

# Refrigerator Cryostats at BENSC

Michael Meißner and Sebastian Gerischer  
Bastian Klemke and Dirk Wallacher  
HMI Berlin, BENSC

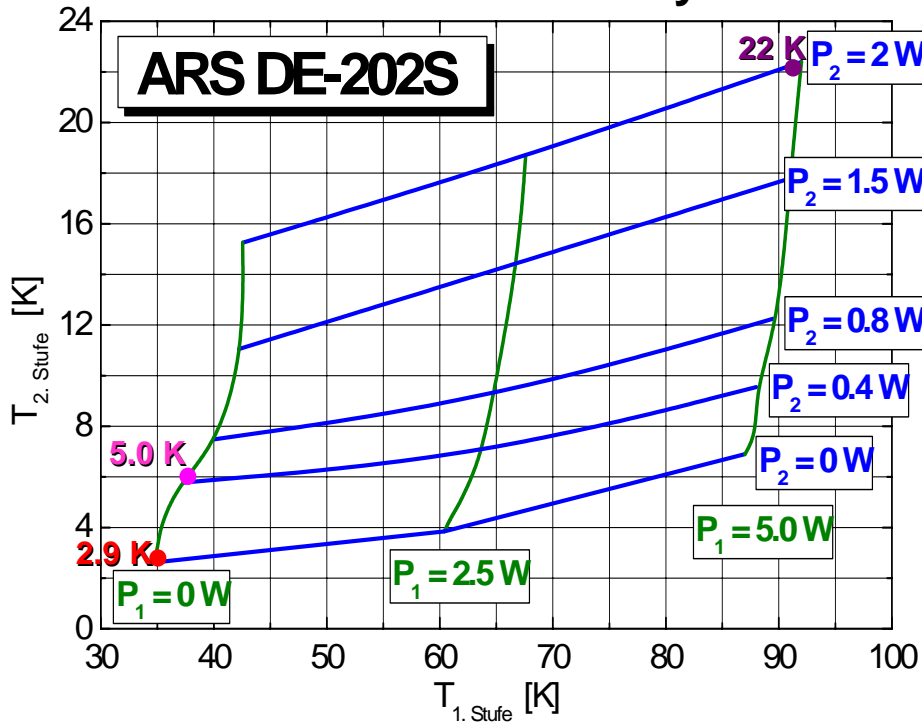
The competition: Liquid Helium-cooled versus Refrigerator-cooled

The marking: Measurements of  $T_{\min}$  &  $T_{\max}$  &  $P(T)$  and  $\Delta T / T_0$  &  $T_0(t)$   
Costs for Invest & Consum and Service & Personal

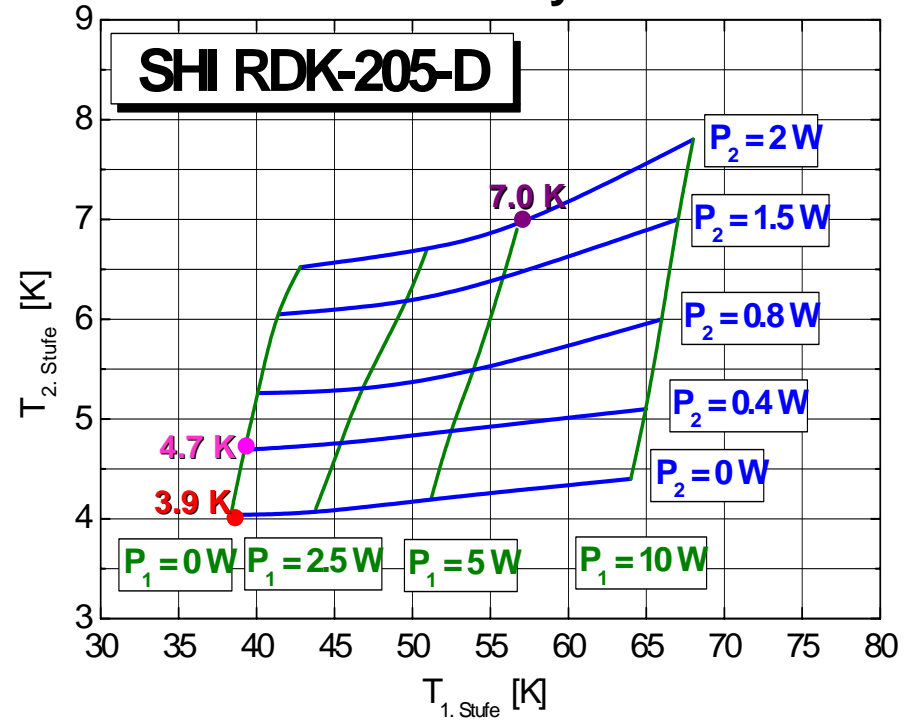
The winner is: A great variety of CCR-cryostats

# Cooling power plots of two GM-CCR's at BENSC (manufactured and delivered in 2004)

## Advanced Research Systems

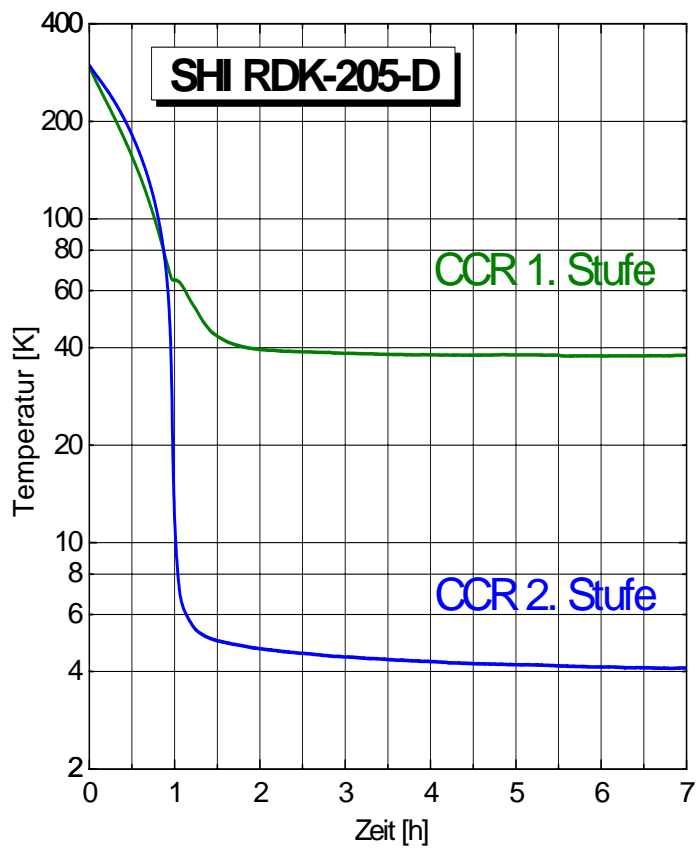
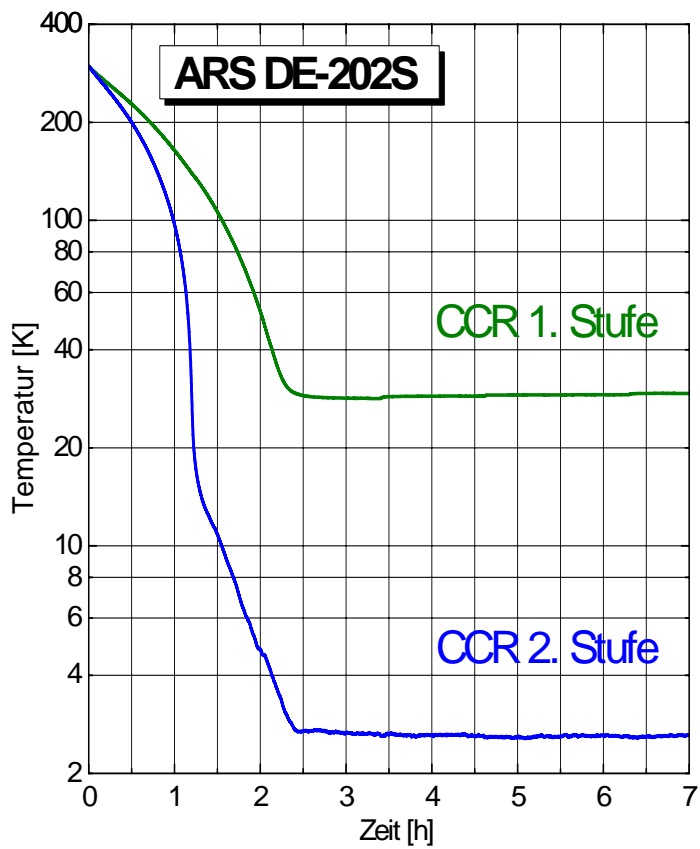


## Sumitomo Heavy Industries



→ differences !!!

# Cooling curves $T_o(t)$ with minimum load

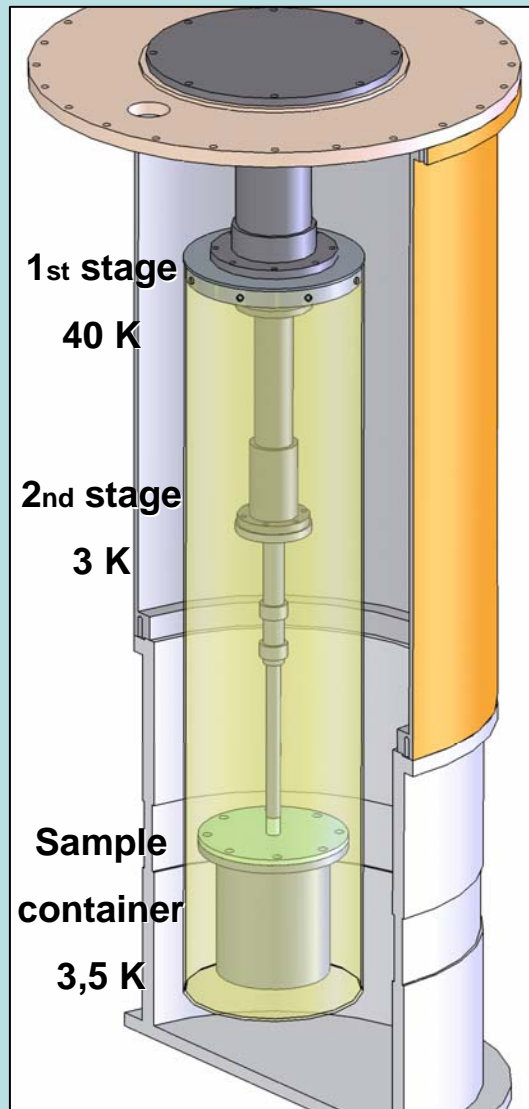


# Example 1

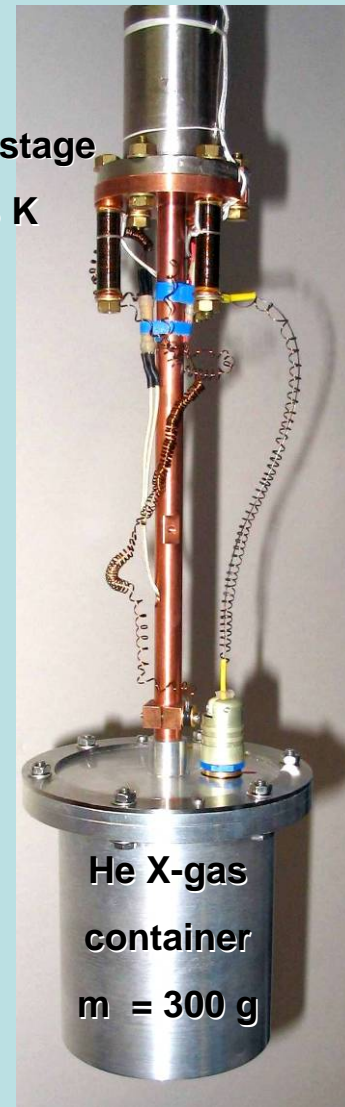
**SHI CCR in ORANGE-body**

**HMI-BENSC**

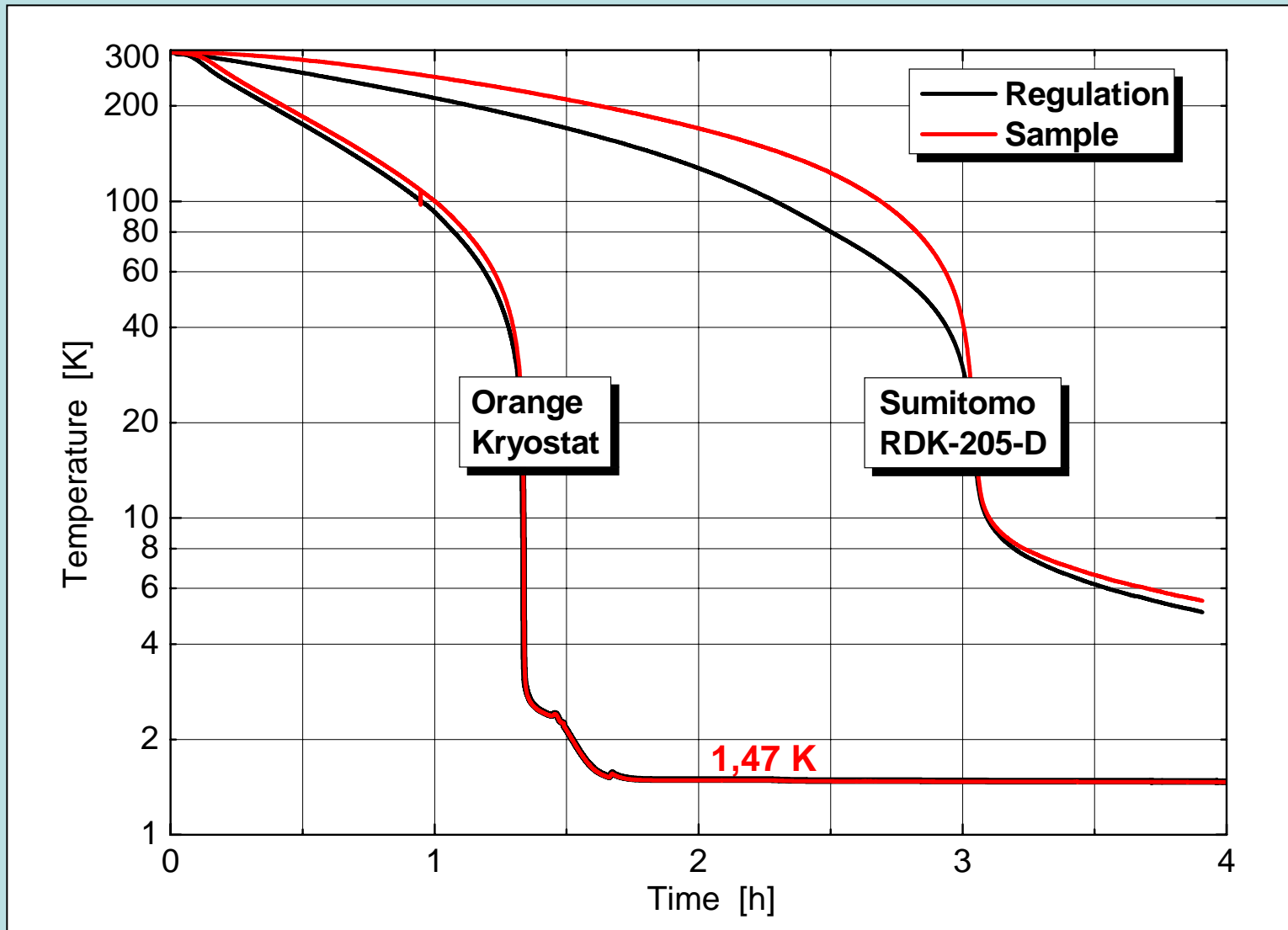
# SHI RDK-205 with OS-OVC for $T = 3.5 \text{ K} \dots 400 \text{ K}$



2nd stage  
3 K



# Comparison of cool-down ORANGE vs. CCR

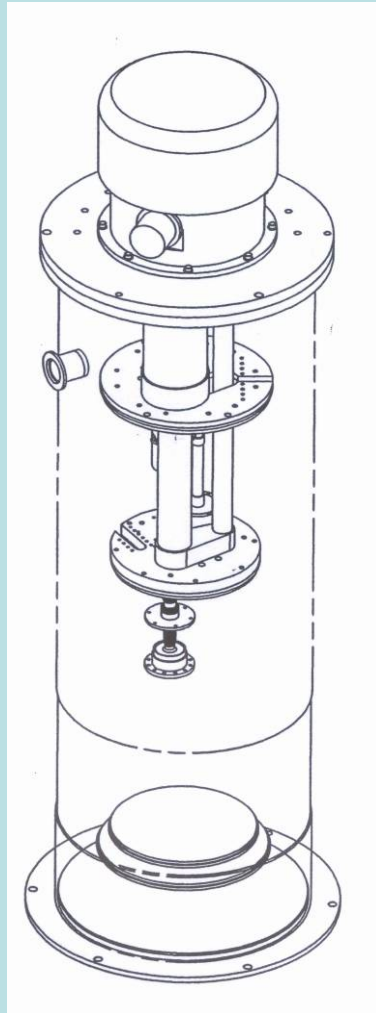


## Example 2

**SHI Pulsetube Refrigerator  
plus  $^3\text{He}$  sorption stage  
OI Heliox AC-V**

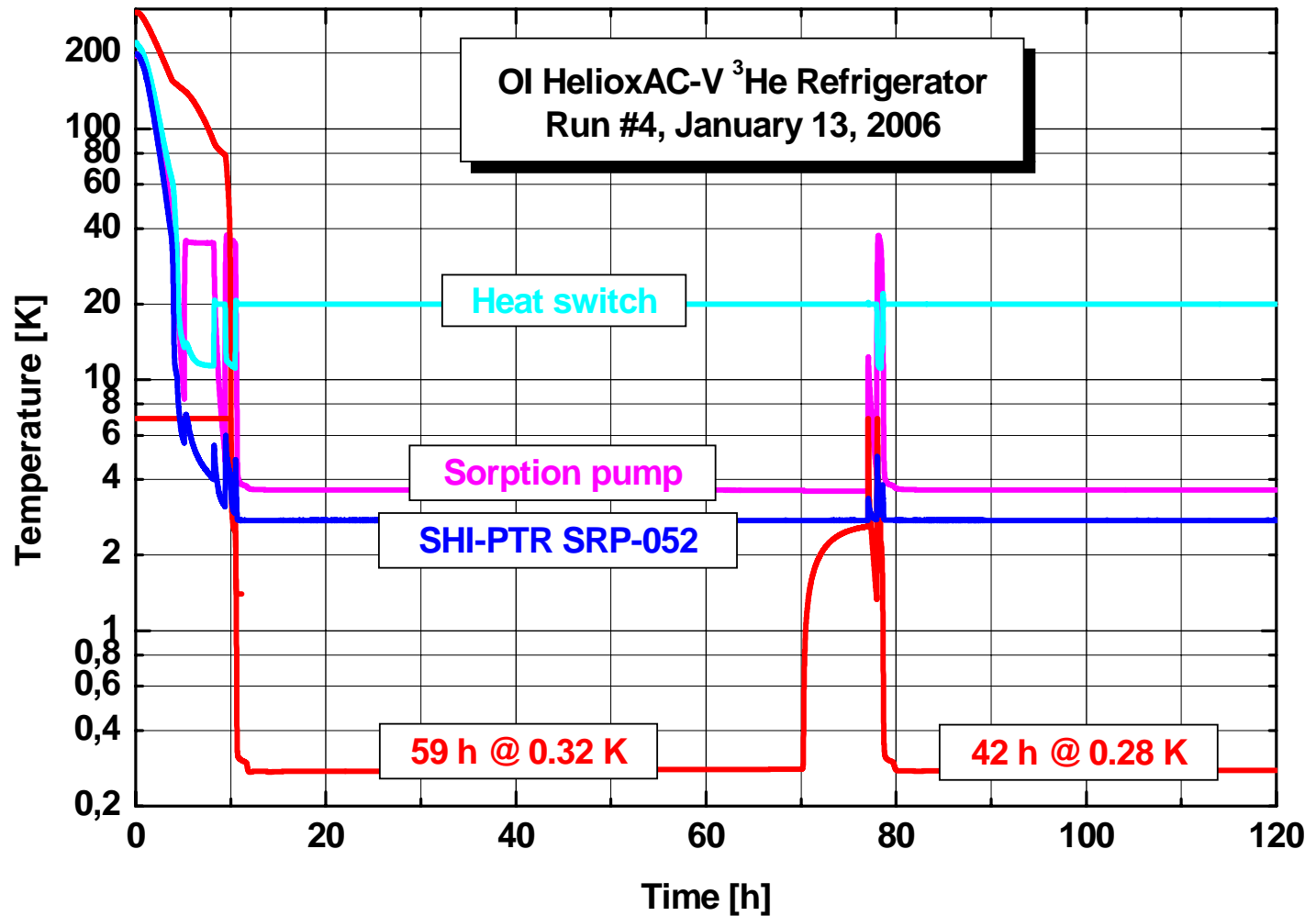
# OI Heliox / SHI-PTR with 3<sup>rd</sup> stage <sup>3</sup>He sorption system

**T = 0.3 K ... 325 K**

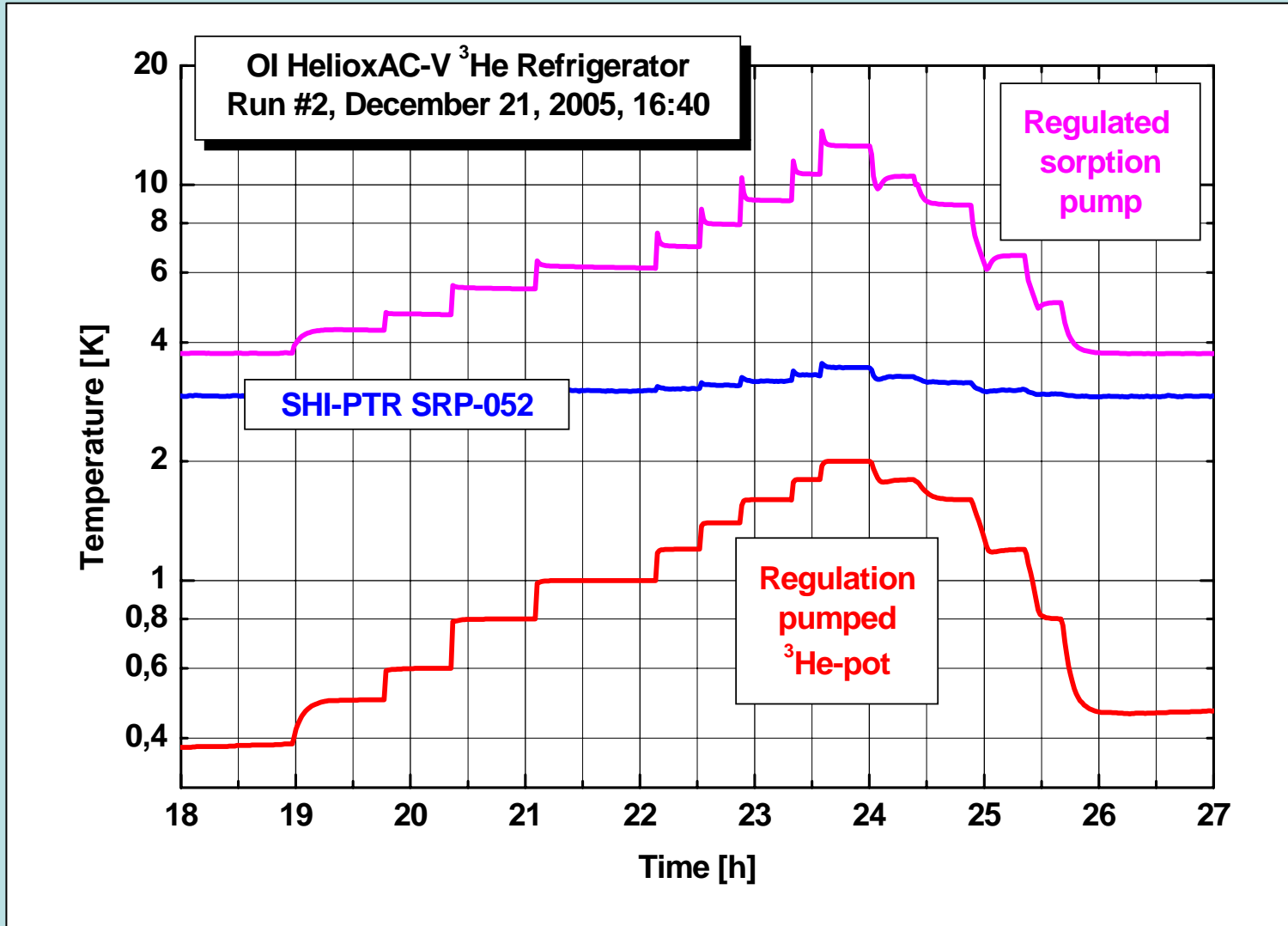




# Cool-down and minimum temperature performance



# Performance of temperature regulation at $T = 0.4 \text{ K} \dots 2 \text{ K}$

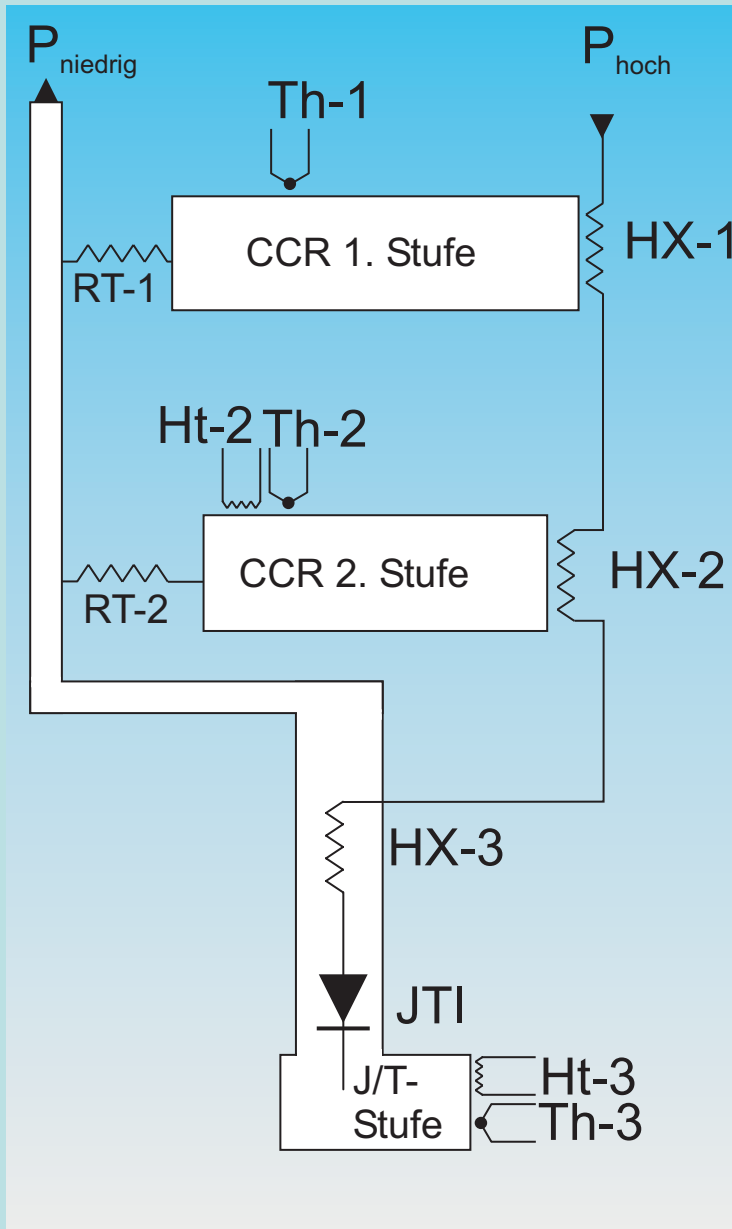


## Example 3

CCR plus J/T-stage

3.1: ARS / ILL  $\rightarrow$   $^4\text{He}$

3.2: SHI / HMI  $\rightarrow$   $^4\text{He}$  or  $^3\text{He}$

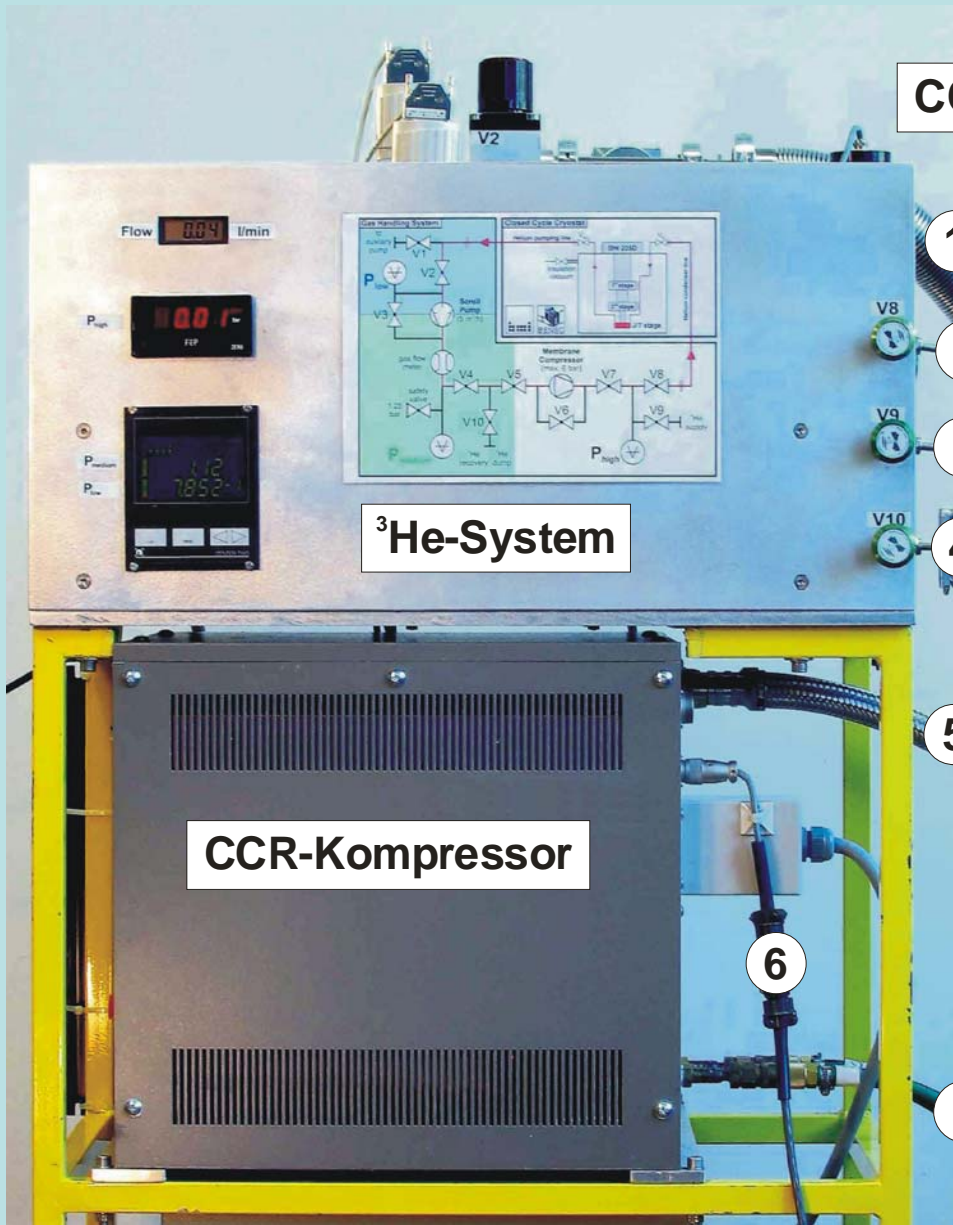


### HMI diploma thesis (2005)

- Bastian Klemke
- SHI RDK-205 +  $^3\text{He}$ -JT
- 0.7 K on n-diffractometer

### ARS & ILL co-op. (2004)

- DE-202 +  $^4\text{He}$ -JT
- 1,7 K in 6-circle goniom.
- 50.000 €



**<sup>4</sup>He-Betrieb**

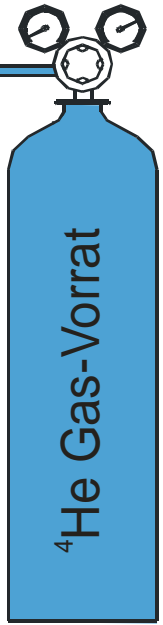
$P_{\text{niedrig}} = \text{0,1 ... 1 mbar}$

$P_{\text{hoch}} = \text{1 ... 6 bar}$

Scroll-  
pumpe

SHI-205-D

Membran-  
kompressor



<sup>3</sup>He Gas-Vorrat

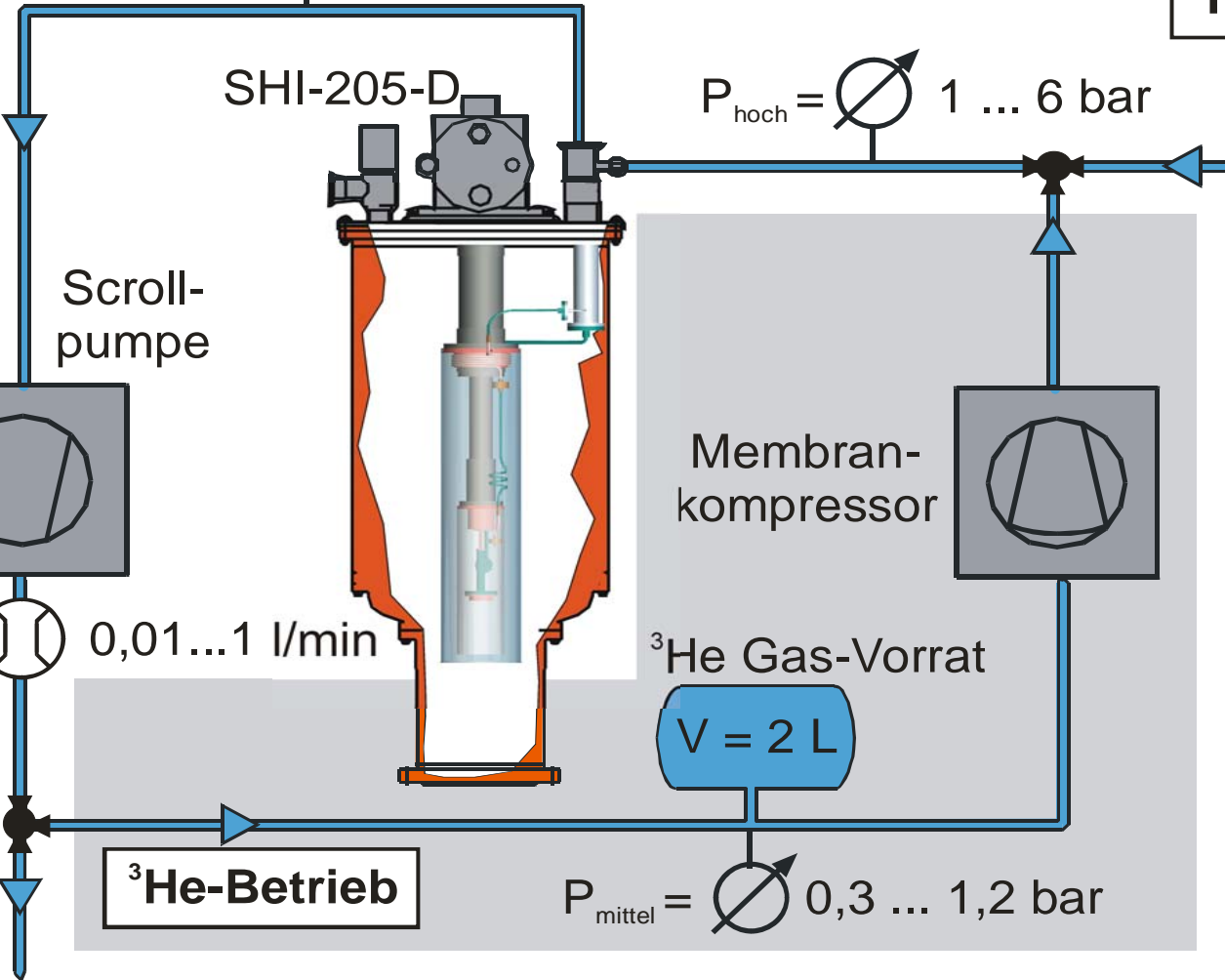
$V = 2 \text{ L}$

**<sup>3</sup>He-Betrieb**

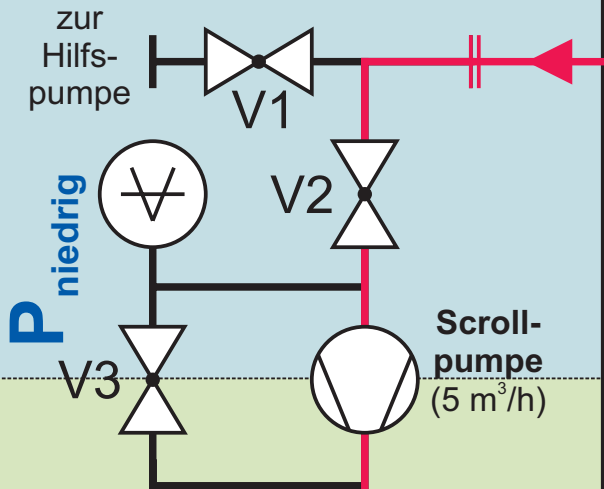
$P_{\text{mittel}} = \text{0,3 ... 1,2 bar}$

$\dot{V} = \text{0,01...1 l/min}$

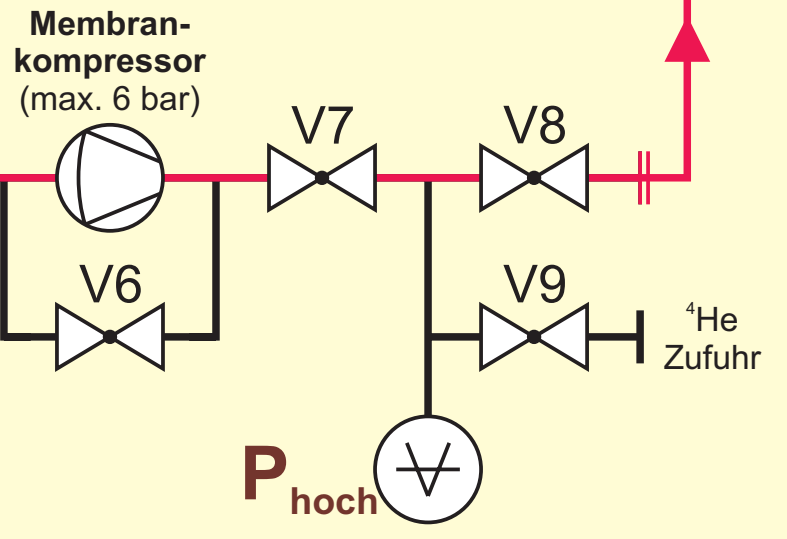
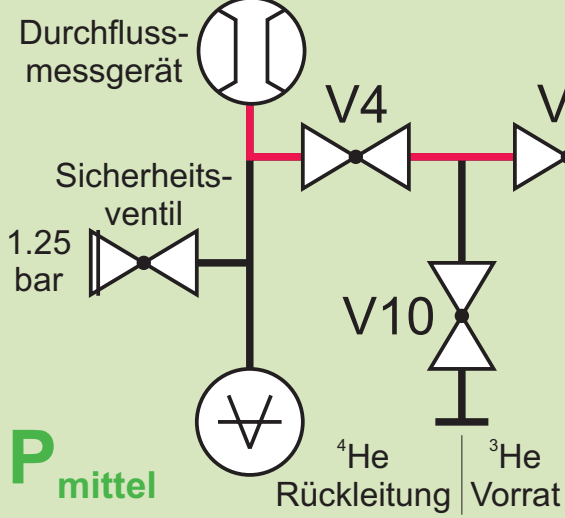
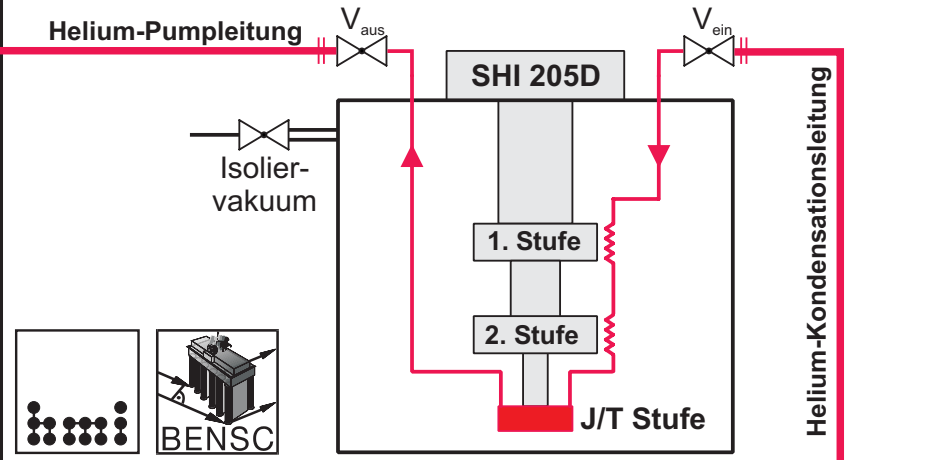
<sup>4</sup>He  
Rückleitung



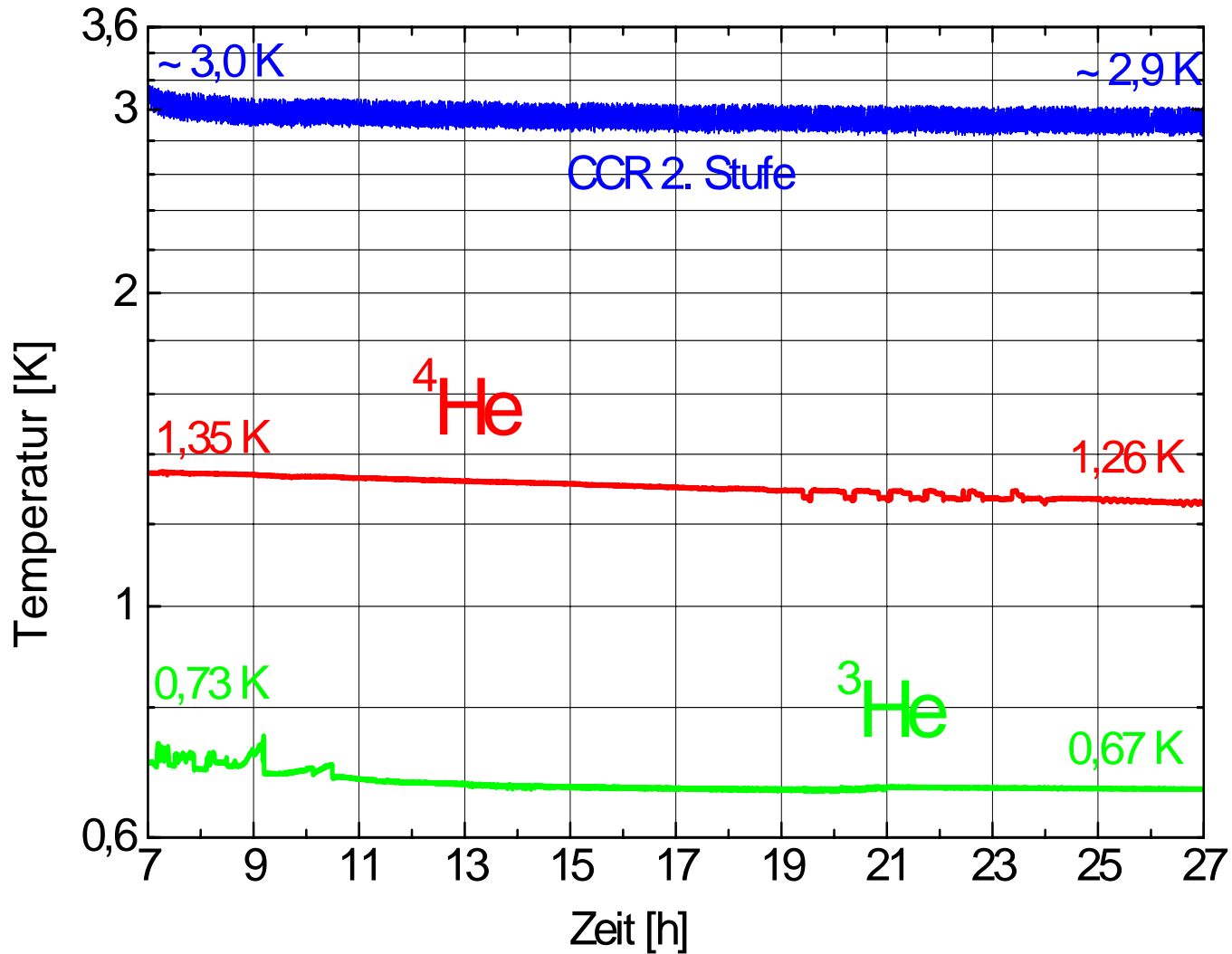
### Gas-Handling-System



### Closed-Cycle Kryostat



# Minimum temperature performance





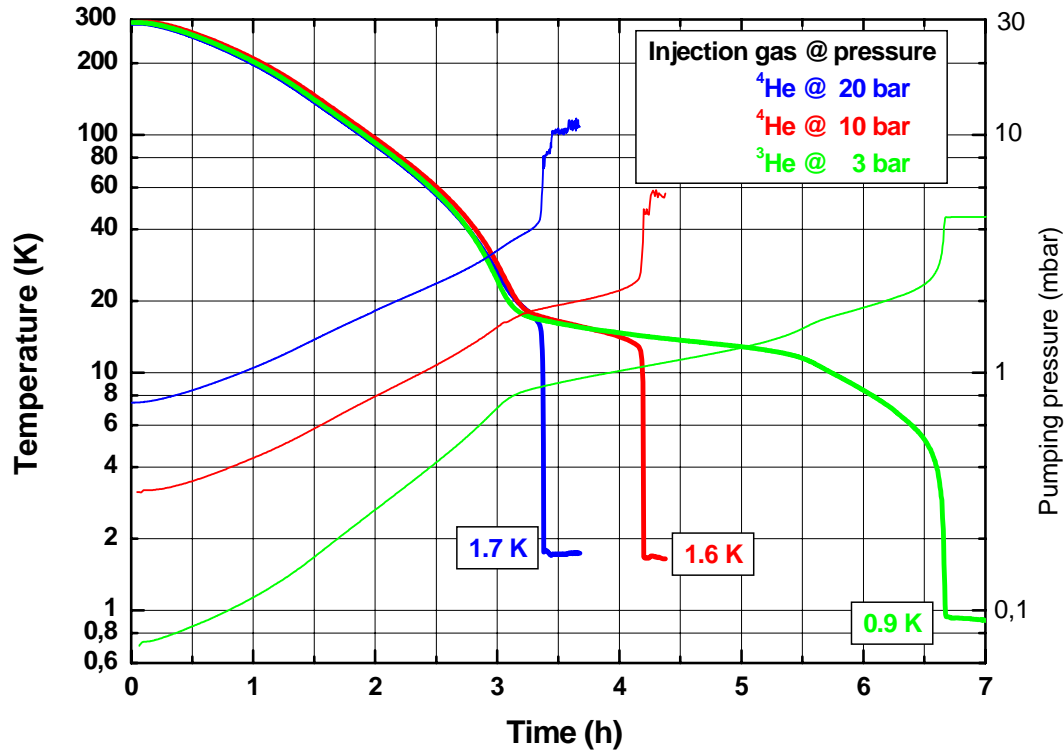
# ARS DE-202 with $^4\text{He}$ -J/T as 3<sup>rd</sup> stage

Delivered July 2006 for HMI's diffraction instrument MAGS at synchrotron beamline (BESSY)

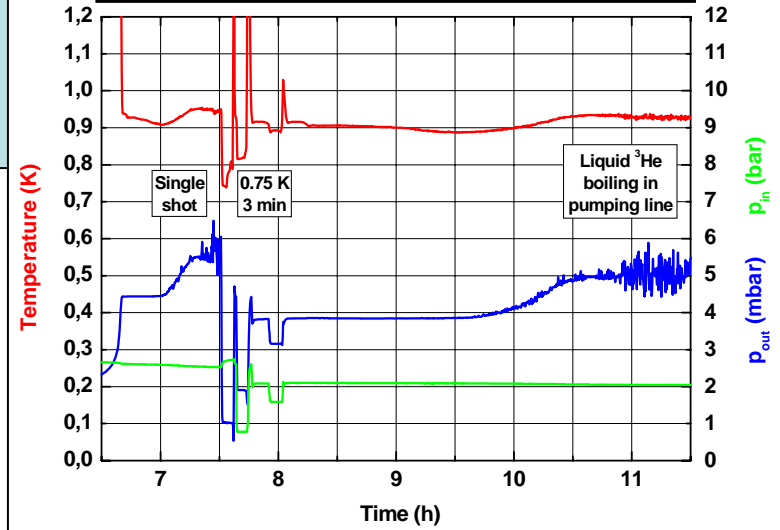


# Performance at low temperature

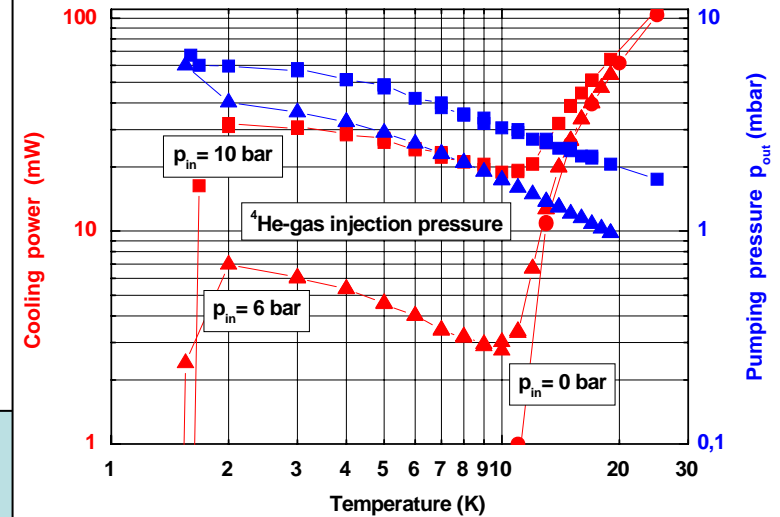
Cool-down of ARS-CCR DE-202 with J/T-stage



Min. temperature of ARS-CCR DE-202 with  $^3\text{He}$  in J/T-stage



ARS-CCR DE-202 with  $^4\text{He}$  in J/T stage



## Example 4

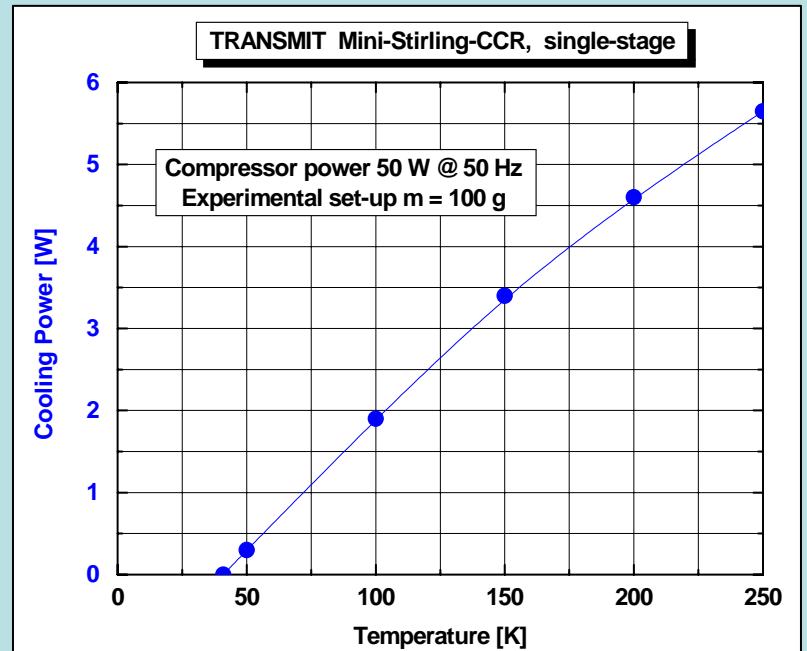
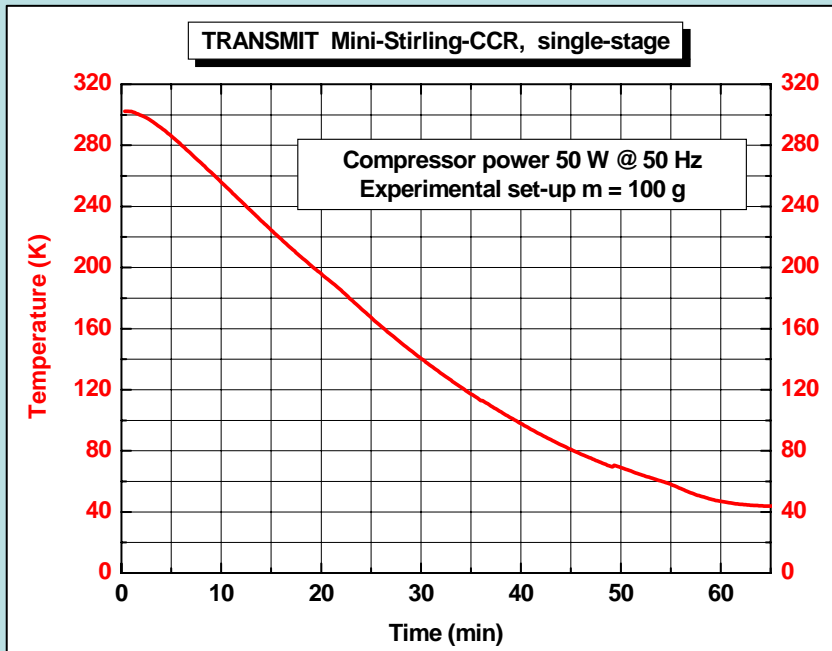
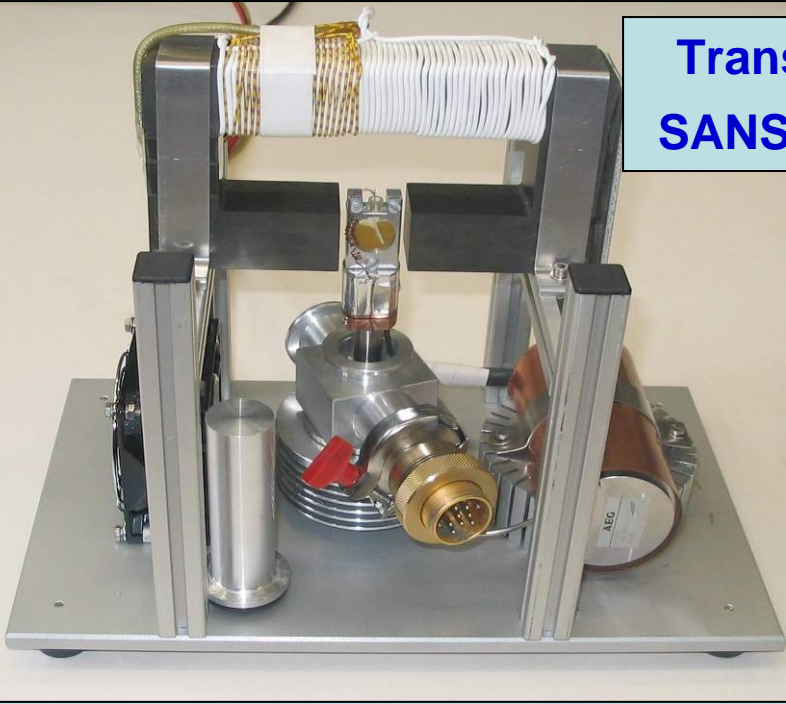
4.1: TransMIT Stirling Refrigerator

4.2: TransMIT Pulstube Refrigerator

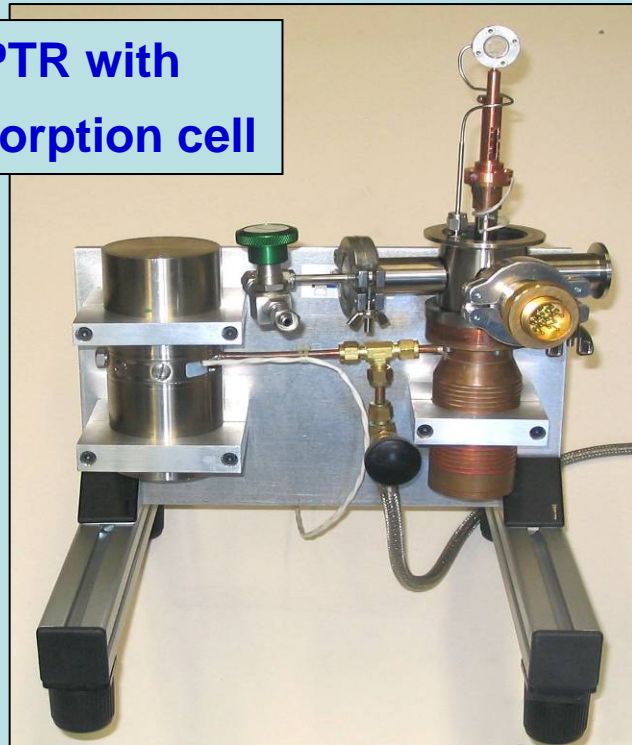
**HMI-BENSC**

**also → Sun Power, Air Liquide, ...**

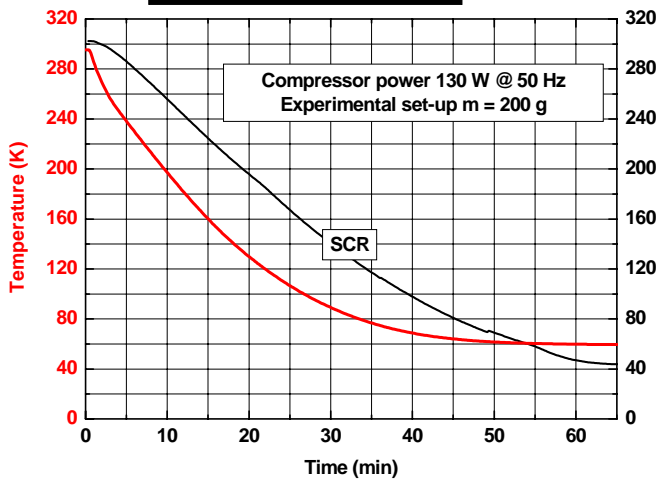
# TransMIT Stirlingmotor SANS 10 kHz AC magnet



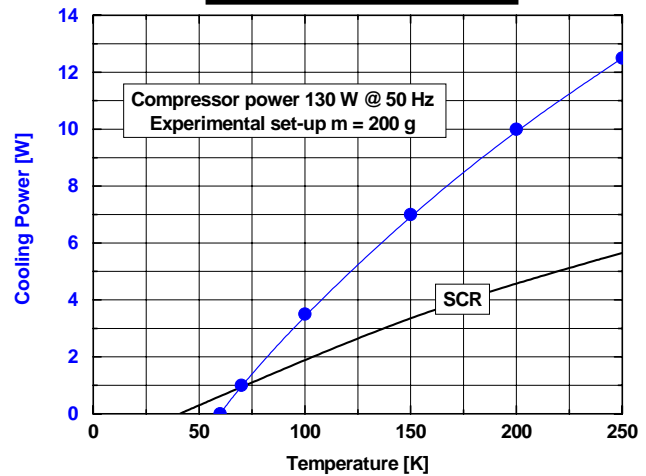
# TransMIT PTR with SANS gas adsorption cell



TransMIT Mini-PTR, single-stage



TransMIT Mini-PTR, single-stage



# Refrigerator cryostats

**-performance in beamline experiments –**

**T-range low: 325 K → 2.5 K → 1.4 K (<sup>4</sup>He) → 0.3 K (<sup>3</sup>He)**

**T-range high: 4 K → 600 K ... 800 K**

**T-regulation &  $\Delta T$ -stability: within LS-340 quality**

**Cooling power: ~500 g in 1 h with CCR of ~1 W @ 4 K**

**CCR or PTR: PTR vibrations are smoother;**

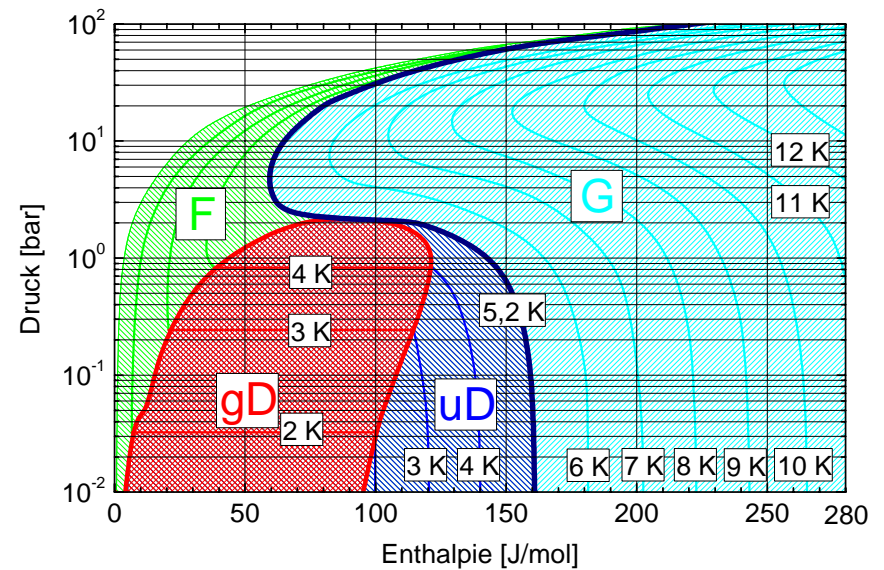
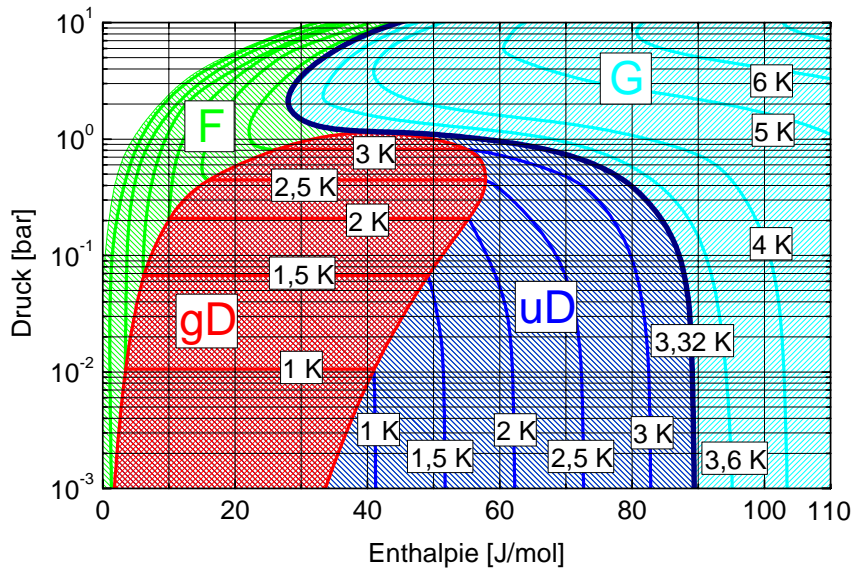
**Temps lower → <sup>4</sup>He: 2.2 K and <sup>3</sup>He: 1.3 K !!!**

**Finis**

# Pressure – Enthalpy – Diagram

$^3\text{He}$  (CP: 3,3 K / 1 bar)

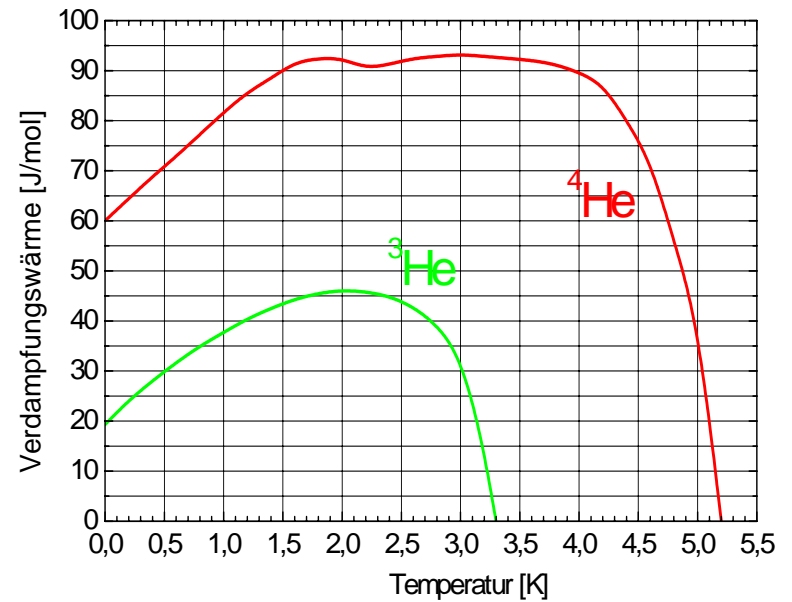
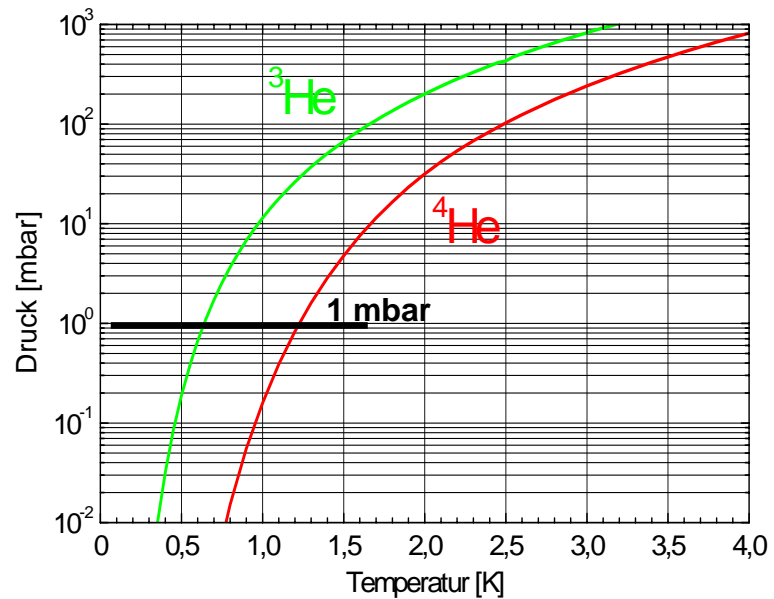
$^4\text{He}$  (CP: 5,2 K / 2 bar)





## Vapor pressure

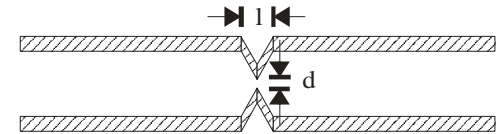
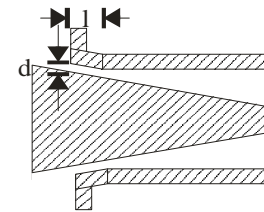
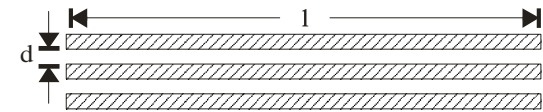
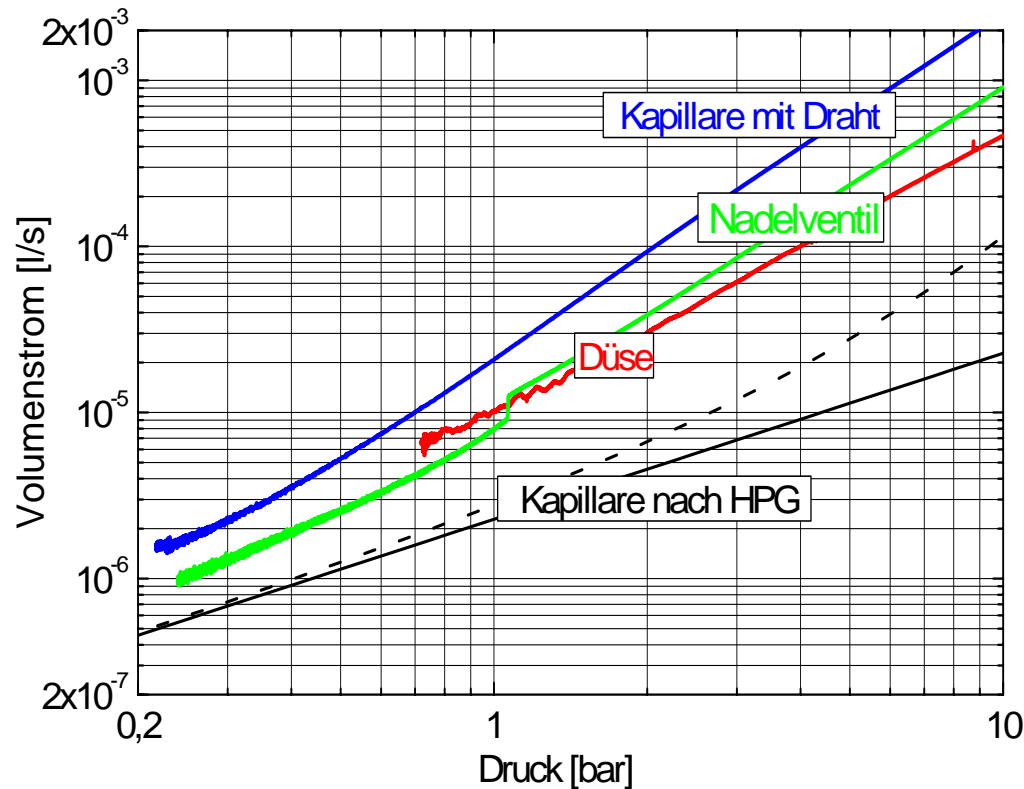
## Latent heat



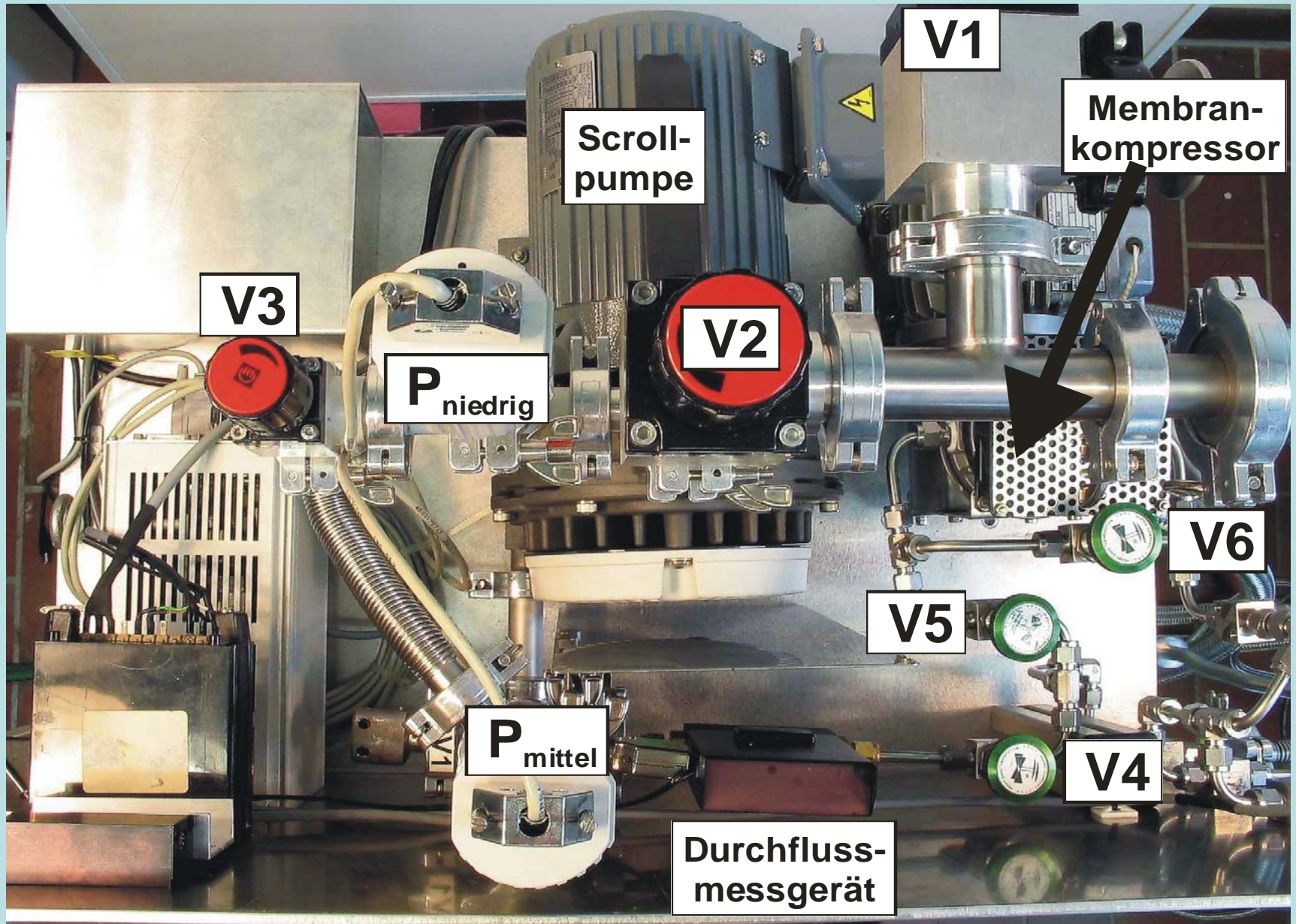
$p \sim 1 \text{ mbar}$ :  $T \sim 1,2 \text{ K}$  bzw.  $0,6 \text{ K}$

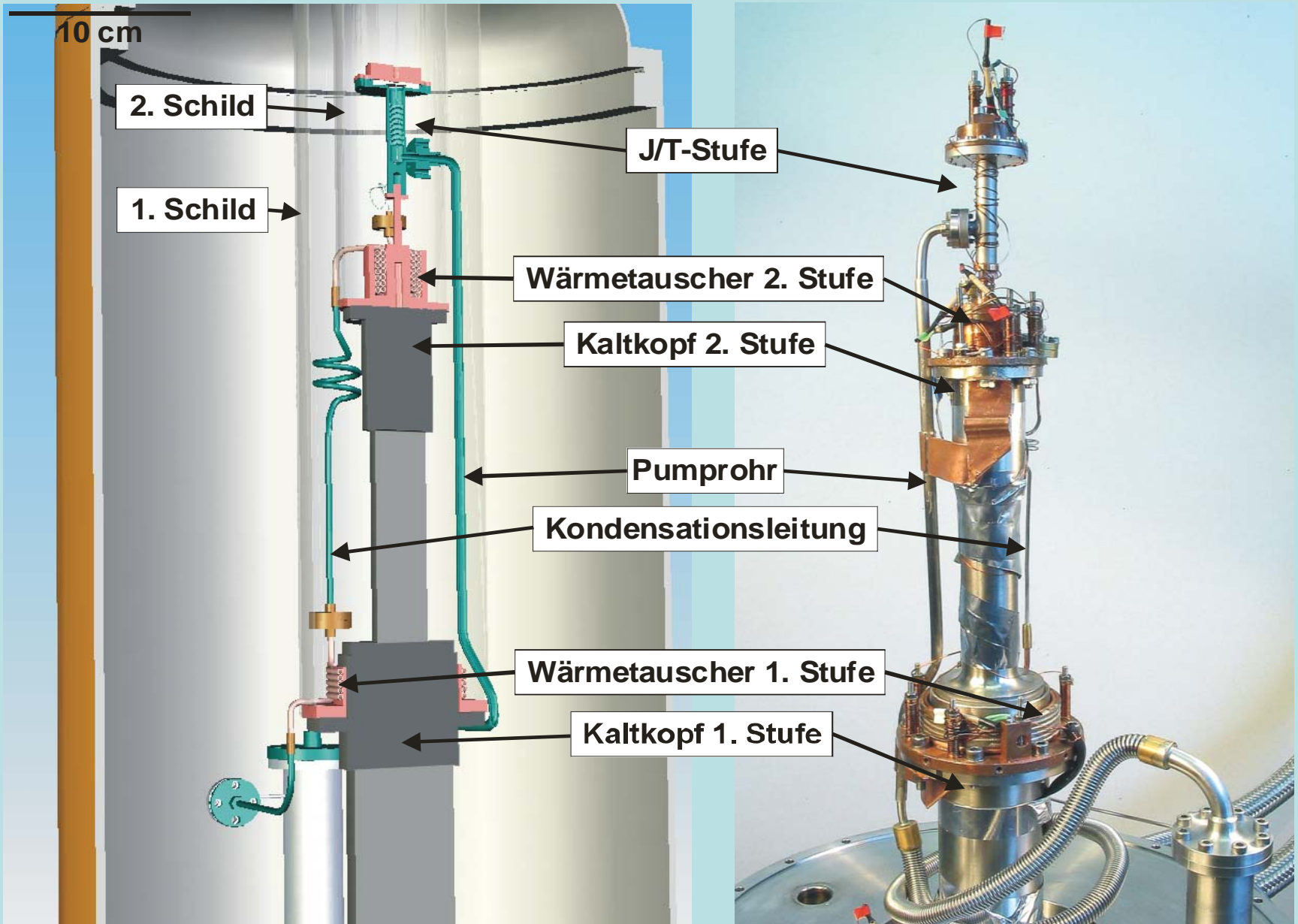
$\Delta V/\Delta t \sim 10^{-4} \text{ mol/s} \rightarrow P_L \sim 5 \dots 10 \text{ mW}$

# Gas flow trough 3 types of J/T-valves

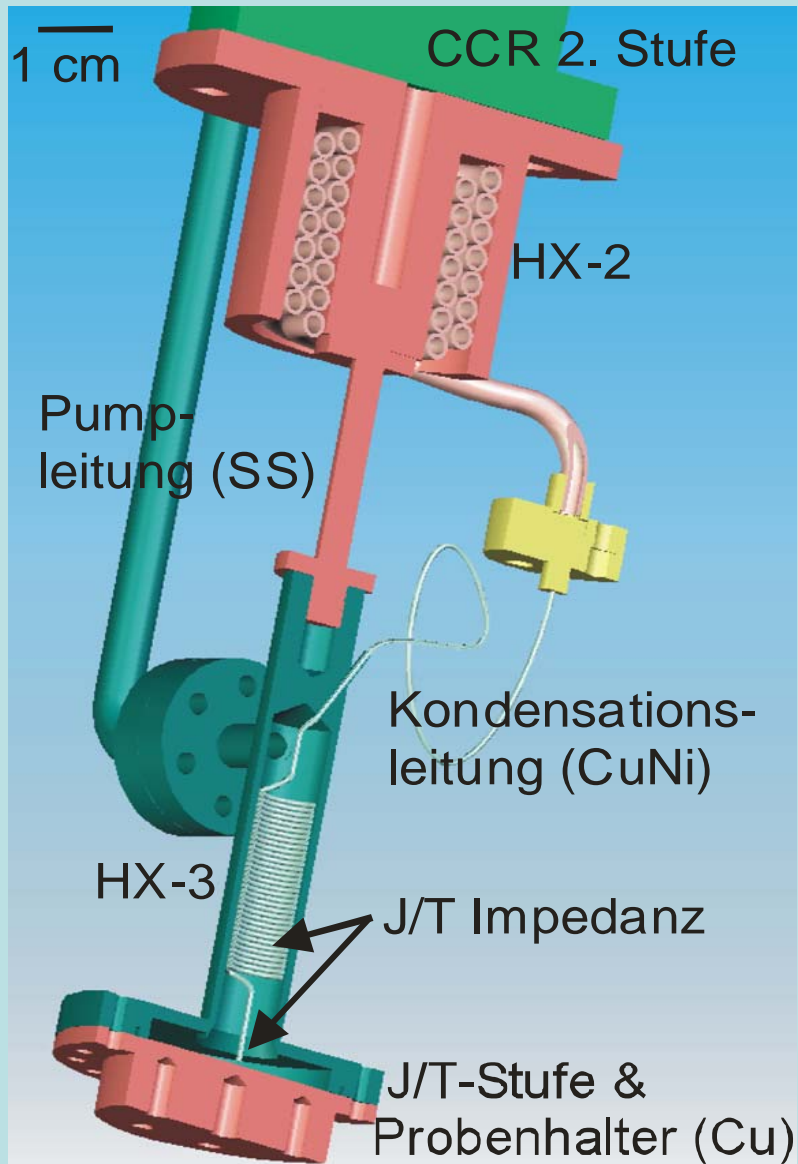


Viscous flow:  $\Delta V/\Delta t = \Delta p \pi R^4 / 8 \eta L$ ; Expansion of capillary:  $R = R_0 (1 + 3 \cdot 10^{-3} \Delta p)$

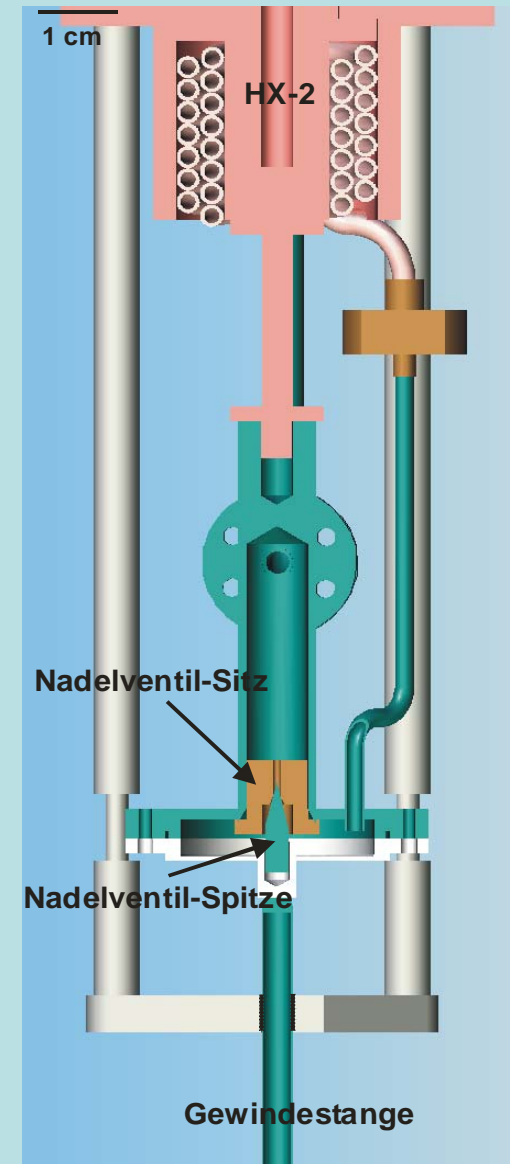




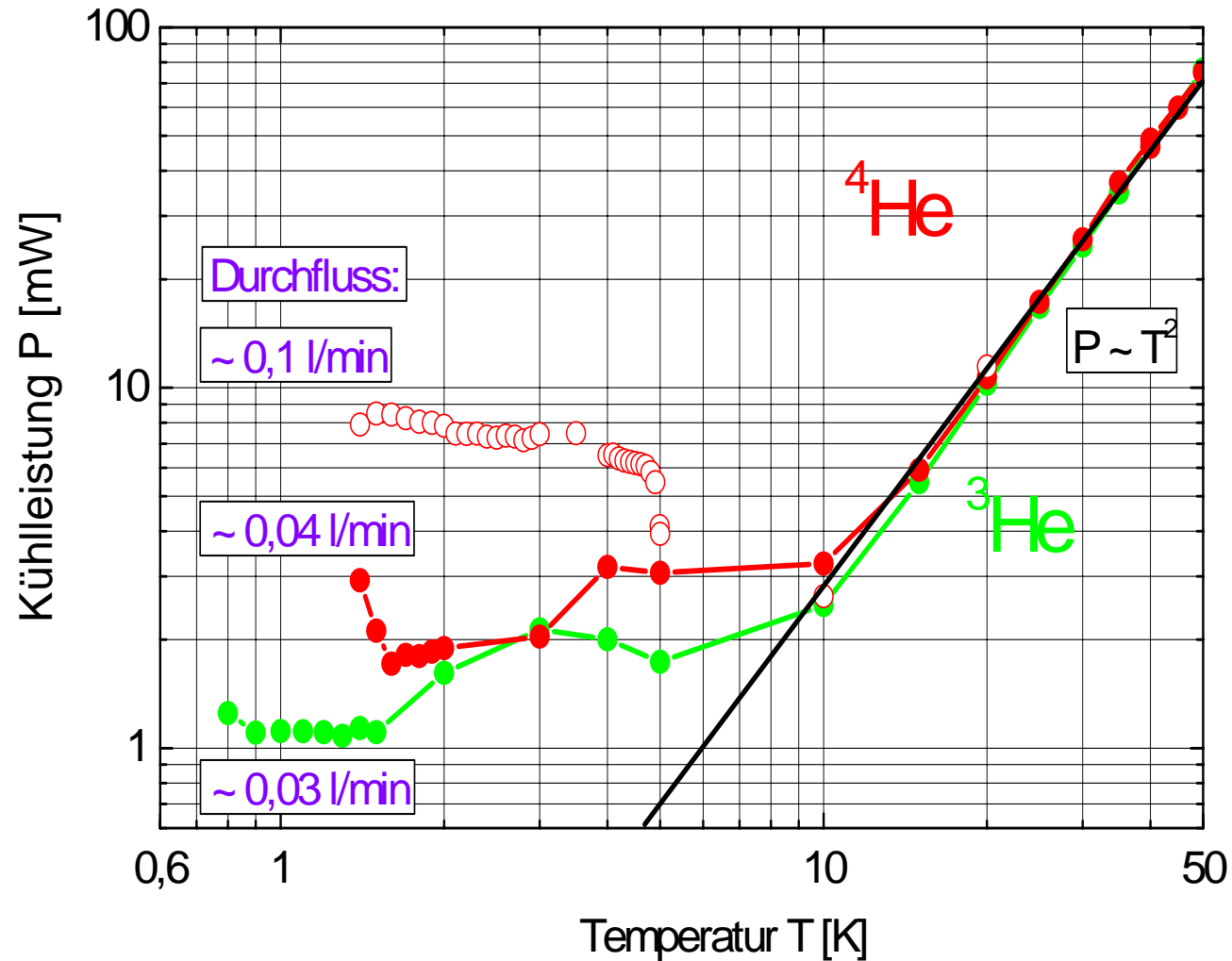
## Design J/T-stage and LHe-chamber



## Design of needle valve



# Cooling power of J/T-stage with different flow



# PID-controlled temperatures $\Delta T / T_0 < 0,1 \%$ with $\tau < 1 \dots 5$ min

