# RJM – Beaumont SO2 – Control Processes

### **Presented By Will Goss**

**Prepared 7/21/03** 



### Wet Scrubbing – SO2 Control

- Early Technologies (Wet)
  - Pulp & Paper (Caustic)
  - Boilers (Limestone)
  - Boilers (Soda Ash)
- Later Technologies
  - Spray Dryers (Semi-Dry)
  - Reactors (Semi-Dry)
  - Flash Dryers (Semi-Dry)







### Wet Scrubbing Systems

### Limestone Chemistry (Wet Systems)

 $\begin{array}{rcl} CaCO_3 + CO_2 + H_2O \rightarrow & Ca(HCO_3)_2 (aq) \\ Ca(HCO_3)_2 + 2SO_2 \rightarrow & Ca(HSO_3)_2 + 2CO_2 \\ Ca(HSO_3)_2 + O_2 \rightarrow & CaSO_4 + H_2SO_4 & (oxidation) \\ H_2SO_4 + CaCO_3 \rightarrow & CaSO_4 + CO_2 + H_2O \\ CaSO_4 + 2H_2O \rightarrow & CaSO_4 - 2H_2O & (gypsum conton to tot) \\ \end{array}$ 

### **Semi-Dry – Scrubbing Advances**

1978 First Spray Dryers (Disks) Appear 1980 First Nozzle Spray Dryers 1982 Spray Dryer (disk) with Recycle **1988 First Reactors (Incinerators) 1990 DOE Clean Coal Projects** 1992 EPRI Cost Study of Processes 2002 Patents covering Flash Dryer



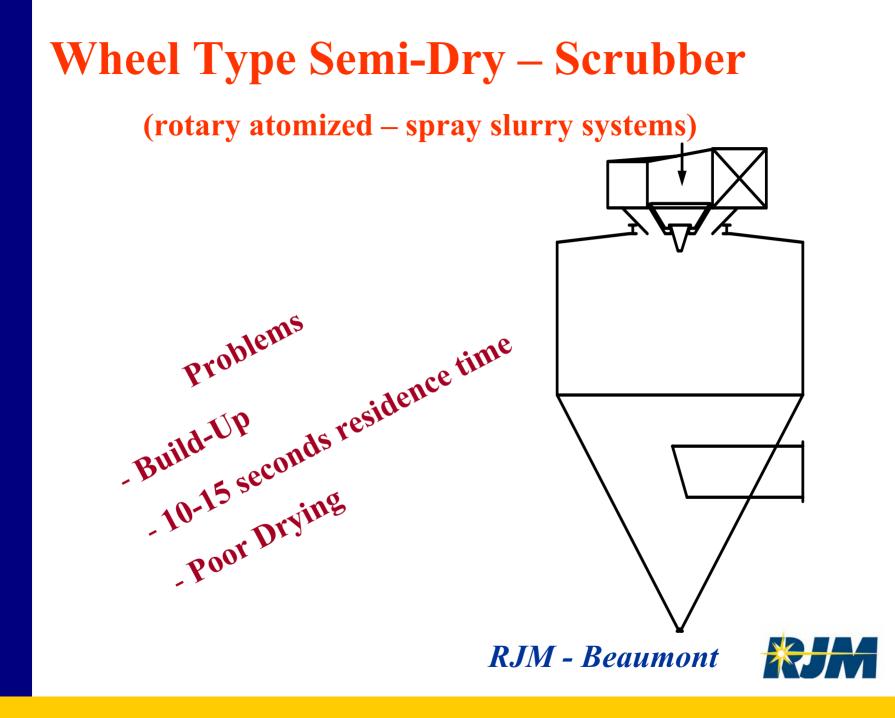
## **Semi-Dry Chemistry**

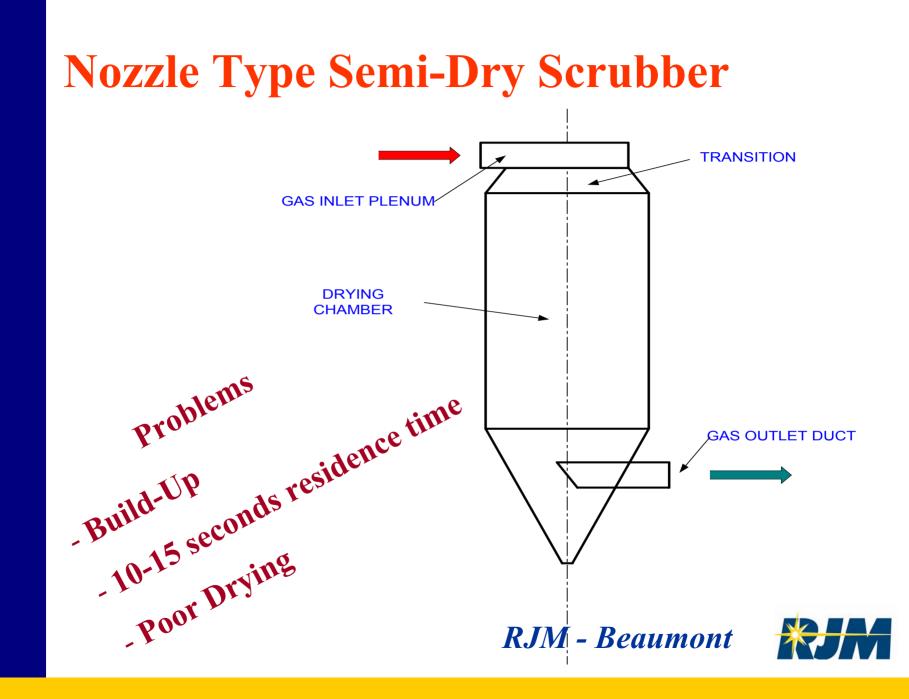
#### (slaking pebble lime)

CaO +  $H_2O$  ----> Ca(OH)<sub>2</sub> Ca(OH)<sub>2</sub> + SO<sub>2</sub> ----> CaSO<sub>3</sub> •  $\frac{1}{2}$  H<sub>2</sub>O +  $\frac{1}{2}$ H<sub>2</sub>O

 $Ca(OH)_2 + SO_3 + H_2O - CaSO_4 \odot 2H_2O$ 







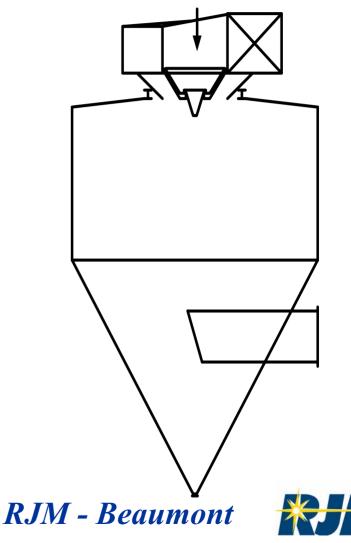
### **Wheel Type Semi-Dry – Scrubber**

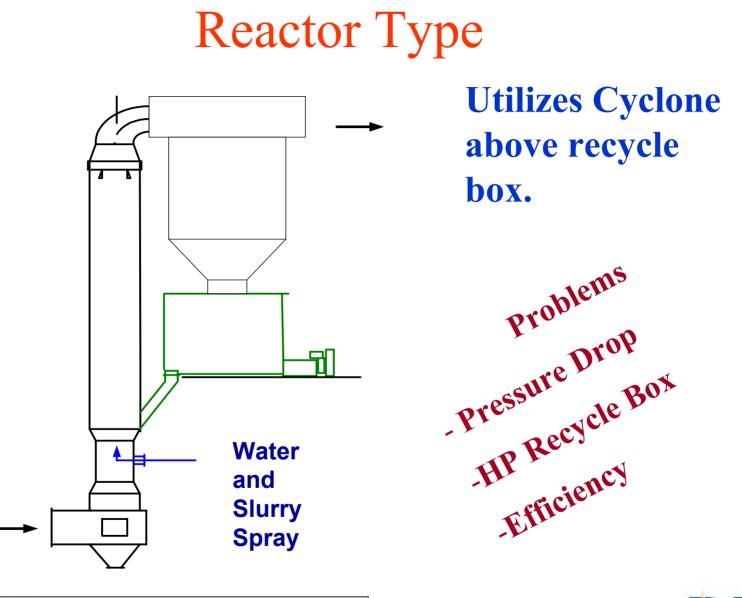
(rotary atomized – spray slurry systems)

**Recycle Added** 

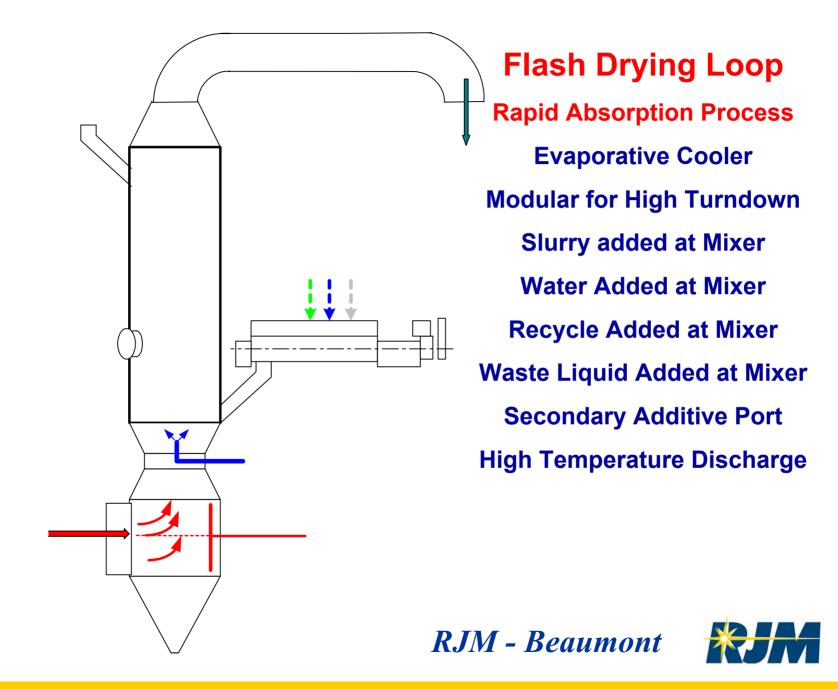
- Able to improve efficiencies
- Able to improve utilization











#### Photo of Semi-Dry Stack at 165 F







## What is Multi-Pollutant Control

- Control for Combustion Processes Typically Boilers,
- Where the System is Selected to Control more than one Pollutant in a Common Vessel,
- Using a Minimum Number of Components,
- That Include the Flexibility to meet Future Requirements,
- In a Cost Effective Design,
- With no Liquid Disposal and,
- Dry Safe Disposal Material





## What to Control?

- Temperature
- H2SO4
- HCl
- SO3
- SO2
- Mercury
- Other Toxic Metals (NESHAP)
- Ash
- Fine Particulate





### **Flash Drying RAP Reactor**

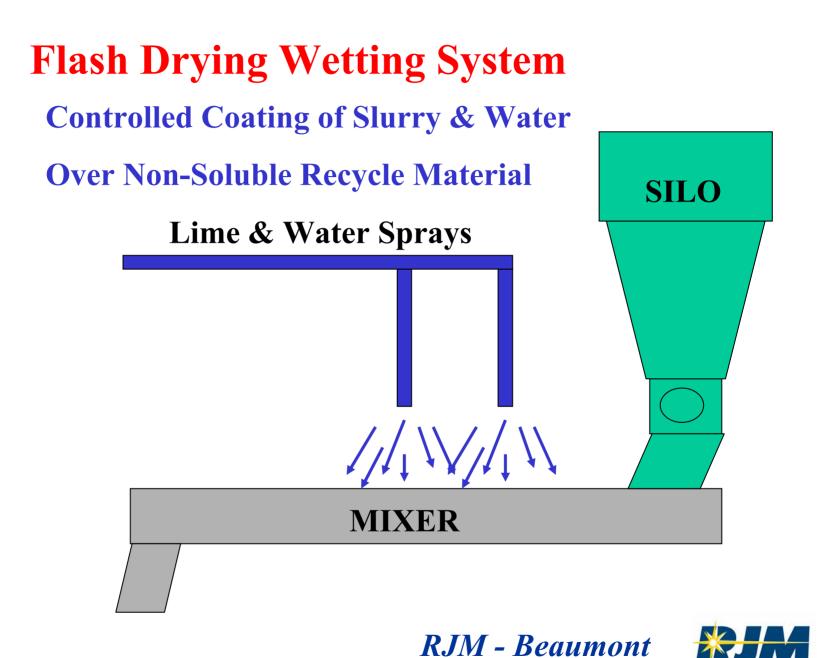
Maximize Surface Area by

- \* Increasing Recycle Rate
- \* Recycling Fines

**The Finely Coated Particles** 

- \* Improved Cooling
- \* Improved Reaction
- \* Decreased Drying Time
- \* Higher Outlet Temperature



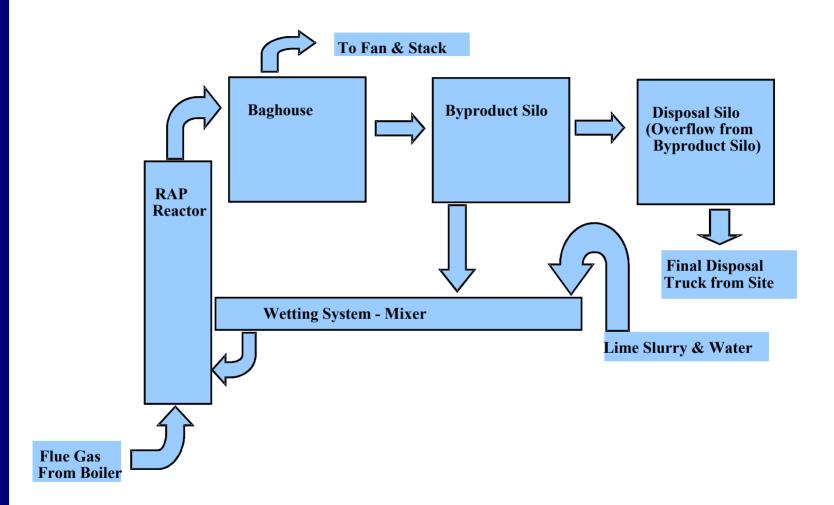








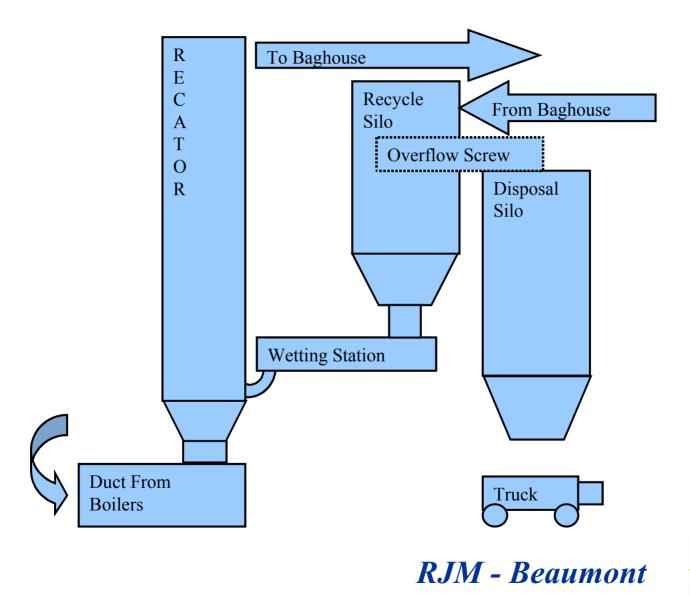
#### **Rap System**



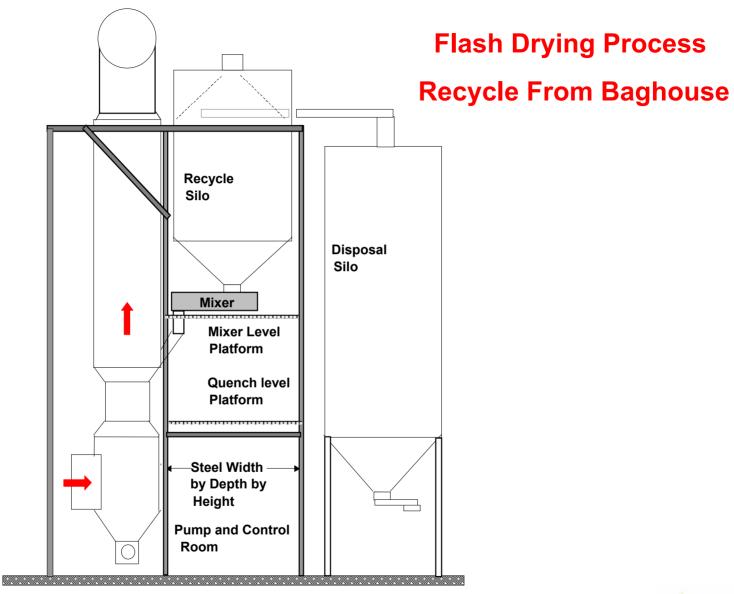




#### **Material Handling**

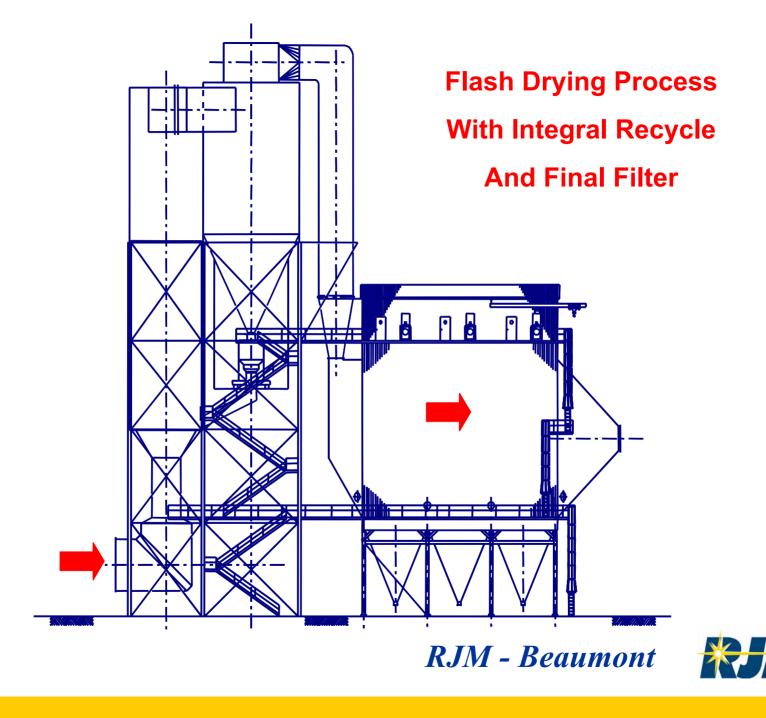














#### RAP Installation

### MCO Coal Fired Boilers





## **Flash Dryer Improvements**

- Maintain -or- Improve
  - Efficiency
  - Utilization
- Eliminate Internal Sprays
- Decrease Overall Height
- Eliminate Separate Recycle Loop
- Lower System Pressure Drop
- Improve Turndown Capability
- Simplify Controls
- Lower Capital Costs
- Reduce Cooling Water Requirements







Lime Silo and Slaker Pre-Wired Pre-Piped





#### **Slurry and Water Pumps**







## **SO2** Control

- 90 to 99% SO2 Removal
- High Outlet Temperature 180 to 200 F
  - Less Potential corrosion
  - Reduces need for Reheat
  - Eliminates Special Chimney Liners

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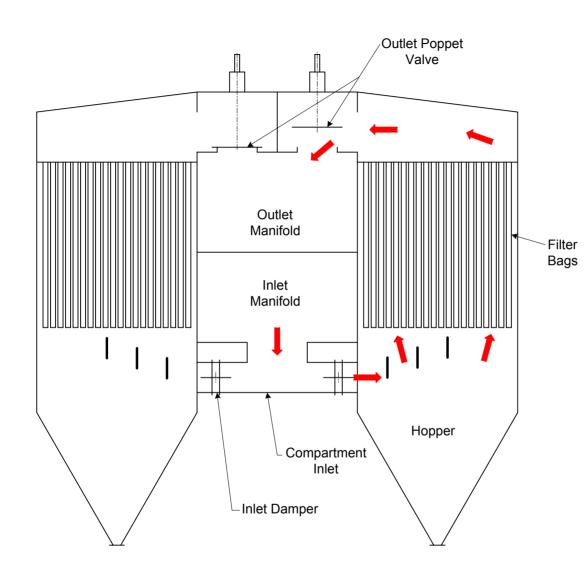
- High Utilization
- Requires Smaller Footprint
- Requires Less Power



## **Particulate Control**

- For Multi-Pollutant Control a Pulse type Filter is recommended
- Filter should be designed for Recycle with High Inlet Grain Loadings
- Shorter Bags, Wider Spacing and Enhanced Cleaning Controls
- Use of Electro-Pulse will improve Fine Particulate Collection, Bag Life and Operating Pressure Drop

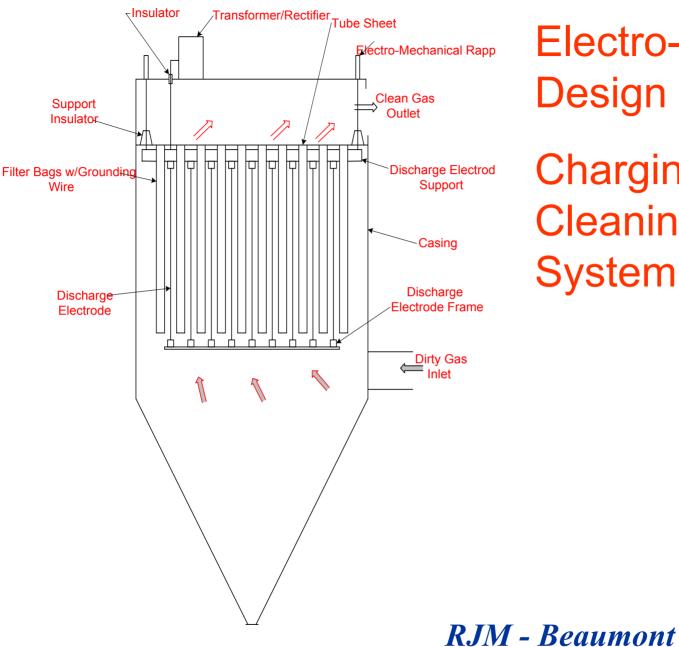




Pulse System Design & Cleaning System







**Electro-Pulse** Design Charging& Cleaning **System** 

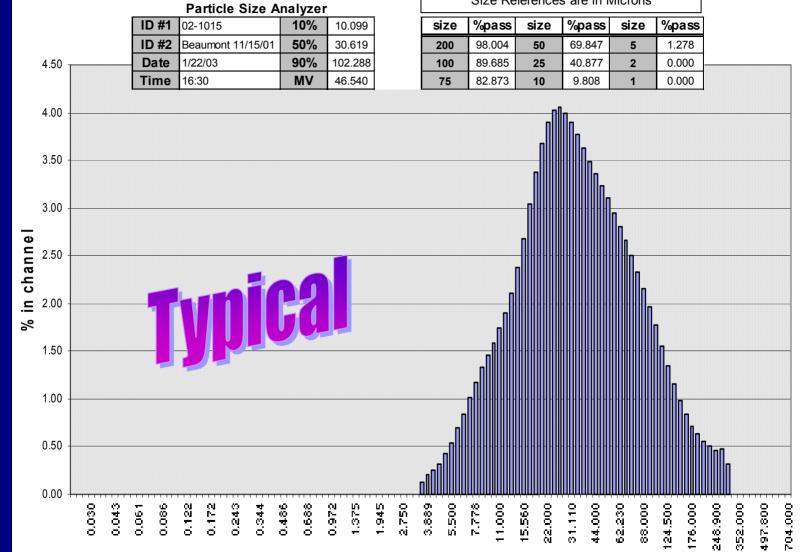




#### Beaumont Environmental Systems Medical College of Ohio

Sample 11/15/01

Size References are in Microns





## **Byproduct Material**

- •Material is Dry allowing Transport and Use
- •Material Does Not Leach Easy Disposal
- •Material Can be Utilized for Fill
- •Material can be integrated into byproduct building materials if no waste disposal is available



### Capital & Costs USA Pricing

- Typical 80 to 150 MWe (and up as modules) Turnkey
  - \$35 / KW For Flash Drying System \$40 / KW For Pulse Type Fabric Filter
  - \$400 / Ton SO2 for <1% Sulfur Coal</p>
  - \$200 / Ton SO2 for <3% Sulfur Coal</p>
- Below 80 MWe Capital Costs Will Rise

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• Above 150 MWe Capital Costs Fall



### **End of Presentation**

#### **Thank You**



