer, but they are not required to participate.

(b) If they are not performing normal duties, while taking part in a production they are off-duty. They then may negotiate with the producer for pay for their services.

(c) The producer bears the travel and per diem costs for Air Force people involved in nongovernment AV productions, whether on duty or off. The producer may handle this directly with the people, or the parent unit may bill the producer at prevailing military or government civilian rates. The bill must be sent to the producer through the Air

Force unit project officer, with a copy to SAF/PAMB.

Winnibel F. Holmes,

Air Force Federal Register Liaison Officer.

[FR Doc. 82-21307 Filed 8-5-82; 8:45 am]

BILLING CODE 3910-01-M

DEPARTMENT OF THE INTERIOR**National Park Service****36 CFR Part 50****National Capital Parks Regulations; Camping; Correction**

AGENCY: National Park Service, Interior.

ACTION: Final rule; correction.

SUMMARY: This document corrects the authority citation for Part 50 of 36 Code of Federal Regulations contained in final regulations specifying the types of activities considered by the National Park Service to be camping which must be confined to designated camping areas. The final regulations were published on June 4, 1982 (47 FR 24299) and the authority citation was found at page 24302 of that publication.

FOR FURTHER INFORMATION CONTACT:

Sandra Alley, Associate Regional Director, Public Affairs, National Capital Region, National Park Service, 1100 Ohio Drive, SW., Washington, D.C. 20242, telephone: 202-426-6700; Richard G. Robbins, Assistant Solicitor, National Capital Parks, Office of the Solicitor, Department of the Interior, Washington, D.C. 20240, telephone: 202-343-4338.

Date approved: July 26, 1982.

Craig Potter,

Deputy Assistant Secretary for Fish and Wildlife and Parks.

PART 50—NATIONAL CAPITAL PARKS REGULATIONS

Accordingly, the National Park Service is correcting the authority citation for Part 50 to read as follows:

Authority: Sec. 6 of the Act of July 1, 1898 (30 Stat. 571); Sections 1-3 of the Act of August 25, 1916 (39 Stat. 535, as amended); Section 16 of the Act of March 3, 1925 (43 Stat. 1128, as amended); Act of March 17, 1948 (62 Stat. 81); Act of August 8, 1953 (67 Stat. 495); 16 U.S.C. 1-3; D.C. Code 8-137 (1981); D.C. Code 40-721 (1981).

[FR Doc. 82-21350 Filed 8-5-82; 8:45 am]

BILLING CODE 4310-70-M

ENVIRONMENTAL PROTECTION AGENCY**40 CFR Part 60**

[AD-FRL 1982-8(a)]

Standards of Performance for New Stationary Sources, Asphalt Processing, and Asphalt Roofing Manufacture

AGENCY: Environmental Protection Agency (EPA).

ACTION: Final rule.

SUMMARY: Proposed standards of performance for asphalt processing and asphalt roofing manufacture were published in the *Federal Register* on November 18, 1980 (45 FR 76404) and amended on May 26, 1981 (46 FR 28180). These standards implement Section III of the Clean Air Act and are based on the Administrator's determination that asphalt processing and asphalt roofing manufacture cause or contribute significantly to air pollution which may reasonably be anticipated to endanger public health or welfare. The intended effect is to require all new, modified, and reconstructed asphalt processing and asphalt roofing manufacturing facilities to use the best demonstrated system of continuous emission reduction considering costs, nonair quality health and environmental impacts, and energy requirements.

EFFECTIVE DATE: August 6, 1982.

Under Section 307(b)(1) of the Clean Air Act, judicial review of this new source performance standard is available only by the filing of a petition for review in the U.S. Court of Appeals for the District of Columbia Circuit within 60 days of today's publication of this rule. Under Section 307(b)(2) of the Clean Air Act, the requirements that are the subject of today's notice may not be challenged later in civil or criminal proceedings brought by EPA to enforce these requirements.

ADDRESSES:

Background Information Document. The background information document (BID) for the promulgated standards may be obtained from the U.S. EPA Library (MD-35), Research Triangle Park, North Carolina 27711, telephone number (919) 541-2777. Please refer to "Asphalt Roofing Manufacturing Industry, Background Information for Promulgated Standards of Performance," EPA-450/3-80-021b.

Docket. Docket No. A-79-39, containing information considered by EPA in the development of the promulgated standards, is available for public inspection between 8:00 a.m. and

4:00 p.m., Monday through Friday, at EPA's Central Docket Section (A-130), West Tower Lobby, Gallery 1, Waterside Mall, 401 M Street, SW., Washington, D.C. 20460.

FOR FURTHER INFORMATION CONTACT:

Ms. Susan R. Wyatt, Emission Standards and Engineering Division (MD-13), Environmental Protection Agency, Research Triangle Park, North Carolina 27711, telephone (919) 541-5578.

SUPPLEMENTARY INFORMATION:

The Standards

Standards of performance for new stationary sources established under Section III of the Clean Air Act reflect:

* * * application of the best technological system of continuous emission reduction (taking into consideration the cost of achieving such emission reduction, and any nonair quality health and environmental impacts, and energy requirements) the Administrator determines has been adequately demonstrated. [Section 111(a)(1)]

For convenience, this will be referred to as "best demonstrated technology" or "BDT."

The standards limit particulate emissions from the following newly constructed, modified, or reconstructed facilities: asphalt storage tanks, blowing stills, saturators, and mineral handling and storage areas in asphalt roofing plants; and asphalt storage tanks and blowing stills in asphalt processing plants and petroleum refineries.

Blowing still particulate emissions when firing natural gas or No. 2 fuel oil in the afterburner are limited to 0.60 kg/Mg (1.20 lb/ton) of asphalt charged during conventional blowing and 0.67 kg/Mg (1.34 lb/ton) of asphalt charged during catalytic blowing. When No. 6 fuel oil is used to fire the afterburner, the particulate emissions from blowing stills are limited to 0.64 kg/Mg (1.28 lb/ton) of asphalt charged for conventional blowing and 0.71 kg/Mg (1.42 lb/ton) of asphalt charged for catalytic blowing. Saturator particulate emissions are limited to 0.04 kg/Mg (0.08 lb/ton) of shingle and mineral-surfaced roll roofing produced or to 0.4 kg/Mg (0.8 lb/ton) of saturated felt and smooth-surfaced roll roofing produced, depending on the product.

An opacity standard is being promulgated for each affected facility as follows: 20 percent for saturators; zero percent for asphalt storage tanks except for one consecutive 15-minute period in any 24-hour period when the transfer lines are being blown for clearing; 1 percent for mineral handling and storage areas; and 0 percent for blowing stills, unless an opacity greater than 0 percent is established by the Administrator for

an individual blowing still that is using fuel oil to fire the afterburner used as the control device. A fugitive emission standard of no visible emissions 80 percent of the time is being promulgated for capture systems on newly constructed and reconstructed saturators. Saturators that become subject to the standards through modification are exempt from the visible emissions standard.

The performance test methods for determining compliance with the promulgated standards would be Reference Method 5A (proposed as Method 26) for particulate emissions and Reference Method 22 for fugitive emissions. Reference Method 9 is to be used to determine opacity.

Continuous monitoring of the operating temperature of the control devices used for blowing stills and saturators would be required to ensure proper operation and maintenance.

Summary of Environmental, Energy, and Economic Impacts

It is projected that growth in the industry during the 5 years after proposal (November 18, 1980) of the standards will be: 5 new medium-size plants; 5 small-size plants upgraded to medium-size plants by the addition of a roofing line; 5 plants with reconstructed saturators to replace saturators destroyed by fire; and 20 plants with saturators modified to increase production by 20 percent.

The fifth-year nationwide reduction in particulate emissions beyond the State implementation plan (SIP) level would be 2,040 Mg/yr (2,250 tons/yr). The annual percentage reduction in particulate emissions from the SIP level would be 65 percent.

The amount of wastewater to be treated in the fifth year would be increased by about 235 m³/yr (62,000 gal/yr). The quality of the wastewater would not be changed.

A medium-size model plant (2,060,000 roofing squares/yr) subject to SIP control would consume 6,400 m³/yr (40,250 bbl/yr) of oil. A medium-size model plant subject to new source performance standards (NSPS) control would consume 6,600 m³/yr (41,500 bbl/yr) of oil. This is an increase in oil consumption of 200 m³/yr (1,250 bbl/yr). The fifth-year nationwide increase in energy usage over baseline would be 1,530 m³/yr (9,600 bbl/yr) of oil. The percentage increase from baseline would be 3.2 percent.

The initial capital cost for control devices for a medium-size model plant to comply with the NSPS would be \$100,000 above the cost to comply with SIP's, and the annualized costs would be

\$60,000. The nationwide cumulative capital costs from November 1980 through November 1985 would be \$1,300,000, and the annualized cost would be \$620,000. These costs could increase the product price of asphalt shingles by 0.12 percent. If the product price is not increased, the reduction in net profit would be about 0.3 percent. The costs associated with the standard are not expected to inhibit industry growth.

The environmental, energy, and economic impacts are discussed in greater detail in the background information document for the promulgated standards, "Asphalt Roofing Manufacturing Industry, Background Information for Promulgated Standards of Performance," EPA 450/3-80-021b.

Public Participation

Prior to proposal of the standards, interested parties were advised by public notice in the *Federal Register* (44 FR 65670) of a meeting of the National Air Pollution Control Techniques Advisory Committee to discuss the asphalt processing and asphalt roofing manufacture standard recommended for proposal. This meeting was held on December 12, 1979. The meeting was open to the public, and each attendee was given an opportunity to comment on the standards recommended for proposal. The standards were proposed and published in the *Federal Register* on November 18, 1980 (45 FR 76404). The preamble to the proposed standards discussed the availability of the background information document (BID), "Asphalt Roofing Manufacturing Industry Background Information for Proposed Standards," EPA 450-3-80-021a. The regulatory alternatives considered and the impacts of those alternatives are described in detail in the BID. The opportunity for a public hearing was provided at the time of proposal. Since no requests for a hearing were received, a public hearing was not held. Public comments were solicited at the time of proposal; and, when requested, copies of the BID were distributed to interested parties. The public comment period was from November 18, 1980, to January 19, 1981. Eighteen comment letters were received concerning issues relative to the proposed standards of performance for the asphalt processing and asphalt roofing manufacture industry. On May 26, 1981, an amendment to the proposed standards was published in the *Federal Register* (46 FR 28180). This amendment clarified that the proposed standards applied to asphalt blowing stills and

asphalt storage tanks used for roofing and/or nonroofing asphalts located at asphalt processing plants, petroleum refineries, and asphalt roofing plants. Public comments were solicited on the proposed amendment at that time. The public comment period was from May 26, 1981, to July 10, 1981. Three comment letters were received. The comments have been carefully considered and, where determined by the Administrator to be appropriate, changes have been made to the proposed standards.

Significant Comments and Changes to the Proposed Standards

Comments on the proposed standards were received from the following: asphalt roofing manufacturers; petroleum refiners; trade associations; State and Federal government offices; one consultant to the petroleum refining industry; and one individual. A detailed discussion of these comments and responses can be found in the BID that is referred to in the ADDRESSES section of this preamble. The summary of comments and responses in the BID serves as the basis for the revisions which have been made to the standards since proposal. The major and/or most frequent comments and responses are summarized in this preamble. Most major comments are discussed in the following sections: Opacity Standard for Stills, Monitoring Requirements, Applicability of the Standard to Asphalt Storage Tanks, Storage Tank Opacity Limit, and Reference Test Method 5A.

Opacity Standards for Stills

Several commenters stated that the zero opacity limit for stills might not be attainable if the afterburner were fired with fuel oil instead of natural gas. The tested afterburner was fired with natural gas during the emission and opacity test program. It is EPA's judgment that the zero opacity limit is achievable when fuel oil is used to fire an afterburner. However, the Administrator agrees that there may be a chance that the opacity would exceed zero when fuel oil is used. Therefore, § 60.474(k) has been added and describes the procedures that an owner or operator may follow, in accordance with § 60.11(e) of the General Provisions, to petition the Administrator to establish an opacity standard for a blowing still that will be the opacity standard when fuel oil is used to fire the afterburner. If the owner or operator does not elect to follow the prescribed procedure for establishing the opacity limit, the opacity limit when fuel oil is used will be 0 percent, the same as the limit when natural gas is used to fire the afterburner.

Several commenters stated that the opacity standard for stills forced them to use afterburners as the only control device for blowing stills. EPA has stated that any control device that meets the standard may be used. If the control device meets the particulate emission limit during a performance test but does not meet the opacity limit, the operator may petition the Administrator under § 60.11(e) of the General Provisions for an adjustment to the opacity standard for that affected facility.

Monitoring Requirements

Several commenters stated that the requirements to record continuously the operating temperature, maintain the temperature records for 2 years, and report excess emissions quarterly would make excessive demands on personnel or would require additional personnel.

The recordkeeping and reporting requirements were reviewed to determine if their purpose (ensuring proper operation and maintenance of the control device) could be achieved with fewer recordkeeping and/or reporting requirements. The temperature of the control device would be recorded automatically by an instrument onto a permanent, hard copy record. Such automatic recording and subsequent storage for 2 years should not place an excessive demand on personnel, so the recordkeeping requirements are not being changed. Without this requirement, the owner/operator and the enforcement agency would have difficulty determining if the control device were being properly operated and maintained.

The records of constant temperature monitoring, together with the opacity standards being promulgated, should provide enforcement agencies with sufficient means of ensuring that the control devices are properly maintained and operated on a continuous basis without the necessity for quarterly reports. Therefore, in an effort to reduce reporting costs, the Administrator removed the requirement for quarterly reports from the regulation.

Several commenters suggested that constant temperature monitoring "would not be of value" to the enforcement agency in determining if the emission standard had been met or if excess emissions had occurred since temperature was only one of several parameters that determine emissions.

The constant temperature monitoring requirement is based on Section 302(1) of the Clean Air Act which provides:

The term "standard of performance" means a requirement of continuous emission reduction, including any requirement relating to the operation or maintenance of a source

to assure continuous emission reduction. [Emphasis added.]

EPA believes that changes in temperature from those measured during a performance test are good indicators for an owner/operator and an enforcement agency to use to verify good operation and maintenance. Exceeding the temperature measured during the performance test for an HVAF or ESP or not maintaining at least the temperature measured during the performance test for an afterburner could indicate a violation of the requirement to operate and maintain properly the control equipment, as stated in § 60.11(d) of the General Provisions. This section states:

At all times, including periods of startup, shutdown, and malfunction, owners and operators shall to the extent practicable, maintain and operate any affected facility including associated air pollution control equipment in a manner consistent with good air pollution practice for minimizing emissions. Determination of whether acceptable operating and maintenance procedures are being used will be based on information available to the Administrator, which may include, but is not limited to, monitoring results, opacity observations, review of operating and maintenance procedures, and inspection of the source.

Although periods of temperature excursions or reductions (depending on the control device) as determined by temperature measurements would not, of themselves, constitute a violation of the numerical emission limits, they may indicate to an enforcement agency the need to conduct a performance test. The results of the performance test would be used to determine compliance with the numerical emission limits, in accordance with § 60.11(a) of the General Provisions.

EPA acknowledges that the operating temperature of the control device is one of several parameters that determine the amount of particulate emitted and that the correlation between operating temperature and emissions is not absolute. However, it would be burdensome for the owner or operator to keep records of all parameters that influence emissions and then enter values for these parameters into a formula in order to calculate emissions. Instead, EPA believes that the best way to demonstrate proper operation and maintenance is to monitor only temperature, which is critical to the destruction or collection of particulate hydrocarbons.

For afterburners, temperature, hydrocarbon concentration, and exposure time at temperature all influence destruction efficiency. The

emission data collected during the testing program (BID Volume 1 Chapter 4) and other data (Docket No. A-79-39-II-I-025) used in the analyses show that if the residence time is constant, the afterburner operating temperature is critical to the efficiency of hydrocarbon destruction. For HVAF's and ESP's, the collection efficiency increases as the operating temperature decreases (BID Volume 1 Chapter 4).

Applicability of the Standards to Asphalt Storage Tanks

Commenters questioned the applicability of the standards to asphalt storage tanks containing emulsified asphalt, cutback asphalt, or paving asphalt. The commenters stated that the physical properties and emission characteristics of emulsified asphalt, cutback asphalt, and paving asphalt differ from those of roofing asphalt and should, therefore, be excluded from the standards. The Administrator has determined that storage of cutback asphalts (asphalts mixed with solvents to reduce viscosity and thereby facilitate low temperature applications) and storage of emulsified asphalts (asphalts finely dispersed in water with an emulsifying agent) are excluded from these standards. However, blowing and/or storage of all other asphalts, whether used for roofing, paving, or other nonroofing purposes, are included in the standards. These asphalts are essentially the same as some roofing asphalts and are oxidized or stored in the same type of equipment. If the applicability of the standards depended on the eventual use of the product, a still or storage tank could be subject to the regulation on one day (while blowing or storing roofing asphalt) but not subject to the regulation on another day (while blowing or storing nonroofing asphalt). Even if the same still or storage tank were not used for more than one type of asphalt, there could be one unit devoted to roofing asphalts and subject to the regulation while another identical unit devoted to nonroofing asphalts would not be subject to the regulation. Furthermore, to meet the increased demand for roofing asphalt, a manufacturer could increase capacity by constructing new stills or storage tanks but then limit the use of the new facilities to nonroofing asphalts while devoting a larger number of existing facilities to roofing asphalts, thereby circumventing the emission standard (46 FR 28180).

Since the processes and control technologies are the same whether the asphalt is to be used for roofing or nonroofing purposes, the emission limits remain achievable. Therefore, blowing

stills and storage tanks for paving and other nonroofing asphalts are included in the standards. The definition of "asphalt storage tanks" was changed with the amendment to the proposed standards (46 FR 28180) to specifically exempt cutback and emulsified asphalts.

Storage Tank Opacity Limit

A commenter suggested that the opacity limit on emissions from asphalt storage tanks should be relaxed to permit visible emissions for periods not to exceed 15 minutes in any 24-hour period. This would allow continuation of the necessary industry practice of blowing transfer lines to clear high softening point asphalt from the lines before it solidifies. Often large transfer lines in refineries are thousands of feet long, terminate at remote locations, and must be quickly cleared of asphalt to avoid plugging. At remote locations the only practical method of clearing the line is to blow the line back to the tank using nitrogen or air.

The opacity standard for asphalt storage tanks has been changed to allow the blowing back of the transfer lines. The promulgated standard allows emissions for not more than 15 consecutive minutes in any 24-hour period and states that the control device must not be bypassed during this 15-minute period.

Reference Test Method 5A

During the public comment period following proposal of the standards, several comments were received regarding the proposed Reference Test Method 5A (formerly Method 26). This test method was developed specifically to measure emissions from asphalt processing and asphalt roofing manufacture facilities, since Reference Test Method 5, the EPA method usually used to determine particulate emissions, could not accurately measure asphalt emissions. Several commenters objected that EPA did not attempt to correlate Method 5A results with industry results previously obtained using Method 5. One of these commenters cited test results that indicated Method 5A measurements made at one facility were six times higher than Method 5 measurements made at the same facility. Because of this difference, the commenter was concerned that the standards may not be achievable if measurements were made using Method 5A.

There are two significant differences between Method 5A and Method 5. One difference between the methods is the procedure followed to clean the sampling probe: in Method 5 an acetone rinse is used; in Method 5A a

trichloroethane rinse is used to remove the collected asphalt. A second difference is the temperature of the sampling probe and filter: in Method 5 the probe and filter are maintained at $121 \pm 14^\circ\text{C}$; in Method 5A the probe and filter are maintained at $42 \pm 10^\circ\text{C}$. These two differences could account for a major portion of the differences in test results cited by the commenter.

Test data from Method 5 were not used to establish the emission limits nor to assess the performance of control equipment. The standards are based solely on data from Method 5A. Three control devices, representative of best demonstrated technology, were tested at asphalt roofing plants. The proposed emission limits were set at levels achievable by each of the three control devices, using Method 5A to measure the emissions. If best demonstrated technology is used to control emissions, the standards will be achievable using Method 5A as the compliance test method. A correlation between the results of Method 5 and Method 5A, assuming such a correlation is possible, would not change the achievability of the standards.

A major point made later by one commenter is that Method 5A results vary according to the temperature of the sampling filter: the higher the filter temperature, the lower the test results. This commenter used Method 5A to measure emissions from a saturator. A series of twelve individual test runs was conducted over a 16.6°C temperature range. The commenter then compared the results of two individual runs that were collected simultaneously, one at a filter temperature of 39.4°C and the other at a filter temperature of 51.1°C . The results were 0.024 kg/Mg and 0.010 kg/Mg , respectively. The commenter believes the 0.014 kg/Mg difference, due to filter temperature (as the only variable), indicates that Method 5A results are unreliable.

The Agency acknowledges that Method 5A test results vary according to sampling filter temperature. The reason is because Method 5A measures condensed hydrocarbons, and whether or not the hydrocarbons are in the condensed form is a function of temperature. The temperature dependence is related to the physical properties of the hydrocarbons being measured rather than to the test method. Asphalt emissions consist of tars, oils, and other hydrocarbons. Whether these materials are in the particulate (liquid) or gaseous state is a function of temperature. Because of this temperature dependence, emission control can be achieved by cooling the

emissions to form particulates and then removing the particulates by means of control devices such as electrostatic precipitators, scrubbers, or filters. Without this cooling and subsequent removal, the gaseous hydrocarbons would be emitted to the atmosphere where they would condense, at air temperatures, to form particulates. Better control of these condensible hydrocarbons is achieved by cooling them to form particulates prior to removal by the control devices.

A compliance test method designed to reflect the performance of the control system must measure condensed emissions and therefore must be conducted at low temperatures. The temperature of the Method 5A sampling train during acquisition of the test data for the proposed standards was maintained over the range of 32°C to 52°C. This allowable range is included in Method 5A to allow for normal variation in sampling temperature without excessive care by the test team. The commenter's data demonstrated that if the temperature of the sampling train is maintained over a narrow range (3.3°C), the measured particulate at a low average sampling temperature will be higher than the measured particulate at a higher average sampling temperature. This result is consistent with the expected change in the physical state (liquid or gas) of the emissions.

The extent of the variability in test results is limited by the inclusion of both a minimum and a maximum sampling temperature in Method 5A. In addition, performance test results are required to be an average of three test runs (§ 60.8(f) of the General Provisions), further reducing the variability of test results. If the commenter had averaged the three individual runs with filter temperatures closest to each of the two temperatures (39.4° and 51.1°C), the results compared would have been 0.017 kg/Mg and 0.008 kg/Mg, a difference of 0.009 kg/Mg. It should be noted that the level of the standard for saturators is 0.04 kg/Mg, a limit well above the commenter's highest test run result of 0.024 kg/Mg.

Other Changes Made to Standard Since Proposal

On May 26, 1981, an amendment to the proposed standard was published (46 FR 28180). This amendment clarified that the blowing and storing of nonroofing asphalts are included in the standard. The amendment added the definitions of asphalt processing plant and asphalt roofing plant, removed the definition of asphalt roofing manufacture, and changed the definitions of asphalt processing and

blowing still so that they were not limited to roofing asphalts.

The definition of saturant blow was removed from the regulation. An explanation of this change is contained in the BID.

Saturators that become subject to the standards as a result of modification have been exempted from the visible emissions standard. At this time there is not enough information available about the cost of retrofitting enclosures for the Agency to be certain that the costs would be reasonable in all cases. Therefore, an exemption from the visible emissions standard for modified saturators was added to the regulation. Existing saturators that become subject to the standards through reconstruction are not exempt from the visible emissions standard, since possible constraints associated with retrofitting the enclosure would not be present with reconstructed saturators.

The number of Method 26 was changed to Method 5A. The proposed version of Method 5A did not specify a minimum temperature or a range of operating temperatures. Because the collection temperature directly affects the amount of particulate collected, the Administrator has decided to specify a range of filter and probe temperatures including an upper and lower limit for operation. The probe and filter operating temperature specifications have been revised to 42°±10°C (108°±18°F). All of the emission tests were performed within this temperature range. The results of EPA's emission tests show that this range of temperatures can be maintained by commercially available source sampling equipment. This specification will minimize the effect of temperature variations during sampling on the amount of particulate collected and will not interfere with the achievability of the standard. Method 5A has been further revised to clarify that the precollector cyclone is not to be used except under specific stack conditions. Use of the glass wool filter has been eliminated as being unnecessary for sampling well controlled sources. Method 22 was changed to require prescribed training of the observer.

Docket

Docket No. A-79-39 is an organized and complete file of all the information considered by EPA in the development of this rulemaking. The docket is a dynamic file, since material is added throughout the rulemaking development. The docketing system is intended to allow members of the public and industries involved to readily identify and locate documents so that they can

effectively participate in the rulemaking process. Along with the statement of basis and purpose of the proposed and promulgated standards and EPA responses to significant comments, the contents of the docket will serve as the record in case of judicial review (except for those portions of the docket excluded from the record under Section 307(d)(7)(A)).

Miscellaneous

The effective date of this regulation is August 6, 1982. Section 111 of the Clean Air Act provides that standards of performance or revisions thereof become effective upon promulgation and apply to any saturator or mineral handling and storage facility that commences construction or modification after November 18, 1980. Any asphalt storage tank or blowing still that processes and/or stores asphalt used for roofing only or for roofing and other purposes, and that commences construction or modification after November 18, 1980, is subject to the requirements of this regulation. Any asphalt storage tank or blowing still that processes and/or stores only nonroofing asphalts and that commences construction or modification after May 26, 1981, is subject to the requirements of this regulation.

As prescribed by Section 111, the promulgation of these standards was preceded by the Administrator's determination (40 CFR 60.16, 44 FR 49222, dated August 21, 1979) that these sources contribute significantly to air pollution which may reasonably be anticipated to endanger public health or welfare. In accordance with Section 117 of the Act, publication of these promulgated standards was preceded by consultation with appropriate advisory committees, independent experts, and Federal departments and agencies.

This regulation will be reviewed 4 years from the date of promulgation as required by the Clean Air Act. This review will include an assessment of such factors as the need for integration with other programs, the existence of alternative methods, enforceability, improvements in emission control technology, and reporting requirements. The reporting requirements in this regulation will be reviewed as required under EPA's sunset policy for reporting requirements in regulations.

Section 317 of the Clean Air Act requires the Administrator to prepare an economic impact assessment for any new source standard of performance promulgated under Section 111(b) of the Act. An economic impact assessment was prepared for this regulation and for

other regulatory alternatives. All aspects of the assessment were considered in the formulation of the standards to ensure that cost was carefully considered in determining BDT. The economic impact assessment is included in the background information document for the proposed standards. The BID contains (1) a summary of all the public comments made on the proposed standards and the Administrator's responses to the comments, (2) a summary of the changes made to the standards since proposal, and (3) the final environmental impact statement, which summarizes the impacts of the standards.

The Paperwork Reduction Act of 1980 (Pub. L. 96-511) requires clearance from the Office of Management and Budget (OMB) of certain public reporting/recordkeeping requirements before certain information requests can be made to the public. The reporting/recordkeeping requirements associated with this standard have been approved by OMB.

"Major Rule" Determination. Under Executive Order 12291, EPA is required to judge whether a regulation is a "major rule" and therefore subject to certain requirements of the Order. The Agency has determined that this regulation would result in none of the adverse economic effects set forth in Section 1 of the Order as grounds for finding a regulation to be a "major rule." Fifth-year annualized costs of the standard would be \$620,000. The product wholesale price could increase about 0.15 percent, which could increase the price for a roof on a typical 3-bedroom house by about \$3.00. If the costs were absorbed, the resulting drop in net profit after taxes could be about 0.3 percent. The Agency has also concluded that this rule is not "major" under either of the other criteria established in the Executive Order. The Agency has therefore concluded that the proposed regulation is not a "major rule" under Executive Order 12291.

This regulation was submitted to the Office of Management and Budget (OMB) for review as required by Executive Order 12291.

Regulatory Flexibility Analysis Certification.

A Regulatory Flexibility Analysis was not required for this regulation, because it was proposed before January 1, 1981. However, an analysis was prepared to ascertain if there would be a significant impact on small business.

Current Small Business Administration (SBA) guidelines stipulate that a small business entity in SIC code 2952, asphalt felts and

coatings, is one that has 750 employees or less.¹ This is the criterion to qualify for SBA loans or for the purpose of Government procurement. Of the 31 companies that comprise the asphalt processing and asphalt roofing industry, 13 might qualify as small entities. These companies could become subject to the new source performance standard by building a new facility or by modifying or reconstructing an existing one.

Current EPA criteria stipulate that a regulatory flexibility analysis must be prepared if 20 percent of the small business entities (two to three asphalt processing or asphalt roofing companies) will suffer "significant impacts."

Growth projections indicate that over the next 5 years, 5 new plants, 5 new roofing lines, and 25 saturators could become subject to the NSPS. Thirteen small entities now own 12 percent of the existing plants. If the growth were evenly distributed among existing companies, the 13 small companies would build one new plant and modify or reconstruct two to three saturators. If this new plant and the three affected saturators were each owned by a different company, the 20 percent criterion would be exceeded.

EPA sought to ascertain whether or not any of these four companies would suffer significant impacts if it became subject to the NSPS. A new plant typical of the small entity sector would be a saturated felt plant with a capacity of 27,000 Mg/yr (30,000 tons/yr). To meet existing State requirements, such a plant would cost \$5,800,000 to build and \$7,900,000 a year to operate.² For an additional \$56,000 in building costs and \$25,000 in annualized costs, the plant could be brought into compliance with the NSPS regulatory requirements.³ This additional cost represents less than 1 percent of investment and less than 0.3 percent of annualized cost. These impacts are not considered significant.

Five saturator reconstructions are anticipated as a result of fires. Of these, one reconstruction could be done by a small entity. To comply with the NSPS would require an additional \$20,300 in capital and \$8,500 in annualized costs.³ This additional expense is not expected to cause a significant impact. However, if it did cause a significant impact and the company could demonstrate that it is not "economically feasible" to comply with the NSPS, the Administrator could exempt the company from the NSPS requirements in accordance with § 60.15(b)(2) of the General Provisions.

One to two small companies may modify the saturator to increase production by 20 percent. If this cannot be done within the maintenance

expenditure guidelines of IRS Bulletin 534, the saturator would become an affected facility under the NSPS. The additional costs for each modified saturator would be, \$20,300 capital and \$8,500 annualized costs. However, the decision to increase capacity is a financial one. If the market for greater capacity exists and the costs to install that capacity can be recaptured at an acceptable rate of return, a company will opt to make the investment. If, on the other hand, there are more attractive investments, the company will probably invest the money elsewhere. The extra cost for NSPS compliance may make the decision to increase capacity less attractive if the costs to comply with NSPS requirements cannot be quickly recaptured. However, the decision by a company not to increase capacity cannot be called a significant impact if that company decides on a more lucrative use for its funds.

In conclusion, the economic impacts on small business are minor for new plants because the incremental capital and annualized costs are relatively small. Significant impacts need not be incurred from reconstruction or modification.

Pursuant to the provisions of 5 U.S.C. Section 605(b), I hereby certify that this promulgated rule will not have a significant economic impact on a substantial number of small entities.

List of Subjects in 40 CFR Part 60

Air pollution control, Aluminum, Ammonium sulfate plants, Cement industry, Coal, Copper, Electric power plants, Glass and glass products, Grains, Intergovernmental relations, Iron, Lead, Metals, Motor vehicles, Nitric acid plants, Paper and paper products industry, Petroleum, Phosphate, Sewage disposal, Steel, Sulfuric acid plants, Waste treatment and disposal, Zinc

Dated: July 19, 1982.

Anne M. Gorsuch,
Administrator.

References

- ¹ 13 CFR 121.3, Schedules A and B.
- ² Docket No. A-79-39-IV-B-003.
- ³ Asphalt Roofing Manufacturing Industry—Background Information for Proposed Standards. EPA 450/3-80-021a. June 1980. pp. 8-88 and 8-104.

PART 60—STANDARDS OF PERFORMANCE FOR NEW STATIONARY SOURCES

Accordingly, 40 CFR Part 60 is amended as follows:

1. By adding Subpart UU as follows:

Subpart UU—Standards of Performance for Asphalt Processing and Asphalt Roofing Manufacture

Sec.

60.470 Applicability and designation of affected facilities.

60.471 Definitions.

60.472 Standards for particulate matter.

60.473 Monitoring of operations.

60.474 Test methods and procedures.

Authority: Sec. 111, 301(a), Clean Air Act, as amended, (42 U.S.C. 7411, 7601(a)), and additional authority as noted below.

Subpart UU—Standards of Performance for Asphalt Processing and Asphalt Roofing Manufacture**§ 60.470 Applicability and designation of affected facilities.**

(a) The affected facilities to which this subpart applies are each saturator and each mineral handling and storage facility at asphalt roofing plants; and each asphalt storage tank and each blowing still at asphalt processing plants, petroleum refineries, and asphalt roofing plants.

(b) Any saturator or mineral handling and storage facility under paragraph (a) of this section that commences construction or modification after November 18, 1980, is subject to the requirements of this subpart. Any asphalt storage tank or blowing still that processes and/or stores asphalt used for roofing only or for roofing and other purposes, and that commences construction or modification after November 18, 1980, is subject to the requirements of this subpart.

Any asphalt storage tank or blowing still that processes and/or stores only nonroofing asphalts and that commences construction or modification after May 26, 1981, is subject to the requirements of this subpart.

§ 60.471 Definitions.

As used in this subpart, all terms not defined herein shall have the meaning given them in the Act and in Subpart A of this part.

"Afterburner (A/B)" means an exhaust gas incinerator used to control emissions of particulate matter.

"Asphalt processing" means the storage and blowing of asphalt.

"Asphalt processing plant" means a plant which blows asphalt for use in the manufacture of asphalt products.

"Asphalt roofing plant" means a plant which produces asphalt roofing products (shingles, roll roofing, siding, or saturated felt).

"Asphalt storage tank" means any tank used to store asphalt at asphalt roofing plants, petroleum refineries, and asphalt processing plants. Storage tanks containing cutback asphalts (asphalts

diluted with solvents to reduce viscosity for low temperature applications) and emulsified asphalts (asphalts dispersed in water with an emulsifying agent) are not subject to this regulation.

"Blowing still" means the equipment in which air is blown through asphalt flux to change the softening point and penetration rate.

"Catalyst" means a substance which, when added to asphalt flux in a blowing still, alters the penetrating-softening point relationship or increases the rate of oxidation of the flux.

"Coating blow" means the process in which air is blown through hot asphalt flux to produce coating asphalt. The coating blow starts when the air is turned on and stops when the air is turned off.

"Electrostatic precipitator (ESP)" means an air pollution control device in which solid or liquid particulates in a gas stream are charged as they pass through an electric field and precipitated on a collection surface.

"High velocity air filter (HVAF)" means an air pollution control filtration device for the removal of sticky, oily, or liquid aerosol particulate matter from exhaust gas streams.

"Mineral handling and storage facility" means the areas in asphalt roofing plants in which minerals are unloaded from a carrier, the conveyor transfer points between the carrier and the storage silos, and the storage silos.

"Saturator" means the equipment in which asphalt is applied to felt to make asphalt roofing products. The term saturator includes the saturator, wet looper, and coater.

§ 60.472 Standards for particulate matter.

(a) On and after the date on which § 60.8(b) requires a performance test to be completed, no owner or operator subject to the provisions of this subpart shall cause to be discharged into the atmosphere from any saturator:

(1) Particulate matter in excess of: (i) 0.04 kilograms of particulate per megagram of asphalt shingle or mineral-surfaced roll roofing produced, or (ii) 0.4 kilograms per megagram of saturated felt or smooth-surfaced roll roofing produced;

(2) Exhaust gases with opacity greater than 20 percent; and

(3) Any visible emissions from a saturator capture system for more than 20 percent of any period of consecutive valid observations totaling 60 minutes. Saturators that were constructed before November 18, 1980, and that have not been reconstructed since that date and that become subject to these standards through modification are exempt from the visible emissions standard.

Saturators that have been newly constructed or reconstructed since November 18, 1980 are subject to the visible emissions standard.

(b) On and after the date on which § 60.8(b) requires a performance test to be completed, no owner or operator subject to the provisions of this subpart shall cause to be discharged into the atmosphere from any blowing still:

(1) Particulate matter in excess of 0.67 kilograms of particulate per megagram of asphalt charged to the still when a catalyst is added to the still; and

(2) Particulate matter in excess of 0.71 kilograms of particulate per megagram of asphalt charged to the still when a catalyst is added to the still and when No. 6 fuel oil is fired in the afterburner; and

(3) Particulate matter in excess of 0.60 kilograms of particulate per megagram of asphalt charged to the still during blowing without a catalyst; and

(4) Particulate matter in excess of 0.64 kilograms of particulate per megagram of asphalt charged to the still during blowing without a catalyst and when No. 6 fuel oil is fired in the afterburner; and

(5) Exhaust gases with an opacity greater than 0 percent unless an opacity limit for the blowing still when fuel oil is used to fire the afterburner has been established by the Administrator in accordance with the procedures in § 60.474(k).

(c) Within 60 days after achieving the maximum production rate at which the affected facility will be operated, but not later than 180 days after initial startup of such facility, no owner or operator subject to the provisions of this subpart shall cause to be discharged into the atmosphere from any asphalt storage tank exhaust gases with opacity greater than 0 percent, except for one consecutive 15-minute period in any 24-hour period when the transfer lines are being blown for clearing. The control device shall not be bypassed during this 15-minute period. If, however, the emissions from any asphalt storage tank(s) are ducted to a control device for a saturator, the combined emissions shall meet the emission limit contained in paragraph (a) of this section during the time the saturator control device is operating. At any other time the asphalt storage tank(s) must meet the opacity limit specified above for storage tanks.

(d) Within 60 days after achieving the maximum production rate at which the affected facility will be operated, but not later than 180 days after initial startup of such facility, no owner or operator subject to the provisions of this subpart shall cause to be discharged

into the atmosphere from any mineral handling and storage facility emissions with opacity greater than 1 percent.

§ 60.473 Monitoring of operations.

(a) The owner or operator subject to the provisions of this subpart, and using either an electrostatic precipitator or a high velocity air filter to meet the emission limit in § 60.472(a)(1) and/or (b)(1) shall continuously monitor and record the temperature of the gas at the inlet of the control device. The temperature monitoring instrument shall have an accuracy of $\pm 15^{\circ}\text{C}$ over its range.

(b) The owner or operator subject to the provisions of this subpart and using an afterburner to meet the emission limit in § 60.472(a)(1) and/or (b)(1) shall continuously monitor and record the temperature in the combustion zone of the afterburner. The monitoring instrument shall have an accuracy of $\pm 10^{\circ}\text{C}$ over its range.

(c) An owner or operator subject to the provisions of this subpart and using a control device not mentioned in paragraphs (a) and (b) of this section shall provide to the Administrator information describing the operation of the control device and the process parameter(s) which would indicate proper operation and maintenance of the device. The Administrator may require continuous monitoring and will determine the process parameters to be monitored.

(d) The industry is exempted from the quarterly reports required under § 60.7(c). The owner/operator is required to record and report the operating temperature of the control device during the performance test and, as required by § 60.7(d), maintain a file of the temperature monitoring results for at least two years.

(Sec. 114, Clean Air Act as amended (42 U.S.C. 7414))

§ 60.474 Test methods and procedures.

(a) Reference methods in Appendix A of this part, except as provided in § 60.8(b), shall be used to determine compliance with the standards prescribed in § 60.472 as follows:

(1) Method 5A for the concentration of particulate matter.

(2) Method 1 for sample and velocity traverses;

(3) Method 2 for velocity and volumetric flow rate;

(4) Method 3 for gas analysis; and

(5) Method 9 for opacity.

(b) The Administrator will determine compliance with the standards prescribed in § 60.472(a)(3) by using Method 22, modified so that readings are recorded every 15 seconds for a period

of consecutive observations during representative conditions (in accordance with § 60.8(c) of the General Provisions) totaling 60 minutes. A performance test shall consist of one run.

(c) For Method 5A the sampling time for each run on a saturator shall be at least 120 minutes, and the sampling volume shall be at least 3 dscm. Method 5A shall be used to measure the emissions from the saturator while 106.6-kg (235-lb) asphalt shingle is being produced if the final product is shingle or mineral-surfaced roll roofing or while 6.8-kg (15-lb) saturated felt is being produced if the final product is saturated felt or smooth-surfaced roll roofing. If the saturator produces only fiberglass shingles, Method 5A shall be used to measure saturator emissions while a nominal 100-kg (220-lb) shingle is being produced. Method 5A shall be used to measure emissions from the blowing still for at least 90 minutes or for the duration of the coating blow, whichever is greater. If the blowing still is not used to blow coating asphalt, Method 5A shall be used to measure emissions from the blowing still for at least 90 minutes or for the duration of the blow, whichever is greater.

(d) The particulate emission rate, E , shall be computed as follows:

$$E = Q_{sa} \times C_s$$

(1) E is the particulate emission rate (kg/h);

(2) Q_{sa} is the average volumetric flow rate (dscm/h) as determined by Method 2; and

(3) C_s is the average concentration (kg/dscm) of particulate matter as determined by Method 5A.

(e) The asphalt roofing production rate, P (Mg/h), shall be determined by dividing the weight in megagrams (Mg) of roofing produced on the shingle or saturated felt process lines during the performance test by the number of hours required to conduct the performance test. The roofing production shall be obtained by direct measurement.

(f) The production rate of asphalt from the blowing still, P_s (Mg/h), shall be determined by dividing the weight of asphalt charged to the still by the time required for the performance test during an asphalt blow. The weight of asphalt charged to the still shall be determined at the starting temperature of the blow. The weight of asphalt shall be converted from the volume measurement as follows:

$$M = Vd/c$$

M = weight of asphalt in megagrams

V = volume of asphalt in cubic meters

d = density of asphalt in kilograms per cubic meter

c = conversion factor 1,000 kilograms per megagram

The density of asphalt at any measured temperature is calculated by using the following equation:
 $d = 1056.1 - (0.6176 \times ^{\circ}\text{C})$

The method of measurement shall have an accuracy of ± 10 percent.

(g) The saturator emission rate shall be computed as follows: $R = E/P$.

(h) The blowing still emission rate shall be computed as follows: $R_s = E/P_s$, where:

(1) R is the saturator emission rate (kg/Mg);

(2) R_s is blowing still emission rate (kg/Mg);

(3) E is the particulate emission rate (kg/h) from paragraph (c) of this section;

(4) P is the asphalt roofing production rate (Mg/h); and

(5) P_s is the asphalt charging rate (Mg/h).

(i) Temperature shall be measured and continuously recorded with the monitor required under § 60.473 (a) or (b) during the measurement of particulate by Method 5A and reported to the Administrator with the performance test results.

(j) If at a later date the owner or operator believes the emission limits in § 60.472 (a) and (b) are being met even though the temperature measured in accordance with § 60.473 paragraph (a) is exceeding that measured during the performance test, he may submit a written request to the Administrator to repeat the performance test and procedure outlined in paragraph (h) of this section.

(k) If fuel oil is to be used to fire an afterburner used to control a blowing still, the owner or operator may petition the Administrator in accordance with § 60.11(e) of the General Provisions to establish an opacity standard for the blowing still that will be the opacity standard when fuel oil is used to fire the afterburner. To obtain this opacity standard, the owner or operator must request the Administrator to determine opacity during an initial, or subsequent, performance test when fuel oil is used to fire the afterburner. Upon receipt of the results of the performance test, the Administrator will make a finding concerning compliance with the mass standard for the blowing still. If the Administrator finds that the facility was in compliance with the mass standard during the performance test but failed to meet the zero opacity standard, the Administrator will establish and promulgate in the Federal Register an opacity standard for the blowing still that will be the opacity standard when fuel oil is used to fire the afterburner. When the afterburner is fired with natural gas, the zero percent opacity

remains the applicable opacity standard.

Method 5A—Determination of Particulate Emissions from the Asphalt Processing and Asphalt Roofing Industry

1. Applicability and Principle.

1.1 *Applicability.* This method applies to the determination of particulate emissions from asphalt roofing industry process saturators, blowing stills, and other sources as specified in the regulations.

1.2 *Principle.* Particulate matter is withdrawn isokinetically from the source and collected on a glass filter fiber maintained at a temperature of $42^{\circ}\pm 10^{\circ}\text{C}$ ($108^{\circ}\pm 18^{\circ}\text{F}$). The particulate mass, which includes any material that condenses at or above the filtration temperature, is determined gravimetrically after removal of uncombined water.

2. Apparatus.

2.1 *Sampling Train.* The sampling train configuration is the same as shown in Figure 5-1 of Method 5. The sampling train consists of the following components:

2.1.1 *Probe Nozzle, Pitot Tube, Differential Pressure Gauge, Filter Holder, Condenser, Metering System, Barometer, and Gas Density Determination Equipment.* Same as Method 5, Sections 2.1.1, 2.1.3 to 2.1.5, and 2.1.7 to 2.1.10, respectively.

2.1.2 *Probe Liner.* Same as in Method 5, Section 2.1.2, with the note that at high stack gas temperatures (greater than 250°C (480°F)), water-cooled probes may be required to control the probe exit temperature to $42^{\circ}\pm 10^{\circ}\text{C}$ ($108^{\circ}\pm 18^{\circ}\text{F}$).

2.1.3 *Precollector Cyclone.* Borosilicate glass following the construction details shown in Air Pollution Technical Document-0581, "Construction Details of Isokinetic Source-Sampling Equipment".

Note.—The tester shall use the cyclone when the stack gas moisture is greater than 10 percent. The tester shall not use the precollector cyclone under other, less severe conditions.

2.1.4 *Filter Heating System.* Any heating (or cooling) system capable of maintaining a sample gas temperature at the exit end of the filter holder during sampling at $42^{\circ}\pm 10^{\circ}\text{C}$ ($108^{\circ}\pm 18^{\circ}\text{F}$). Install a temperature gauge capable of measuring temperature to within 3°C (5.4°F) at the exit end of the filter holder so that the sample gas temperature can be regulated and monitored during sampling. The tester may use systems other than the one shown in APTD-0581.

2.2 *Sample Recovery.* The equipment required for sample recovery is as follows:

2.2.1 *Probe-Liner and Probe-Nozzle Brushes, Graduated Cylinder and/or Balance, Plastic Storage Containers, and Funnel and Rubber Policeman.* Same as Method 5, Sections 2.2.1, 2.2.5, 2.2.6, and 2.2.7, respectively.

2.2.2 *Wash Bottles.* Glass.

2.2.3 *Sample Storage Containers.* Chemically resistant, borosilicate glass bottles, with rubber-backed Teflon screw cap liners or caps that are constructed so as to be leak-free and resistant to chemical attack by 1,1,1-trichloroethane (TCE), 500-ml or 1000-ml. (Narrow mouth glass bottles have been found to be less prone to leakage.)

2.2.4 *Petri Dishes.* Glass, unless otherwise specified by the Administrator.

2.2.5 *Funnel.* Glass.

2.3 *Analysis.* For analysis, the following equipment is needed:

2.3.1 *Glass Weighing Dishes, Desiccator, Analytical Balance, Balance, Hygrometer, and Temperature Gauge.* Same as Method 5, Sections 2.3.1 to 2.3.4, 2.3.6, and 2.3.7, respectively.

2.3.2 *Beakers.* Glass, 250-ml and 500-ml.

2.3.3 *Separatory Funnel.* 100-ml or greater.

3. Reagents.

3.1 *Sampling.* The reagents used in sampling are as follows:

3.1.1 *Filters, Silica Gel, and Crushed Ice.* Same as Method 5, Sections 3.1.1, 3.1.2, and 3.1.4, respectively.

3.1.2 *Stopcock Grease.* TCE-insoluble, heat-stable grease (if needed). This is not necessary if screw-on connectors with Teflon sleeves, or similar, are used.

3.2 *Sample Recovery.* Reagent grade 1,1,1-trichloroethane (TCE), ≤ 0.001 percent residue and stored in glass bottles, is required. Run TCE blanks prior to field use and use only TCE with low blank values (≤ 0.001 percent). The tester shall in no case subtract a blank value of greater than 0.001 percent of the weight of TCE used from the sample weight.

3.3 *Analysis.* Two reagents are required for the analysis:

3.3.1 *TCE.* Same as 3.2.

3.3.2 *Desiccant.* Same as Method 5, Section 3.3.2.

4. Procedure.

4.1 *Sampling Train Operation.* The complexity of this method is such that in order to obtain reliable results, testers should be trained and experienced with Method 5 test procedures.

4.1.1 *Pretest Preparation.* Unless otherwise specified, maintain and calibrate all components according to the procedure described in Air Pollution Technical Document-0576, "Maintenance, Calibration, and Operation of Isokinetic Source-Sampling Equipment".

Prepare probe liners and sampling nozzles as needed for use. Thoroughly clean each component with soap and water followed by a minimum of three TCE rinses. Use the probe and nozzle brushes during at least one of the TCE rinses (refer to Section 4.2 for rinsing techniques). Cap or seal the open ends of the probe liners and nozzles to prevent contamination during shipping.

Prepare silica gel portions and glass filters as specified in Method 5, Section 4.1.1.

4.1.2 *Preliminary Determinations.* Select the sampling site, probe nozzle, and probe length as specified in Method 5, Section 4.1.2.

Select a total sampling time greater than or equal to the minimum total sampling time specified in the test procedures section of the applicable regulation. Follow the guidelines outlined in Method 5, Section 4.1.2, for sampling time per point and total sample volume collected.

4.1.3 *Preparation of Collection Train.* Prepare the collection train as specified in Method 5, Section 4.1.3, with the addition of the following:

Set up the sampling train as shown in Figure 5-1 of Method 5 with the addition of

the precollector cyclone, if used, between the probe and filter holder. The temperature of the precollector cyclone, if used, should be about the same as for the filter, i.e., $42^{\circ}\pm 10^{\circ}\text{C}$ ($108^{\circ}\pm 18^{\circ}\text{F}$). Use no stopcock grease on ground glass joints unless the grease is insoluble in TCE.

4.1.4 *Leak Check Procedures.* Follow the procedures given in Method 5, Sections 4.1.4.1 (Pretest Leak Check), 4.1.4.2 (Leak Check During Sample Run), and 4.1.4.3 (Post-Test Leak Check).

4.1.5 *Particulate Train Operation.* Operate the sampling train as described in Method 5, Section 4.1.5, except maintain the gas temperature exiting the filter at $42^{\circ}\pm 10^{\circ}\text{C}$ ($108^{\circ}\pm 18^{\circ}\text{F}$).

4.1.6 *Calculation of Percent Isokinetic.* Same as in Method 5, Section 4.1.6.

4.2 *Sample Recovery.* Using the procedures and techniques described in Method 5, Section 4.2, quantitatively recover any particulate matter into the following containers (additions and deviations to the stated procedures are as noted):

4.2.1 *Container No. 1 (Filter).* Same instructions as Method 5, Section 4.2, "Container No. 1." If it is necessary to fold the filter, do so such that the film of oil is inside the fold.

4.2.2 *Container No. 2 (Probe to Filter Holder).* Taking care to see that material on the outside of the probe or other exterior surfaces does not get into the sample, quantitatively recover particulate matter or any condensate from the probe nozzle, probe fitting, probe liner, precollector cyclone and collector flask (if used), and front half of the filter holder by washing these components with TCE and placing the wash in a glass container. Carefully measure the total amount of TCE used in the rinses. Perform the TCE rinses as described in Method 5, Section 4.2, "Container No. 2," using TCE instead of acetone.

Brush and rinse the inside of the cyclone, cyclone collection flask, and the front half of the filter holder. Brush and rinse each surface three times or more, if necessary, to remove visible particulate.

4.2.3 *Container No. 3 (Silica Gel).* Same procedure as in Method 5, Section 4.2, "Container No. 3."

4.2.4 *Impinger Water.* Treat the impingers as follows: Make a notation of any color or film in the liquid catch. Follow the same procedure as in Method 5, Section 4.2, "Impinger Water."

4.2.5 *Blank.* Save a portion of the TCE used for cleanup as a blank. Take 200 ml of this TCE directly from the wash bottle being used and place it in a glass sample container labeled "TCE blank."

4.3 *Analysis.* Record the data required on a sheet such as the one shown in Figure 5A-1. Handle each sample container as follows:

4.3.1 *Container No. 1 (Filter).* Transfer the filter from the sample container to a tared glass weighing dish and desiccate for 24 hours in a desiccator containing anhydrous calcium sulfate. Rinse Container No. 1 with a measured amount of TCE and analyze this rinse with the contents of Container No. 2. Weigh the filter to a constant weight. For the purpose of Section 4.3, the term "constant

weight" means a difference of no more than 10 percent or 2 mg (whichever is greater) between two consecutive weighings made 24 hours apart. Report the "final weight" to the nearest 0.1 mg as the average of these two values.

4.3.2 Container No. 2 (Probe to Filter Holder). Before adding the rinse from Container No. 1 to Container No. 2, note the level of liquid in the container and confirm on the analysis sheet whether or not leakage occurred during transport. If noticeable leakage occurred, either void the sample or take steps, subject to the approval of the Administrator, to correct the final results.

Measure the liquid in this container either volumetrically to ± 1 ml or gravimetrically to ± 0.5 g. Check to see if there is any appreciable quantity of condensed water present in the TCE rinse (look for a boundary layer or phase separation). If the volume of condensed water appears larger than 5 ml, separate the oil-TCE fraction from the water fraction using a separatory funnel. Measure the volume of the water phase to the nearest ml; adjust the stack gas moisture content, if necessary (see Sections 6.4 and 6.5). Next, extract the water phase with several 25-ml portions of TCE until, by visual observation, the TCE does not remove any additional organic material. Evaporate the remaining water fraction to dryness at 93°C (200°F), desiccate for 24 hours, and weigh to the nearest 0.1 mg.

Treat the total TCE fraction (including TCE from the filter container rinse and water phase extractions) as follows: Transfer the TCE and oil to a tared beaker and evaporate at ambient temperature and pressure. The evaporation of TCE from the solution may take several days. Do not desiccate the sample until the solution reaches an apparent constant volume or until the odor of TCE is not detected. When it appears that the TCE has evaporated, desiccate the sample and weigh it at 24-hour intervals to obtain a "constant weight" (as defined for Container No. 1 above). The "total weight" for Container No. 2 is the sum of the evaporated particulate weight of the TCE-oil and water phase fractions. Report the results to the nearest 0.1 mg.

4.3.3 Container No. 3 (Silica Gel). This step may be conducted in the field. Weigh the spent silica gel (or silica gel plus impinger) to the nearest 0.5 g using a balance.

4.3.4 "TCE Blank" Container. Measure TCE in this container either volumetrically or gravimetrically. Transfer the TCE to a tared 250-ml beaker and evaporate to dryness at ambient temperature and pressure. Desiccate for 24 hours and weigh to a constant weight. Report the results to the nearest 0.1 mg.

Note.—In order to facilitate the evaporation of TCE liquid samples, these samples may be dried in a controlled temperature oven at temperatures up to 38°C (100°F) until the liquid is evaporated.

5. Calibration.

Calibrate the sampling train components according to the indicated sections of Method 5: Probe Nozzle (5.1), Pitot Tube Assembly (5.2), Metering System (5.3), Probe Heater (5.4), Temperature Gauges (5.5), Leak Check of Metering System (5.6), and Barometer (5.7).

6. Calculations.

6.1 Nomenclature. Same as in Method 5, Section 6.1, with the following additions:

C_t = TCE blank residue concentration, mg/g.
 M_t = Mass of residue of TCE after evaporation, mg.

V_{pc} = Volume of water collected in precollector, ml.

V_t = Volume of TCE blank, ml.

V_{tw} = Volume of TCE used in wash, ml.

W_t = Weight of residue in TCE wash, mg.

P_t = Density of TCE, mg/ml (see label on bottle).

6.2 Dry Gas Meter Temperature and Orifice Pressure Drop. Using the data obtained in this test, calculate the average dry gas meter temperature and average orifice pressure drop (see Figure 5-2 of Method 5).

6.3 Dry Gas Volume. Using the data from this test, calculate $V_{m(std)}$ by using Equation 5-1 of Method 5. If necessary, adjust the volume for leakages.

6.4 Volume of Water Vapor.

$$V_{w(std)} = K_1(V_{tc} + V_{pc}) \quad \text{Eq. 5A-1.}$$

Where:

$K_1 = 0.00133 \text{ m}^3/\text{ml}$ for metric units.

$= 0.04707 \text{ ft}^3/\text{ml}$ for English units.

$$B_{wa} = V_{w(std)}/V_{m(std)} + V_{w(std)} \quad \text{Eq. 5A-2.}$$

Note.—In saturated or water droplet-laden gas streams, two calculations of the moisture content of the stack gas shall be made, one from the impinger and precollector analysis (Equations 5A-1 and 5A-2) and a second from the assumption of saturated conditions. The lower of the two values of moisture content shall be considered correct. The procedure for determining the moisture content based upon assumption of saturated conditions is given in the note of Section 1.2 of Method 4. For the purpose of this method, the average stack gas temperature from Figure 2 may be used to make this determination, provided that the accuracy of the in-stack temperature sensor is within $\pm 1^\circ\text{C}$ (2°F).

6.6 TCE Blank Concentration.

$$C_t = M_t/V_t P_t \quad \text{Eq. 5A-3.}$$

6.7 TCE Wash Blank.

$$W_t = (C_t)(V_{tw})(P_t) \quad \text{Eq. 5A-4.}$$

6.8 Total Particulate Weight. Determine the total particulate catch from the sum of the weights obtained from Containers 1, 2, and 3, less the TCE blank.

6.9 Particulate Concentration.

$$C_p = K_2 M_p / V_{m(std)} \quad \text{Eq. 5A-5.}$$

Where:

$K_2 = 0.001 \text{ g/mg.}$

6.10 Isokinetic Variation and Acceptable Results. Method 5, Section 6.11 and 6.12, respectively.

7. Bibliography

The bibliography for Reference Method 5A is the same as for Method 5, Section 7.

Method 22—Visual Determination of Fugitive Emissions From Material Processing Sources

1. Introduction.

This method involves the visual determination of fugitive emissions, i.e., emissions not emitted directly from a process stack or duct. Fugitive emissions include emissions that (1) escape capture by process

equipment exhaust hoods; (2) are emitted during material transfer; (3) are emitted from buildings housing material processing or handling equipment; and (4) are emitted directly from process equipment.

This method determines the amount of time that any visible emissions occur during the observation period, i.e., the accumulated emission time. This method does not require that the opacity of emissions be determined. Since this procedure requires only the determination of whether a visible emission occurs and does not require the determination of opacity levels, observer certification according to the procedures of Reference Test Method 9 are not required. However, it is necessary that the observer is educated on the general procedures for determining the presence of visible emissions. As a minimum, the observer must be trained and knowledgeable regarding the effects on the visibility of emissions caused by background contrast, ambient lighting, observer position relative to lighting, wind, and the presence of uncombined water (condensing water vapor). This training is to be obtained from written materials found in References 7.1 and 7.2 or from the lecture portion of the Method 9 certification course.

2. Applicability and Principle.

2.1 Applicability. This method applies to the determination of the frequency of fugitive emissions from stationary sources (located indoors or outdoors) when specified as the test method for determining compliance with new source performance standards.

2.2 Principle. Fugitive emissions produced during material processing, handling, and transfer operations are visibly determined by an observer without the aid of instruments.

3. Definitions.

3.1 Emission Frequency. Percentage of time that emissions are visible during the observation period.

3.2 Emission Time. Accumulated amount of time that emissions are visible during the observation period.

3.3 Fugitive Emissions. Pollutant generated by an affected facility which is not collected by a capture system and is released to the atmosphere.

3.4 Observation Period. Accumulated time period during which observations are conducted, not to be less than 6 minutes.

4. Equipment.

4.1 Stopwatches. Accumulative type with unit divisions of at least 0.5 seconds; two required.

4.2 Light Meter. Light meter capable of measuring illuminance in the 50- to 200-lux range; required for indoor observations only.

5. Procedure.

5.1 Position. Survey the affected facility or building or structure housing the process to be observed and determine the locations of potential emissions. If the affected facility is located inside a building, determine an observation location that is consistent with the requirements of the applicable regulation (i.e., outside observation of emissions escaping the building/structure or inside observation of emissions directly emitted from the affected facility process unit). Then select a position that enables a clear view of the potential emission point(s) of the affected

facility or of the building or structure housing the affected facility, as appropriate for the applicable subpart. A position at least 15 feet, but not more than 0.25 miles, from the emission source is recommended. For outdoor locations, select a position where the sun is not directly in the observer's eyes.

5.2 Field Records.

5.2.1 Outdoor Location. Record the following information on the field data sheet (Figure 22-1): company name, industry, process unit, observer's name, observer's affiliation, and date. Record also the estimated wind speed, wind direction, and sky condition. Sketch the process unit being observed and note the observer location relative to the source and the sun. Indicate the potential and actual emission points on the sketch.

5.2.2 Indoor Location. Record the following information on the field data sheet (Figure 22-2): company name, industry, process unit, observer's name, observer's affiliation, and date. Record as appropriate the type, location, and intensity of lighting on the data sheet. Sketch the process unit being observed and note observer location relative to the source. Indicate the potential and actual fugitive emission points on the sketch.

5.3 Indoor Lighting Requirements. For indoor locations, use a light meter to measure the level of illumination at a location as close to the emission source(s) as is feasible. An illumination of greater than 100 lux (10 foot candles) is considered necessary for proper application of this method.

5.4 Observations. Record the clock time when observations begin. Use one stopwatch to monitor the duration of the observation period; start this stopwatch when the observation period begins. If the observation period is divided into two or more segments by process shutdowns or observer rest breaks, stop the stopwatch when a break begins and restart it without resetting when the break ends. Stop the stopwatch at the end of the observation period. The accumulated time indicated by this stopwatch is the duration of the observation period. When the observation period is completed, record the clock time.

During the observation period, continuously watch the emission source. Upon observing an emission (condensed water vapor is not considered an emission), start the second accumulative stopwatch; stop the watch when the emission stops. Continue this procedure for the entire observation period. The accumulated elapsed time on this stopwatch is the total time emissions were visible during the observation period, i.e., the emission time.

5.4.1 Observation Period. Choose an observation period of sufficient length to meet the requirements for determining compliance with the emission regulation in the applicable subpart. When the length of the observation period is specifically stated in the applicable subpart, it may not be necessary to observe the source for this entire period if the emission time required to indicate noncompliance (based on the specified observation period) is observed in a shorter time period. In other words, if the regulation prohibits emissions for more than 6 minutes in any hour, then observations may

(optional) be stopped after an emission time of 6 minutes is exceeded. Similarly, when the regulation is expressed as an emission frequency and the regulation prohibits emissions for greater than 10 percent of the time in any hour, then observations may (optional) be terminated after 6 minutes of emissions are observed since 6 minutes is 10 percent of an hour. In any case, the observation period shall not be less than 6 minutes in duration. In some cases, the process operation may be intermittent or cyclic. In such cases, it may be convenient for the observation period to coincide with the length of the process cycle.

5.4.2 Observer Rest Breaks. Do not observe emissions continuously for a period of more than 15 to 20 minutes without taking a rest break. For sources requiring observation periods of greater than 20 minutes, the observer shall take a break of not less than 5 minutes and not more than 10 minutes after every 15 to 20 minutes of observation. If continuous observations are desired for extended time periods, two observers can alternate between making observations and taking breaks.

5.4.3 Visual Interference. Occasionally, fugitive emissions from sources other than the affected facility (e.g., road dust) may prevent a clear view of the affected facility. This may particularly be a problem during periods of high wind. If the view of the potential emission points is obscured to such a degree that the observer questions the validity of continuing observations, then the observations are terminated, and the observer clearly notes this fact on the data form.

5.5 Recording Observations. Record the accumulated time of the observation period on the data sheet as the observation period duration. Record the accumulated time emissions were observed on the data sheet as the emission time. Record the clock time the observation period began and ended, as well as the clock time any observer breaks began and ended.

6. Calculations.

If the applicable subpart requires that the emission rate be expressed as an emission frequency (in percent), determine this value as follows: Divide the accumulated emission time (in seconds) by the duration of the observation period (in seconds) or by any minimum observation period required in the applicable subpart, if the actual observation period is less than the required period and multiply this quotient by 100.

7. References.

7.1 Missan, Robert and Arnold Stein. Guidelines for Evaluation of Visible Emissions Certification, Field Procedures, Legal Aspects, and Background Material. EPA Publication No. EPA-340/1-75-007. April 1975

7.2 Wohlschlegel, P. and D. E. Wagoner. Guideline for Development of a Quality Assurance Program: Volume IX—Visual Determination of Opacity Emissions From Stationary Sources. EPA Publication No. EPA-650/4-74-005-I. November 1975.

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40 CFR Part 81

[A-4-FRL 2180-2 (GA-001)]

Designation of Areas for Air Quality Planning Purposes; Georgia: Redesignation of Rossville Particulate Area

AGENCY: Environmental Protection Agency.

ACTION: Final rule.

SUMMARY: EPA hereby grants a request made by Georgia that the total suspended particulate attainment status of a portion of the northern part of Walker County which includes Rossville, Georgia, be changed from nonattainment to attainment.

EFFECTIVE DATE: This action will be effective on October 5, 1982 unless notice is received within 30 days that someone wishes to submit adverse or critical comments.

FOR FURTHER INFORMATION CONTACT: Mr. Barry Gilbert, Air Management Branch, EPA Region IV at the above address and telephone number 404/881-3286 or FTS 257-3286.

SUPPLEMENTARY INFORMATION: On March 3, 1978 (43 FR 8962 at 8981), the Administrator designated a portion of the northern part of Walker County, Georgia, which includes Rossville, nonattainment for total suspended particulate. On April 29, 1982, the Georgia Environmental Protection Division (GEPD) submitted 24 consecutive months of air quality data showing that the national ambient air quality standards (NAAQS) for total suspended particulate had not been violated. There were no violations of the 150 $\mu\text{g}/\text{m}^3$ secondary NAAQS. The geometric means for March 1980 through February 1981 and March 1981 through February 1982 were 72 and 54 $\mu\text{g}/\text{m}^3$ respectively. Both geometric means are below the 75 $\mu\text{g}/\text{m}^3$ NAAQS. Since there are two years of ambient air quality data showing attainment, EPA is changing the designation to attainment.

The public should be advised that this action will be effective 60 days from the date of this Federal Register notice. However, if notice is received within 30 days that someone wishes to submit adverse or critical comments, this action will be withdrawn and two subsequent notices will be published before the effective date. One notice will withdraw the final action and another will begin a new rulemaking by announcing a proposal of the action and establishing a comment period.

Under 5 U.S.C. Section 605(b), the Administrator has certified that area