**Computer Modeling of Unburned Carbon as Part of Boiler Retrofits and Nitric Oxide Control** 

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## Introduction

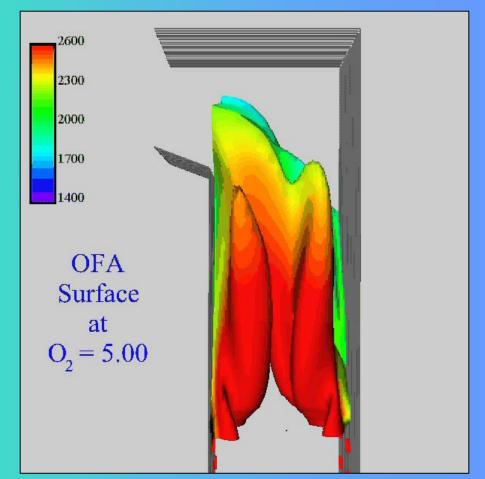
- Developed CFD modeling for Design of NO<sub>x</sub> Controls
- NO<sub>x</sub> control and Unburned Carbon intertwined
- Initially Used Predictions of CO and Fuel Richness at Model Exit to Estimate Impact on UBC
- Expanded to include Unburned Carbon Predictions
- Incorporates ESA Combustion Experience:
  - Controlling Mechanisms of Initial Modeling Effort
  - Incorporated into Modeling Improvement
  - Model Application is only as good as Experience Behind it

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# CFD Modeling for NO<sub>x</sub> Control

- Steady Navier-Stokes
  Equations
- Coal Devolatilization and combustion
- Turbulence, radiation, two-phase flow
- Commercial Software base

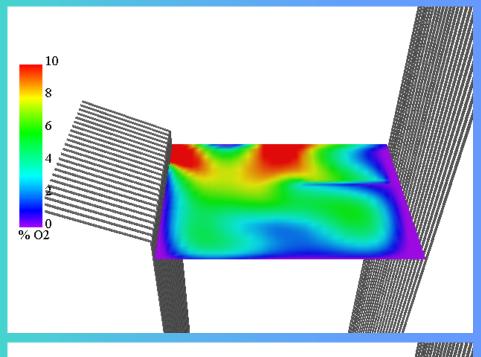
- NO<sub>x</sub> Ports Block Furnace Flow
  - Temperature difference of 650 F vs 3200 F between gas
  - Hot Flames form bouyant bypass chimneys

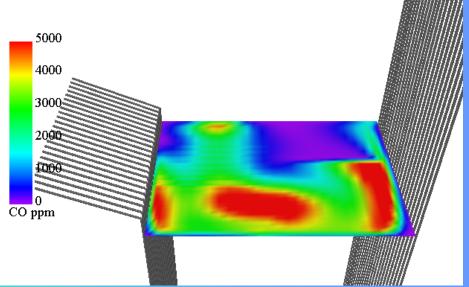




# NO<sub>x</sub> Control effect on Exit CO and O<sub>2</sub>

- NO<sub>x</sub> Control Principle: Fuel-rich at Adiabatic Flame Peak Temperature
- O<sub>2</sub> and CO commonly predicted in CFD models
- CO good indicator of UBC Problems
- Integrate CO and/or fuel richness at Furnace Exit to estimate impact on UBC



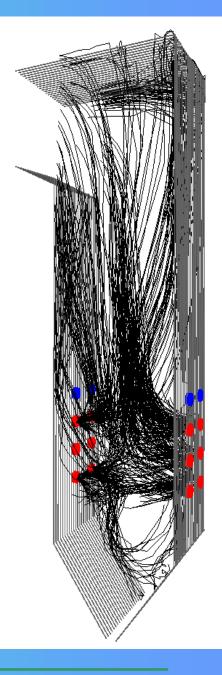




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# CFD Modeling of Coal Particles for UBC

- Directly track individual coal particles
- Simulate Volatilization and Char burn out for mass transfer
- Count particles still existing at model exit to determine UBC impact





# NO<sub>v</sub> Control Experience

- Low Excess Air: LEA most important
- Superheat and Reheat Temperatures depend on Furnace Air Residence Time
- Corrosion Mechanisms Change in Reducing atmosphere
- Carbon: LOI dependent on LEA, Air balance, and Air profile



## First Example: Lean Gas Reburning UBC

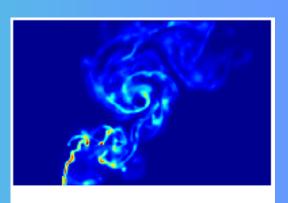
• CFD and LIM Modeling used to design Fuel Lean Gas Reburn System for Duke Energy Riverbend Unit 7 - 144 MW Tangential

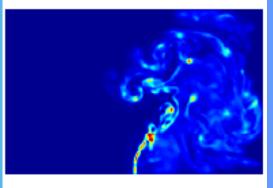
- Models to Predict Expected NO<sub>x</sub> Reduction and CO increase
- Models used to Select injector location and number
- Design Iteration of Natural Gas impact on CO and UBC
- Models and test data employed to re-analyze design to mitigate impact on CO and UBC

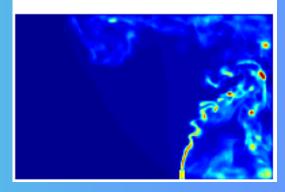


# FLGR LIM Model for Injector Positioning

- Natural Gas as NO<sub>x</sub> Reducing/Finishing Agent
- Riverbend Fuel Lean Gas Reburn
- High Excess Air near walls
- Reburn Mixing into Fireball
- Natural Gas burns easily, quenching O<sub>2</sub> availability for Carbon burnout





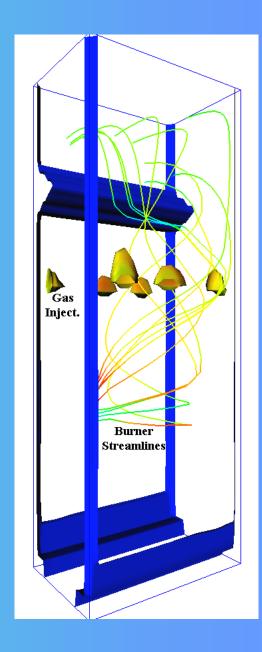


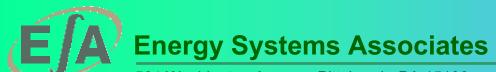


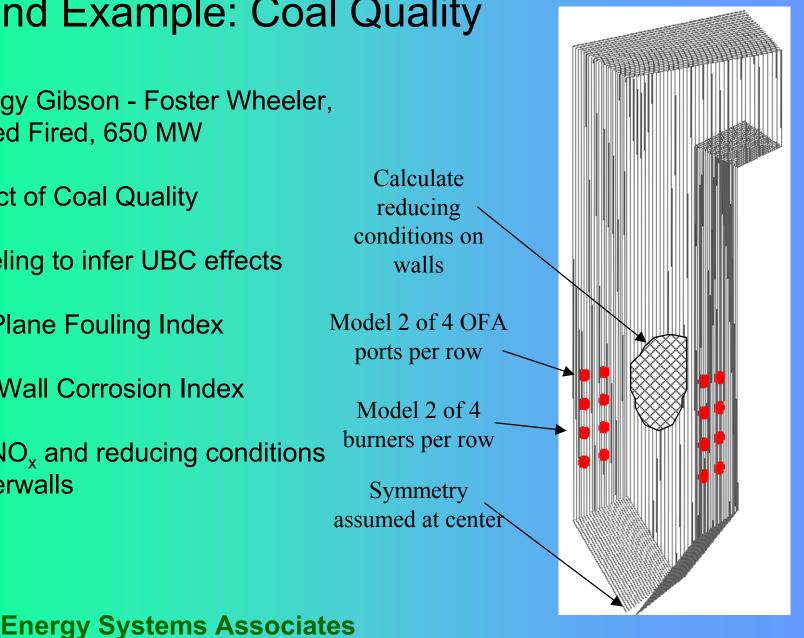
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# FLGR CFD Model

- Unexpected Impact on CO and UBC
- Initial Modeling focused on FLGR
- Missed impact on CO and UBC
- Modeling of Primary Coal Combustion interaction with OFA Separated from Secondary Reburn Combustion to Correct UBC impact



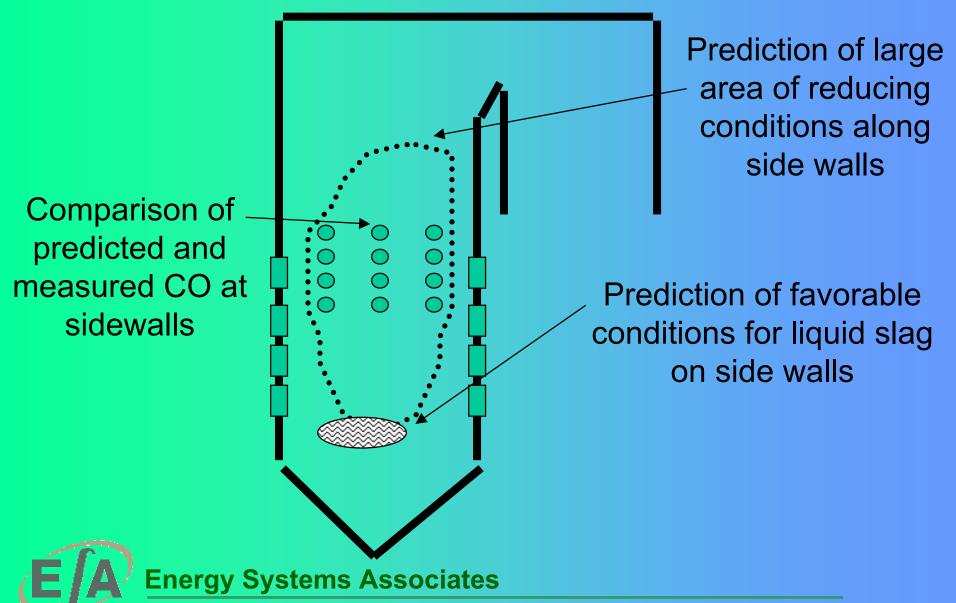




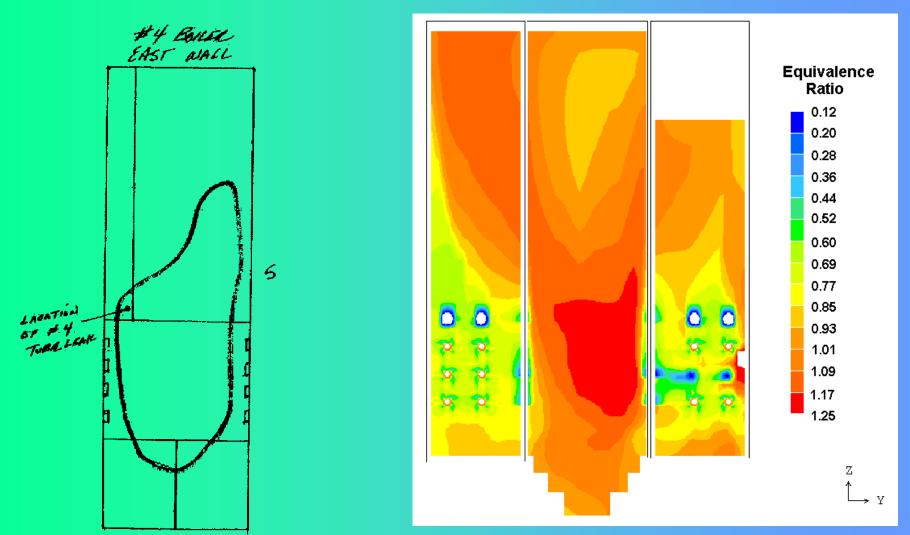
### Second Example: Coal Quality

- Cinergy Gibson Foster Wheeler, **Opposed Fired**, 650 MW
- Impact of Coal Quality
- Modeling to infer UBC effects
- Exit Plane Fouling Index
- Side Wall Corrosion Index
- Exit NO<sub>x</sub> and reducing conditions on waterwalls

### **CFD Model Matching Observations**

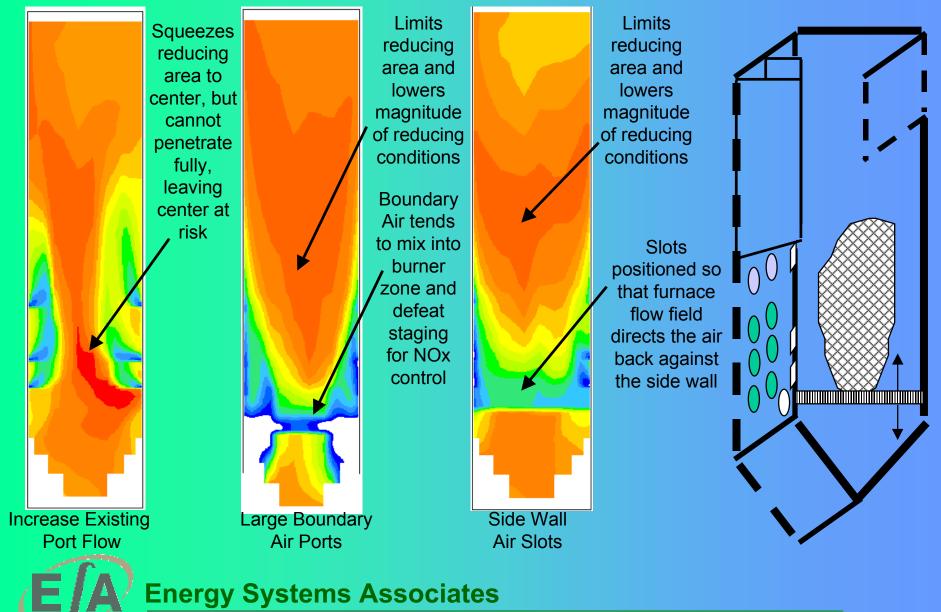


### **CFD Model Matching Observations**



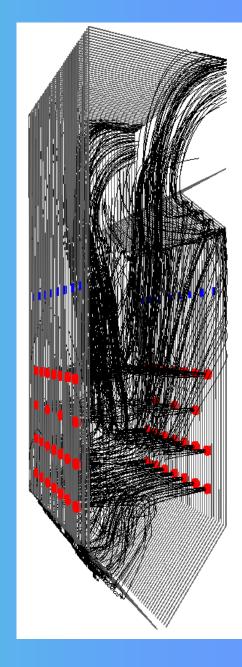
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### **CFD Model Predictions**



# Third Example: OFA Design

- B & W Oppossed Fired Unit OFA Design
- PRB Coal, Low UBC under current Operation
- Design OFA System for NO<sub>x</sub> reduction
- Model to find Optimum of NO<sub>x</sub>, CO and UBC





# Example of Pre-Retrofit Analysis

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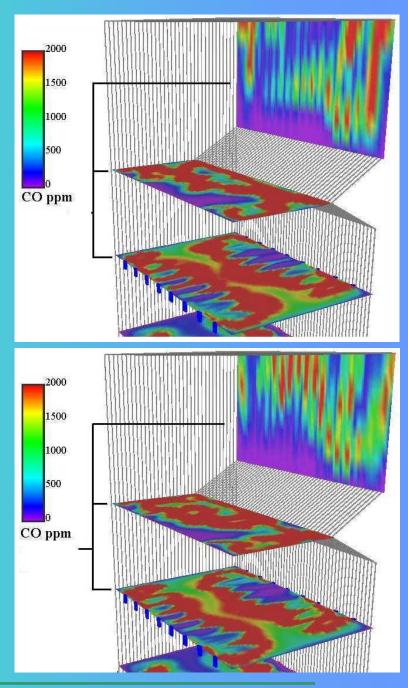
- Model Multiple OFA
  Designs
- Address UBC During Design Phase
- Small Changes to Port Design improves UBC without effecting NO<sub>x</sub>

Redesign Ports: UBC 1% above Baseline

Initial Design:

**Baseline** 

UBC 2% above



## **CFD Use in Design**

Computation Fluid Dynamics

### **Design**

#### **Computer Furnace Models**

Simulate unbuilt configuration

#### **Experience**

- Incorporate Operating Data and Experience of Approximately Similar Situation
- NO<sub>x</sub> Reduced 50 %
- UBC maintained with LEA, OFA, or LNB

#### **Operation**



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# Fourth Example: Computer Optimization Model

- NO<sub>x</sub> Reduction and Heat Rate Improvement
- Demonstration of *QuickStudy* Adaptive Process Control (APC) software to determine the extent to which NO<sub>x</sub> could be reduced without affecting boiler efficiency
- Involves spatial monitoring and balancing of furnace excess O<sub>2</sub> levels as measured by an O<sub>2</sub> grid in the boiler outlet
- Spatial balancing allows reduced excess O<sub>2</sub> levels without exceeding the "CO threshold"
- QuickStudy acts as a "silent sentry" for low O<sub>2</sub> operation that is transparent to the boiler operator





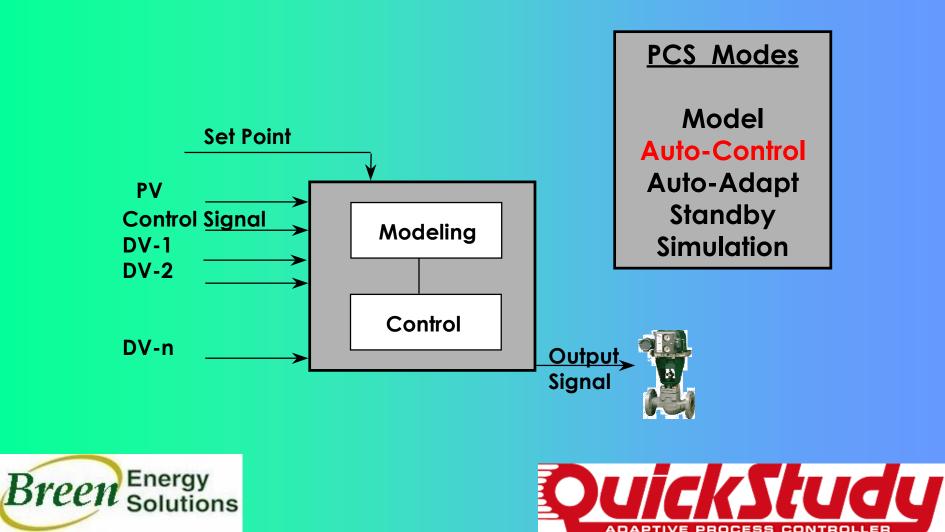
# Test Unit: Albright #1

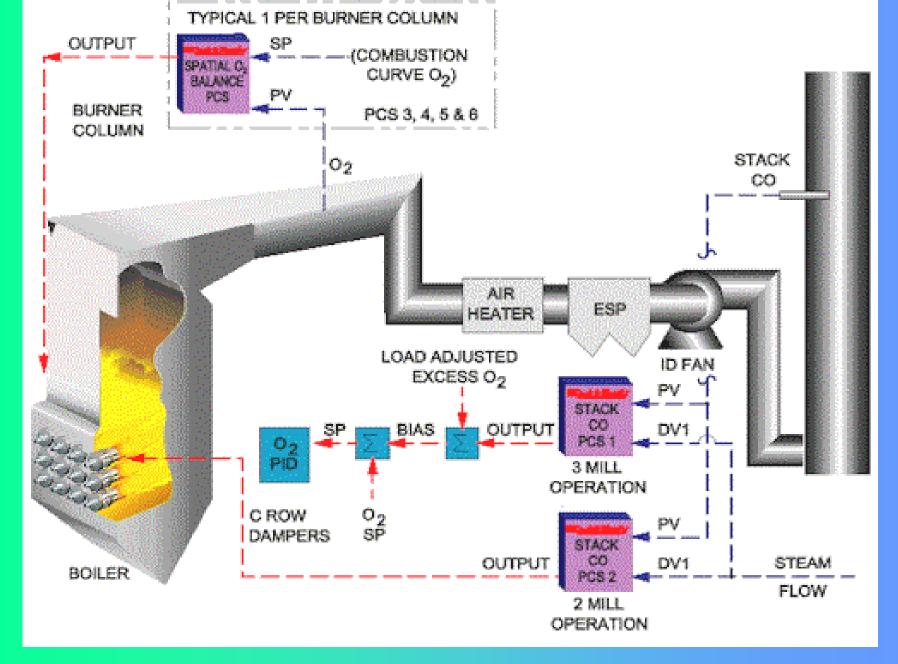
- Riley Stoker sub-critical, single reheat drum boiler with nominal rating of 80 MW
- Equipped with 12 Riley CCV-90 low NO<sub>x</sub> Burners
- Fires eastern bituminous coal
- Burner array is three rows by four columns
- Each burner row supplied by one B&W E70 pulverizer
- Design conditions at rated load are 700K lb/hr steam flow, superheat outlet conditions of 910 psig and 905 °F





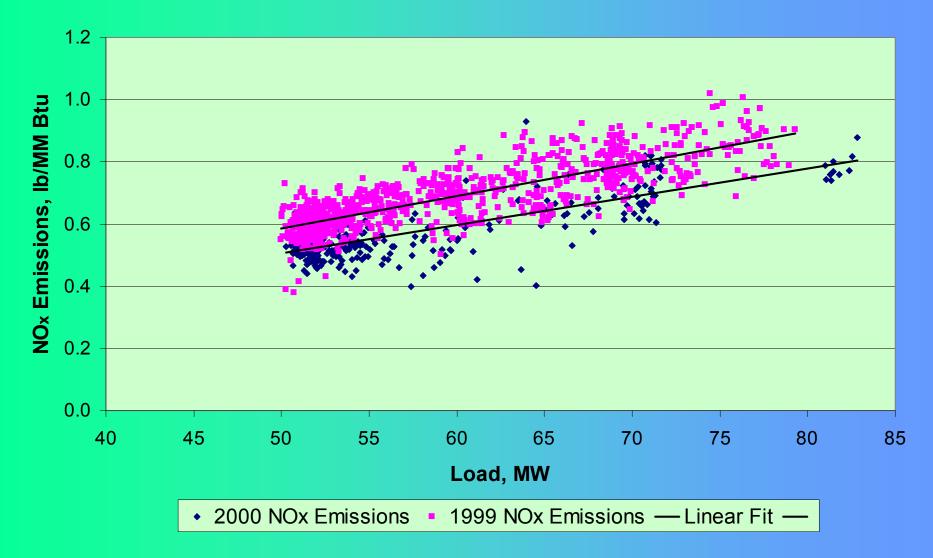
## **PCS Block Operating Modes**





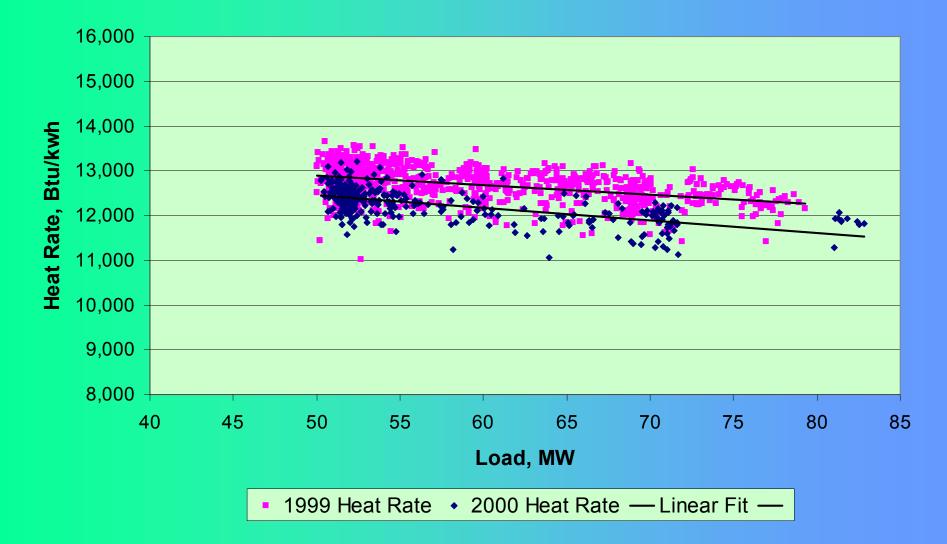
The Adaptive Process Control Strategy

#### Albright Unit 1 1999 & 2000 Ozone Season NOx Emissions Three Mill Operation



Albright Unit 1 NO<sub>x</sub> CEM Data with and without APC - 3 Mill Operation

#### Albright Unit 1 1999 & 2000 Ozone Season Heat Rate Three Mill Operation



Albright Unit 1 CEM Heat Rate Data with and without APC - 3 Mill Operation

## QuickStudy Results: Albright #1

- NO<sub>x</sub> reduced by 15-17% on average, 18% with 3 mills
- CEM heat rate improved by minimum of 2%
- CO emissions controlled to below 250 ppm
- Average opacity levels were slightly improved
- Furnace slagging conditions were improved as a result of controlling air supplies to individual burners by means of spatial balancing of O<sub>2</sub>





### Conclusions

