FINAL REPORT -PHOTOASSISTED ELECTRON TRANSFER REACTIONS -BERKELEY PIT WATER

MINE WASTE TECHNOLOGY PROGRAM ACTIVITY IV, PROJECT 3B

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Mine Waste Technology Program Activity IV, Project 3B

Foreward

Industries are attempting to develop and modify their existing operations to manufacture products with environmentally-safe technologies. Wastes generated by these industries are often unsightly and can threaten public health as well as degrade the environment, especially if they are left untreated or are improperly treated. Mine wastes are particularly suspect because of the presence of "mobile toxic constituents" such as, for examples, cyanide that remains in tailings ponds and heap leach pads or acid mine drainage that contains heavy metals leached from sulfide minerals in exposed ore bodies.

The U.S. Environmental Protection Agency (U.S. EPA) is charged by Congress with protecting the nation's land, air, and water resources. Under mandate of national environmental laws, the U.S. EPA strives to formulate and implement actions leading to a balance between human activities and nature's ability to support and nuture life. Such laws direct the U.S. EPA to define environmental problems and thereby perform research, measure impacts, and find solutions. In this regard, the U.S. EPA's National Risk Management Research Laboratory (NRMRL) is responsible for planning, implementing, and managing research, development and demonstration programs to provide an authoritative and defensible engineering basis in support of the U.S. EPA's policies, programs and regulations with respect to drinking water, wastewater, pesticides, toxic substances, solid and hazardous wastes, and Superfund-related activities.

Similar responsibilities have also been assigned to the U.S. Deparment of Energy (U.S. DOE) through the Pittsburg Energy Technology Center (PETC), one of several U.S. DOE centers in charge of planning, implementing, and managing research and development programs. In June 1991, an Interagency Agreement was signed between U.S. EPA and U.S. DOE, IAG No. DW89935117-01-0, which made funds available to support the Western Environmental Technology Office (WETO) and their operating contractor, MSE Technology Applications, Inc. (MSE-TA), as well as Montana Tech of The University of Montana (Montana Tech) for the development of the Mine Waste Technology Program (MWTP).

The MWTP serves as a telecommunication and technology transfer center for the training and education of students (kindergarten through college) and professionals (K-12 teachers through mining representatives), a communication link that is vital to the general public's undertsanding of the issues surrounding mine wastes and mining-related activities. Also, the MWTP funds projects for researchers to develop, demonstrate and/or implement technologies that solve environmental problems related to mine wastes and mining-related activities. Written reports of the projects are used to inform the user and professional communities and simultaneously complement the technology transfer facet of the MWTP. In this regard, workplans, quality assurance project plans (QAPP), and final reports on quality assurance/quality control (QA/QC) data are standard communications of the MWTP. The ensuing manuscript is a final report for presenting the QA/QC data that was obtained for MWTP Activity IV, Project 3B, "Photoassisted Electron Transfer Reactions of Application to Mine Wastewater Cleanup: Berkeley Pitlake Water." Project objectives were to identify and evaluate

appropriate technologies for using ultraviolet radiation to remediate Berkeley Pitlake Water, an acidmine drainage system which contains dissolved heavy metals toxic to human life, via photooxidation and then to recommend whether follow-up research was needed or not.

Executive Summary

This final report presents QA/QC data obtained for MWTP Activity IV, Project 3B, "Photoassisted Electron Transfer Reactions of Application to Mine Wastewater Cleanup: Berkeley Pitlake Water." Several photoassisted electron transfer reactions were explored for the cleanup of mobile toxic constituents commonly found in mine wastewaters, in particular ferrous (Fe²⁺), manganous (Mn²⁺), arsenate (AsO₄³⁻), and sulfate (SO₄²⁻). Each of these reactions were photo-assisted involving electron transfer with solid photocatalysts and dissolved photosensitizers.

In this study, photo-oxidation experiments of Berkeley Pitlake water were conducted to remediate ferrous, manganous and arsenate ions with anatase (titanium dioxide, TiO₂) and hydrogen peroxide (H_2O_2) which are photochemical that were successfully used and demonstrated for the destruction of free and metal-complexed cyanide in MWTP Activity IV, Projects 3 and 3A (Ref. 1,2). Ferrous and manganous ions are expected to be removed by their oxidation to ferric and manganese(IV) and subsequent precipitation as oxy-hydroxides or other similar compounds. On the other hand, arsenate remediation is expected to occur via adsorption at the precitate surface. In addition, photo-reduction experiments for sulfate remediation were conducted using strong reducing agents of sodium formate (NaCOOH) and hydrazine (H_4N_2) in the absence and presence of the anatase (TiO₂) in hopes of producing sulfide (S²⁻) for the additional remediation of additional mobile toxic constituents such cupric (Cu²⁺), zincic (Zn²⁺), and cadmous (Cd²⁺) cations via their precipitation as sulfide compounds. Research involving sulfate photo-reduction appears to be innovative since no published work on the method could be found. Reaction efficiencies were calculated and compared as remediation percentages for all experiments.

Results show that sulfate photo-reduction does work but, under the conditions examined, is not 100% effective. Photo-reduction the dissolved photochemicals proved to work best with hydrazine and formate yielding 9.2% and 6.7% remediation, respectively. When hydrazine and formate were used simultaneously with anatase, remediation percentages were observed to decrease to 5.4% and 2.9%, respectively. Anatase, by itself, only yielded 2.3% remediation. Consequently, it is concluded that the presence of anatase, as a solid photocatalyst, with either hydrazine or formate, as dissolved photochemicals, is detrimental to the homogeneous photolysis processes. Although sulfide formation was never observed, it is clear that photo-reduction of sulfate is possible with both homogeneous photolysis and heterogeneous photocatalysis. These promising technologies should therefore be examined in more detail in the near future.

By comparison, ferrous photo-oxidation could be 100% effective but is dependent on the conditions applied, especially pH. Results indicated that homogeneous photolysis with hydrogen peroxide worked better than heterogeneous photocatalysis with anatase: 28.8% remediation versus 6.1% remediation. Higher dosages of either photochemical yielded only marginal improvement in remediation. Further experiments showed that photolysis with hydrogen peroxide improved with decreasing wavelegth, but was actually best in the absence of UV radiation. This surprising result was attributed to bubbling in

oxygen during the experiments as well as to not adding the photochemical continuously and observing a side reaction for only the UV-assisted experiments. The side reaction was attributed to photo-oxidation of organic species. Oxygen bubbling is believed to have created a mixed potential which lowered the solution potential (E_H) in the experiments below the potential required for manganous oxidation to occur. In this regard, manganous concentrations were not observed to change and its measurement was therefore removed from the critical list. Unfortunately, the selected pH condition of 3 was too low to observe adequate ferrous remediation. Iron concentrations in solution therefore remained high and interfered with the arsenic concentration measurement. In this regard, arsenic concentration was unable to be determined and its measurement was also removed from the critical list. Clearly, this photo-oxidation technology is promising but requires further study especially in regards to delineating the effect of pH, oxygen, contiuous photochemical addition, and wavelength. The remediation of manganese via this technique would establish a process where the pH does not have to be adjusted to pH 11 as with the two-stage lime addition process which is, at this time, the best-determined available technology (BDAT). In this regard, this technique could eliminate the second stage and thereby yield substantial savings of lime.

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Acronyms and Abbreviations

А	acceptors
D	donors
EPA	U.S. Environmental Protection Agency
g/L	grams per liter
IC	ion chromatograph
ICP	inductively-coupled plasma
Μ	mole
ml	milliliter
Montana Tech	Montana Tech of the University of Montana
MWTP	Mine Waste Technology Program
nm	Nanometers
ppm	Parts per million
QA/QC	quality assurance/ quality control
S	photosensitizers
UV	Ultraviolet

1. INTRODUCTION

This final report was prepared from technical information and validated Quality Assurance/Quality Control (QA/QC) results obtained from Berkeley Pitlake water samples treated experimentally at Montana Tech of The University of Montana (Montana Tech) in Butte, Montana, for the Mine Waste Technology Program (MWTP), Activity IV, Project 3B - "Photoassisted Electron Transfer Reactions of Application to Mine Wastewater Cleanup: Berkeley Pitlake Water." All enclosed materials are follow-up to the approved MWTP Activity IV, Project 3B, Work Plan and Quality Assurance Project Plan (QAPP) dated June 1995 and May 1996, respectively (Ref. 3,4). The information and results are described in accordance with the requirements of the Interagency Agreement (IAG) Activity IV Scope of Work which was signed in June 1991 by the U.S. Environmental Protection Agency (U.S. EPA) and the U.S. Department of Energy (U.S. DOE) to initiate work on the MWTP. Furthermore, this MWTP final report addresses the testing and evaluation of a promising photolytic technologies for the remediation of mobile toxic constituents in mine wastewaters identified in MWTP Activity I Prioritization Reports (Ref. 5), Water and Acid Drainage.

1.1 Relevance to MWTP

Discharge waters from various municipal and industrial operations transport many dissolved chemicals that may have adverse effects on the environment of both plant and animal life. For example, dissolved chemicals may leach various heavy metals which would otherwise remain immobile. Aquatic life of all sorts can become sick or die due to the toxicity of both the dissolved chemicals and metals. Many wastewater processing technologies that are currently available or being developed consequently emphasize the removal of the dissolved chemicals as well as the heavy metals from the discharge waters. The remediation of the discharge waters has been considered paramount at several locations in Montana and throughout the United States (Ref. 5).

Impetus for this study emanated from the previous and successful studies on free and metal-complexed cyanide (Ref. 1,2) and from fundamental interests regarding the interaction of UV radiation (i.e. sunlight) with acid mine drainage systems such as the Berkeley Pitlake (Ref. 6). Further impetus comes from concerns of citizens near sites contaminated with acid mine drainage such as ARCO's and MRI's Berkeley Pitlake in Butte, Montana, where residents are concerned about the contamination entering their drinking (well) water especially after the Berkeley Pitlake reaches the critical water level. Similar problems have been noted for other sites in Montana and the United States (Ref. 5). In summary, photolytic technologies have been examined in this study and results are discussed in this final report for remediating Berkeley Pitlake water.

A Record of Decision (ROD) has been made which stipulates that lime precipitation is the Best Demonstrated Available Technology (BDAT) for remediating Berkeley Pitlake water (Ref. 7). However, because the critical water level of the Berkeley Pitlake will not be reached until 2021, the ROD also stated that a treatment plant did not have to operating until 2017 with construction beginning in 2013. This means there is over 15 years in which a better technology can be determined. In this regard, a plethora of technologies have been and are presently being examined by the MWTP as part of Activity IV, Project 7 (Ref. 8). These technologies include The High Density Solids (HDSTM) Process by Tetra Technologies, Inc. (Ref. 9), a silica gel chelation process by Purity Systems, Inc., (Ref. 10), an ion exchange process by Technical Assistance International, Inc., in conjunction with The Group of Russian Scientists (Ref. 11), a biosorption process with *Azolla* biofilter by SPC International and Hebrew University of Jerusalem (Ref. 12), and The Green PrecipitateTM Process by Geo2 Limited (Ref. 13). Because one of the goals of this study was to develop a photolytic process for remediating Berkeley Pitlake water, it was not considered to be a demonstration project and consequently was submitted and later accepted as an Activity IV Project in which technologies are identified and evaluated (see Forward).

1.2 Research Objectives

The major objective of this project is to evaluate the effectiveness of photoassisted remediation of the mobile toxic constituents in the Berkeley Pitlake water, particularly iron and sulfate (as critical measrements) and arsenic and manganese (as non-critical measurements). Because iron and manganese are present in reduced states of +II, their remediation could be accomplished by photooxidation and subsequent precipitation of schwertmannite and pyrolusite, respectively. The photooxidation process would maintain the oxidation state of arsenic +V species and would convert any arsenic +III species to +V. Because arsenic +V species favor adsorption at iron precipitate surfaces, arsenic remediation would likely occur simultaneously with schwertmannite precipitation. On the other hand, because sulfate exists in a highly oxidized state (i.e., sulfur is +IV), its remediation can be accomplished by photo-reduction to sulfide and subsequent precipitation of heavy metal sulfides such as Cu^{2+} , Zn^{2+} and Cd^{2+} . Although somewhat neglible, some sulfate will be removed during schwertmannite precipitation. Through a proper selection of pH or redox (i.e., E_H) conditions, it would be possible to perform photoassisted remediation selectively. Other secondary objectives include examining direct photolysis, homogeneous photolysis, and heterogeneous photocatalysis to show feasibility, compare reaction efficiencies, and determine the effects of UV wavelength, reagent type, and reagent amount.

Because it is known that deep Berkeley Pitlake water (i.e., water taken from 200 feet or more below the surface) contains ferrous ion (Fe²⁺), manganous ion (Mn²⁺), arsenic predominantly as arsenate (AsO₄³⁻), sulfur predominantly as sulfate (SO₄²⁻) and a number of other elements as metallic cations or oxyanions, it will be clear from ensuing discussions in Section 2 that these species can be remediated by photolysis. The questions to be answered include (1) can ferrous be oxidized photolytically (i.e., photo-oxidized) to ferric and thereby induced to precipitate as ferrihydrite, (2) will the reaction be faster than with bubbled and dissolved oxygen as examined in previous studies (Ref. 14), (3) can arsenite photo-oxidize to arsenate simultaneously, (4) will resulting ferrihydrite precipitate adsorb, (5) will manganese behave similarly and thereby photooxidize to Mn⁴⁺ and simultaneouly precipitate out as pyrolusite (MnO₂), and (6) can sulfate be photoreduced to sulfide (S²⁻) which can then be recycled for precipitation of other mobile toxic constituents as sulfides such as Cu²⁺, Zn²⁺ and Cd²⁺ as has been similarly demonstrated with sulfate-reducing bacteria, SRBs (Ref. 15-17). In this regard, other project goals were to answer these questions and determine if the remediation can be accomplished selectively thereby demonstrating that a recovery process could be developed as opposed to a process which generates a sludge requiring disposal. Ultimately, it was hoped that a technology would be developed for sites where acid mine drainage occurs or, at least, be recommended for further study.

2. PHOTOCHEMISTRY

2.1 Technology Background

Remediation research of polluted waters originating from active or inactive mine sites and associated materials handling procedures has primarily focused on bringing to the affected areas foreign substances and processes which could ultimately disturb a naturally established ecosystem. Remediation methods by, for example, lime addition are inherently expensive and can make the sites difficult to revegetate. Overwhelming evidence shows that natural processes occur that heal environmental scars caused by mining activities. These processes include electron transfer reactions which lower the concentrations of mobile toxic constituents in surface and ground waters via interactions with electromagnetic radiation from the sun, ultraviolet (UV) radiation in particular. However, these naturally photoassisted processes suffer at night, on cloudy days, and in winter months. During these periods, artificial UV sources are needed to sustain the processes. Furthermore, because the processes may still proceed too slowly, photocatalysts or photosensitizers can be supplemented to absorb and transfer the UV radiant energy to the reactants thereby remediating the water within more acceptable time frames. Photocatalysts are predominantly solid semiconductors and photosensitizers are usually dissolved in solution.

In photolysis, solutions (or other sample types) are irradiated with electromagnetic radiation, usually UV, to promote electron transfer reactions between toxins (i.e., metal-complexed cyanide) and other available species. The toxins either undergo photoreduction or photooxidation to yield less toxic or non-toxic compounds depending on the reduction/oxidation (redox) chemistry of the system. Photolysis can be accomplished with direct or indirect techniques. Direct photolysis requires the substance being remediated to absorb the radiation. Indirect processes can be induced by having a second material absorb the radiation and then transfer the photo-energy to the substance being remediated. In this regard, solid semiconductors can be used such that they participate only as catalysts (heterogeneous photocatalysis). On the other hand, dissolved photosensitizers can either be consumed during the reaction (homogeneous photolysis) or participate as catalysts (homogeneous photocatalysis). These photoassisted processes are discussed below but, for simplicity, only as solid photocatalysis and dissolved photolysis.

2.1.1 Solid Photocatalysis

To date, most work has entailed studying the oxidation of toxic organic compounds using solid semiconductors as electron transfer photocatalysts to ultimately produce both carbon dioxide and water (Ref. 18-31). However, current emphasis appears to be on applying this successful technology to the remediation of inorganic compounds in order to satisfy new and more stringent environmental regulations including nitrate (Ref. 1,31-38), free cyanide (Ref. 1,38-56), metal-complexed cyanide (Ref. 2,50-60), and several metal cations (Ref. 18-20,26,35,44,49,54-65). Of course, it is the latter reports which are pertinent to this study; however it is important to illustrate that both photo-oxidation (e.g., cyanide) and photo-reduction (e.g., metal ions) is possible. Photo-reduction is less frequently observed presumably because the reducing power of the excited electron is significantly lower than the oxidizing power of the hole and because the compounds must kinetically compete with oxygen and/or

water as the electron acceptor (Ref. 25).

Numerous solid photocatalysts have been reported to work well: TiO_2 , ZnO, WO_3 , CdS, SiC, Fe_2O_3 and certain zeolites, to name a few. The anatase polymorph of TiO_2 has been preferred because of its low cost, relative abundance, and high quantum efficiency in converting photon energy into chemical energy (Ref. 39,40). In order for these solid semiconductors to function as electron transfer photocatalysts, their band gap energies must be less than the absorbed UV radiation as determined from the equation:

$$\mathbf{E} = \mathbf{h}?$$
 [1]

where h is Planck's constant and ? is the frequency of the UV radiation. Upon absorbance, an electron is excited into the conduction band from the valence band where a "hole" is created (see Figure 2.1):

semiconductor
$$\mathbf{6}^{\text{h?}}$$
 (e⁻ h⁺) [2]

Because the band gap between the conduction and valence band edges lacks energy levels, the excited electron will reside at the conduction band edge whereas the hole will reside at the valence band edge. Consequently, the electron-hole $(e^{-}h^{+})$ pair will be relatively stable possessing a lifetime that is long enough for electron transfer reactions to occur:

$$h^{+} + D \mathbf{6} D^{+}$$
 [3]

$$e + A \mathbf{O} A$$
 [4]

Clearly, electron donors (D) become oxidized when the release electrons to fill the holes (Reaction 3) and electron acceptors (A) are reduced when the consume the excited electrons (Reaction 4).

Solid electron transfer photocatalysis can not occur unless both A and D are preadsorbed at the semiconductor surface and the products, D^+ and A^- , do not react with respective excited electrons and holes to reproduce the reactants. Otherwise no net reaction results. Furthermore, the Nernst potentials of Reactions 3 and 4 must be thermodynamically favorable. Each of these requirements can be met by (1) using semiconductors that are amenable to the adsorption of both A and D but not A^- and D^+ , (2) choosing a semiconductor whose band gap is appropriate for the electron transfer reactions to occur, (3) choosing ligands which react with the radical products to form inert species, (4) selecting appropriate pH conditions, (5) stirring/bubbling the system to remove the radical products from the surface, (6) promoting reactions between the radical products themselves, and (7) depositing metals (i.e., platinum) at the surface as a co-catalyst to localize the excited electrons. Clearly, the surface, electro-, solution, and analytical chemistries of the solid electron transfer photocatalytic reactions must be well understood before they can be induced and/or enhanced. It is important to note that platinum-deposition is accomplished by the photo-reduction of platinum in solution using an appropriate

photocatalyst which essentially is the same as remediating platinum from solution (Ref. 64,65)!

2.1.2 Dissolved Photolysis

Photochemical reactions in the absence of solid semiconductors have involved both organic and inorganic compounds and have been classified as either direct or indirect processes. In direct photochemical processes, the compound (designated as X in subsequent equations) absorbs the electromagnetic radiation to form an excited state which then reacts to form a variety of products (see Figure 2.2):

$$X + h? 6 X^* 6$$
 products [5]

For most organic compounds, this reaction is typical of a decomposition reaction. For certain inorganic compounds, this reaction either (1) yields changes in oxidation states or (2) tranfers the photo-energy to water yielding hydroxyl radicals (OH^{*}) which can then decompose various organic compounds or react with other inorganic species to produce specific radicals (Ref. 18-21,39,61). With indirect photochemical processes, photosensitizers absorb the radiation

$$S + h? 6 S^*$$
 [6]

and then transfer the photo-energy to the compound thereby catalyzing the following reaction:

$$S^* + X 6 S + X^* 6 S + products$$
 [7]

or transfer the energy to another species (usually oxygen) to induce the following reactions:

$$S^{*} + O_{2} 6 O_{2}^{*} + S 6 products + S [8] O_{2}^{*} + X 6 products [9]$$

where the oxygen radical may participate as either a reactant or a co-catalyst. In some cases, the photosensitizer (S) is consumed in the process and is therefore not considered to be a dissolved photocatalyst.

Each of the radicals mentioned above (i.e., inorganic, organic, hydroxyl, specific, photosensitizer, and oxygen) are dissolved photocatalysts and can induce oxidation (electron donating) or reduction (electron accepting) reactions in the same manner as solid photocatalysts. However, the dissolved photocatalysts are not dependent on adsorption and other surface area phenomenon and, by comparison, can therefore be expected to enhance reaction rates by orders of magnitude, dependent only on the concentration of the dissolved photocatalyst. Other dissolved photocatalysts include photon-active redox couples where the oxidant would be the electron donor and the reductant would

be the electron acceptor.

2.2 E_H-pH Diagrams

Because photolysis involves electron transfer reactions, it is helpful to examine thermodynamic equilibrium diagrams such as E_{H} -pH diagrams to see what possible reactions may occur between reacting species and to see what products my be formed as the reaction occurs. In this regard, E_{H} -pH diagrams were generated using STABCAL (Ref. 66,67) and shown to be very reliable in previous and other ongoing MWTP projects (Ref. 1,2,68-71). STABCAL is a program developed for IBM-compatible personal computers to calculate various types of thermodynamic stability diagrams. In order to construct the diagrams for iron, arsenic, manganese, sulfate and anatase, thermodynamic data at 298K was obtained from NBS tables using a reference library within the STABCAL program (Ref. 72).

At the 200-foot depth of the Berkeley Pitlake (i.e., deep Berkeley Pitlake water) where samples are often collected for research purposes, E_{H} -pH conditions typically measure 0.6 volts (E_{H}) and 2.65 (pH). These conditions are marked with a star on each of the ensuing E_{H} -pH diagrams.

2.2.1 Iron Photo-Oxidation

The E_{H} -pH diagram for the iron-water system in Figure 2.3 confirms that the predominant iron species for deep Berkeley Pitlake Water is aqueous ferrous cations (Fe²⁺). However, if the conditions are perturbed via UV irradiation and, if necessary, the addition of a photochemical, the ferrous cation can be oxidized to ferric cation by, for example, reacting with a hole, h⁺:

$$Fe^{2+} + h^{+} = Fe^{3+}$$
[10]

Because ferric cations are relatively unstable in water, an immediate reaction with water or dissolved oxygen will occur in which hematite (Fe_2O_3), or other similar iron species such as ferrihydrite [$Fe(OH)_3$], will precipitate:

$$2Fe^{3+} + 3H_2O = Fe_2O_3 + 6H^+$$

$$2Fe^{3+} + 3/2O_2(aq) = Fe_2O_3$$
[11a]
[11b]

The iron-precipitate can be easily removed via conventional solid/liquid separation processes such as thickening and filtering. However, because Berkeley Pitlake water contains sulfate at high concentrations, it is most likely that, under the conditions of deep Berkeley Pitlake water, ferrous sulfate [FeSO₄ (aq)] is the predominant iron species and schwertmannite [Fe₈O₈(OH)₆SO₄·5H₂O] is the likely precipitate that will form upon photooxidation (Ref. 73,74). This is illustrated in the E_H-pH diagram for the iron-sulfur-water system in Figure 2.4 and is similar to the iron-water system in Figure 2.3.

2.2.2 Arsenic Photo-Oxidation

An E_{H} -pH diagram for the arsenic-water system is illustrated in Figure 2.5. The dihydrogen arsenate ion (H₂AsO₄⁻) is depicted to be predominant arsenic species under the conditions noted for deep Berkeley Pitlake water. However, because deep Berkeley Pitlake water conditions are near the stability region of arsenious acid (HAsO₂), it is likely that arsenious acid will be present in minor amounts. Nevertheless, arsenious acid will convert to arsenate ion in the presence of UV radiation and an appropriate photochemical (Ref. 75):

$$HAsO_2 + 2H_2O + 2h^+ = H_3AsO_4 + 2H^+$$
 [12]

This is significant for two reasons: all arsenic species would be present as As (V) and As (V) species are easier to remove from solution than As (III), especially if the ferrihydrite adsorption method is used (Ref. 76-78). Consequently, arsenic remediation can be conducted simultaneously with the ferrous photooxidation process described above (see Reactions 10-11).

2.2.3 Manganese Photo-Oxidation

An E_{H} -pH diagram for the manganese-sulfur-water system is shown in Figure 2.6. It confirms that the predominant manganese species under the conditions of deep Berkeley Pitlake water is manganous cation (Mn^{2+}). Like iron, manganous cations can also photo-oxidize to form a precipitate:

$$Mn^{2+} + 2H_2O + 2h^+ = MnO_2 + 4H^+$$
[13]

The precipitate of pyrolusite (MnO_2) can also be removed by conventional solid/liquid separation techniques. It is not known whether manganese will form a precipitate similar to schwertmannite due to the presence of sulfate in the Berkeley Pitlake water. Nevertheless, manganese removal from acid mine waters can be conducted simultaneously with iron and arsenic removal or selectively if appropriate redox potentials can be maintained.

2.2.4 Sulfate Photo-Reduction

Because of the presence of sulfate in the Berkeley Pitlake water, the E_{H} -pH diagram in Figure 2.7 for the sulfur-water system was previously superimposed on Figures 2.4-2.6 for the iron-, arsenic- and manganese-sulfur-water systems, respectively. However, in order to remediate sulfate by photolysis, a reduction reaction involving photon-excited electrons must be induced to yield elemental sulfur (S°) or aqueous hydrogen sulfide (H₂S):

$$SO_4^{2-} + 8H^+ + 6e^- = S^0 + 4H_2O$$
 [14a]

$$SO_4^{2-} + 8H^+ + 8e^- = S^{2-} + 4H_2O$$
 [14b]

Although elemental sulfur could be removed via conventional solid/liquid separation techniques, its formation is unlikely due to a large activation energy barrier that must be overcome and consequently leads to the production of aqueous hydrogen sulfide (Ref. 79,80). In this regard, elemental sulfur was

not included in any of the previous E_{H} -pH diagrams (see Figures 1.4-1.6). Nevertheless, aqueous hydrogen sulfide could be used directly or converted to a gas for recycling and precipitation of other heavy metals (e.g., Cu^{2+} , Zn^{2+} and Cd^{2+}) in the Berkeley Pitlake water (Ref. 9,68). A similar approach to this is the use of sulfate-reducing bacteria to produce sulfide (Ref. 15-17). Conventional solid/liquid separations could then be used to process the sulfide precipitates.

2.2.5 Anatase Photocatalysis

Reactivities for electron-hole pairs produced at anatase (TiO₂) surfaces were superimposed on the E_HpH diagram presented for the iron-water system in Figure 2.3. For clarity, the reactivities were not shown for iron-sulfur, arsenic-sulfur, manganese-sulfur, and sulfur-only E₁₁-pH diagrams in Figures 2.4-2.7. A comparison of Figures 2.1 and 2.3 shows that the valence and conductance bands are reversed; however, this is merely due to convention. The position of the bands concurs with those determined at pH 1, 7, and 14 and illustrates that the bandgap for anatase is 3.2 eV (Ref. 18-20,61). According to Equation 1, a photon must have a frequency of 7.75×10^{14} Hz in order for its absorbance to occur. This equates to a maximum wavelength of 387.5 nm and therefore indicates that the various UV sources employed in this study were adequate for inducing solid photocatalysis (see Section 3 -Treatability). As previously noted, conductance and valence bands represent the affinity for electrons to be consumed (by holes) and donated (as excited electrons) and are therefore a measure of relative reduction and oxidation potentials, respectively. Because ferrous and manganous cations as well as arsenous acid lie below the valence band, they can be expected to undergo oxidation, as depicted in Reactions 10 through 13, by releasing electrons to photon-produced holes. Similarly, since sulfate species lie above the conductance band, it can be expected to undergo reduction, as depicted in Reaction 14, by accepting photon-excited electrons.

2.3 Preliminary Investigations

Two preliminary investigations to this QA/QC study were conducted separately; the first by Steve Cashin led to the initiation of this MWTP Acitivity IV Project 3B (Ref. 81), and the second by Yu-Chuan Tai resulted in his thesis (Ref. 82) as well as the QA/QC results (see Section 3).

2.3.1 Cashin and Young

Preliminary data obtained previous to this investigation by Cashin and Young (Ref. 81) for iron remediation from Berkeley Pitlake water in the absence and presence of UV radiation and a photolytic reagent (i.e., H_2O_2) is shown in Figure 2.8. These results were obtained by stirring 200 ml of Berkeley Pitlake water under open conditions. The best results are observed to occur when the photolytic reagent was used and exposed to UV radiation for 240 minutes. The iron concentration in the Berkeley Pitlake decreased from approximately 1300 ppm to nearly 620 ppm due to Fe(II) oxidation and subsequent precipitation of an Fe(III) species such as hematite, ferrihydrite or schwertmannite (see Reactions 10 and 11a,b). This equates to a remediation value of 52%. By comparison, only 42% iron remediation was observed in the absence of UV radiation (i.e., dark). Clearly, these exciting results led to a thesis (Ref. 82) and the study reported in this final report.

It is important to note that iron oxidation in the absence of a photolytic reagent could be achieved simply by stirring in open air and reacting with molecular oxygen. However, reaction times are shown to be very slow in agreement with the literature (Ref. 68). Interestingly, equilibrium results were obtained more quickly in the presence of UV radiation. This direct photolytic process suggested that sunlight may play a significant role in acid mine drainage systems. This conclusion has given rise to a future study on naturally-occuring reactions in the surface waters of the Berkeley Pitlake (Ref. 6).

Cashin and Young (Ref. 81) also examined the concentrations of other metals during these preliminary iron oxidation experiments. Results for Mn, Al, Cd, Cu and Zn are shown in Figures 2.9 through 2.13, respectively. Mn as shown in Figure 2.9 appers to behave like Fe. Examination of the E_{H} -pH diagram for Mn suggests Mn²⁺ photo-oxidized to Mn^{4+} and precipitated out as MnO_2 as discussed earlier (see Figure 2.6 and Recation 13). By comparison, E_{H} -pH diagrams for Cu, Zn, Al, and Cd in the literature (Ref. 83,84) show that increased oxidation potentials caused by photolysis of H₂O₂ should not affect their solution concentrations. The results obtained for Al and Cd in Figures 2.10 and 2.11 appear to verify this hypothesis. However, the results for Cu and Zn in Figures 2.12 and 2.13 appear to as well but only in the presence of UV radiation. This behavior is explained by Cu and Zn adsorption at the surface of the Fe and Mn precipitates in the absence of UV radiation. In the presence of UV radiation, interfacial phenomena, perhaps induced by the formation of holes and excited electrons at the precipitate surfaces due to photocatalytic properties, prevent their adsorption. In this regard, the behavior of Al and Cd is tentatively referred to UV-independent adsorption and the behavior of Cu and Zn is referred to as UV-dependent adsorption. Based on these results and the possibility of using sunlight as a free source of UV radiation, it is understandable how these preliminary results led to this investigation.

2.3.2. Tai and Young

As part of his thesis (Ref. 82), Tai conducted a series of experiments in the absence and presence of UV radiation to examine the effect of pH on H_2O_2 photo-oxidation of Berkeley Pitlake water. The pH was adjusted with NaOH instead of lime to avoid gypsum precipitation. Results are presented in Figures 2.14 and 2.15 with and without 254nm UV radiation, respectively.

Figure 2.14 shows Fe is preferentially precipitated at pH values less than 4. At higher pH values, both Cu, Zn, and Al concentrations begin to decrease due to metal-hydroxide formation and/or adsorption at the surface of the iron precipitate. Mn and Cd concentrations are relatively constant until pH values exceed 6. Since Mn was not remediated, the results contrast with those obtained by Cashin and Young (Ref. 81). The reason for this behavior was not determined until QA/QC experiments were conducted (see Section 3.2 - Experimental Results). All other results presented in Figure 2.14 appear to concur with those of Cashin and Young (Ref. 81) as do most of the results presented in Figure 2.15.

Figure 2.15 shows that, in the absence of UV radiation, both Cu and Al are remediated from solution at pH values greater than pH 3. Because Cu and Al exhibit different concentration profiles (compare Figures 2.14 and 2.15), their behavior is attributed to adsorption. On the other hand, the concentration profiles of Zn and Cd as a function of pH appear to be independent of UV exposure. Their pH profiles can therefore be attributed to precipitation. By comparison, the Mn-profile is relatively independent of pH and thus does not exhibit either adsorption or precipitation behavior; hence, the importance of remediating Mn via (photo-)oxidation in order to avoid a 2-stage lime precipitation process.

It was therefore concluded that selective iron removal from Berkeley Pitlake water could be accomplished but, presumably, would require UV radiation to prevent or minimize Cu and Al adsorption and, more importantly, would require pH values to be below pH 4. Consequently, in order to examine the effects of UV radiation on iron without changing the concentration of the other metals, it was decided that QA/QC experiments should be conducted at pH 3 (see Section 3.1 - General Test Procedures).

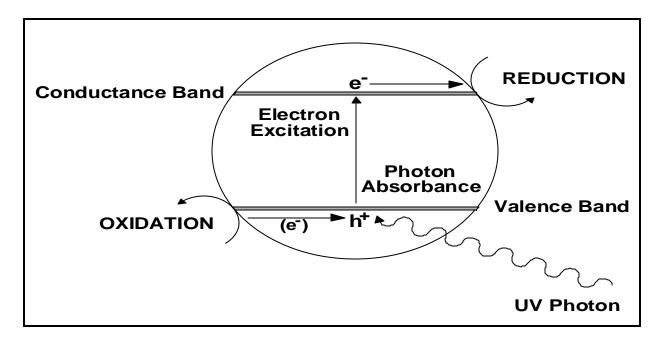


Figure 2.1. Schematic of the photocatalytic process for

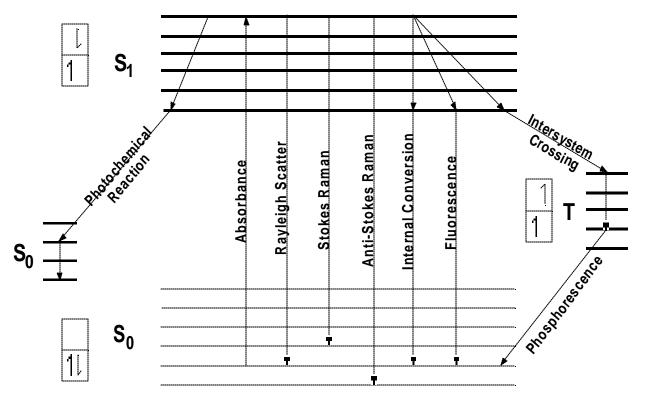
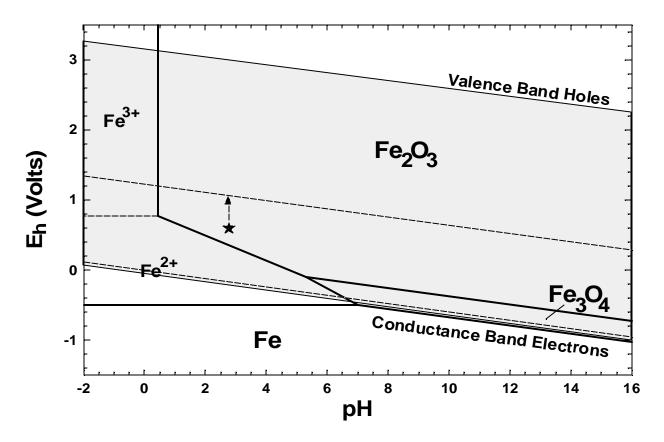


Figure 2.2. Jablonski energy level diagram depicting the various relaxation pathways an electron after being excited by photon Figure



2.3. E_{H} -pH diagram for the iron-water system at 298 K.

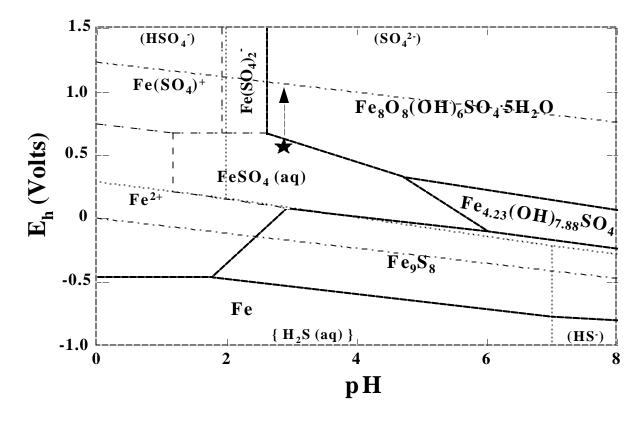


Figure 2.4. $E_{\rm H}$ -pH diagram for the iron-sulfur-water system at 298 K.

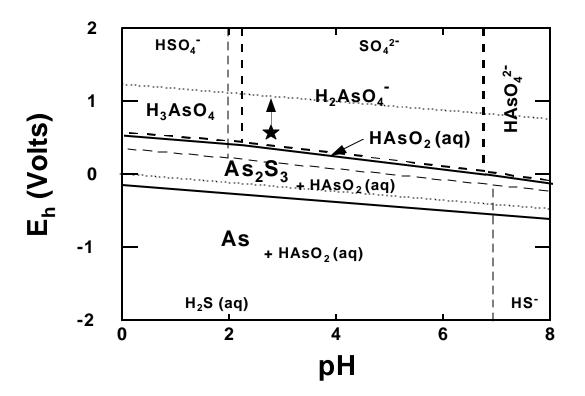


Figure 2.5. $E_{\rm H}\mbox{-}p\mbox{H}$ diagram for the arsenic-sulfur-water system at 298 K.

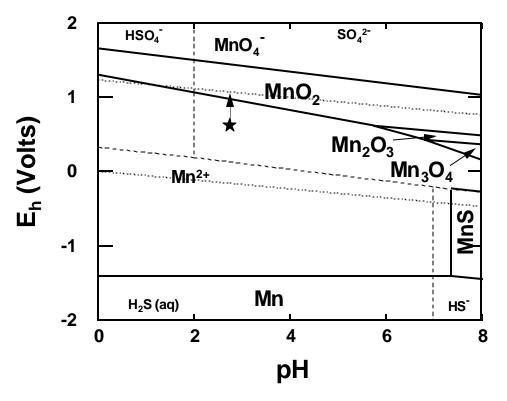


Figure 2.6. E_{H} -pH diagram for the manganese-sulfur-water system at 298 K.

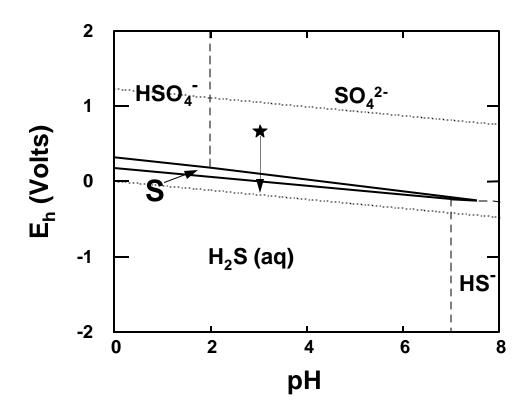


Figure 2.7. $E_{\rm H}$ -pH diagram for the sulfur-water system at 298 K.

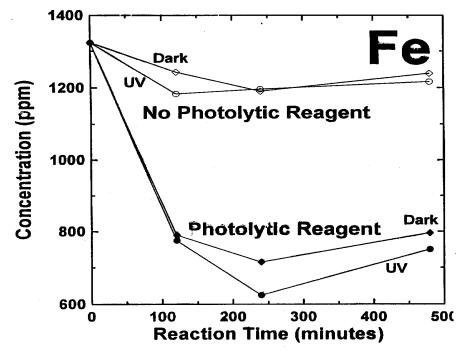


Figure 2.8. The effect of a photolytic reagent and UV irradiation on iron remediation as a function of time.

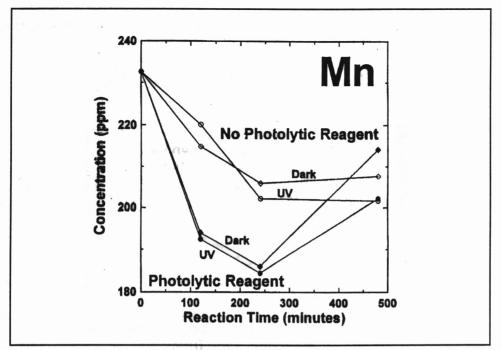


Figure 2.9. The effect of a photolytic reagent and UV irradiation on manganese remediation as a function of time.

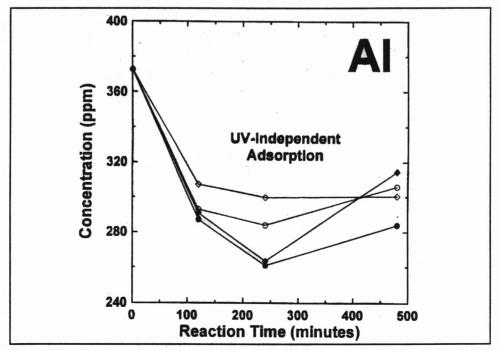


Figure 2.10. The effect of a photolytic reagent and UV irradiation on aluminum remediation as a function of time.

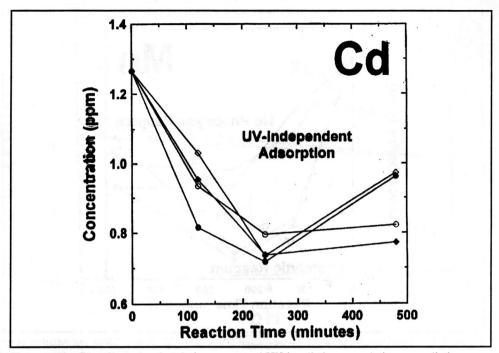


Figure 2.11. The effect of a photolytic reagent and UV irradiation on cadmium remediation as a function of time.

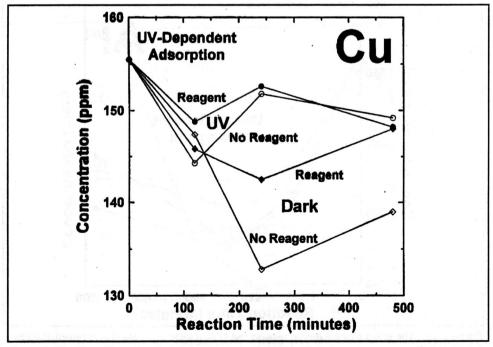
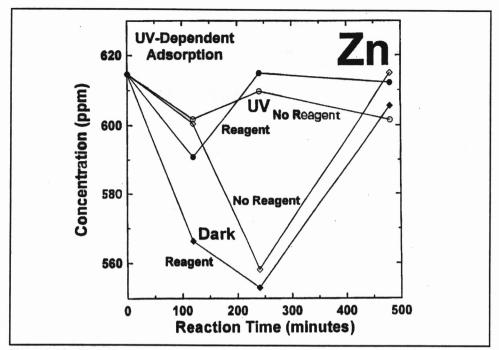
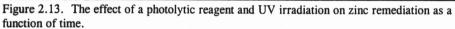


Figure 2.12. The effect of a photolytic reagent and UV irradiation on copper remediation as a function of time.





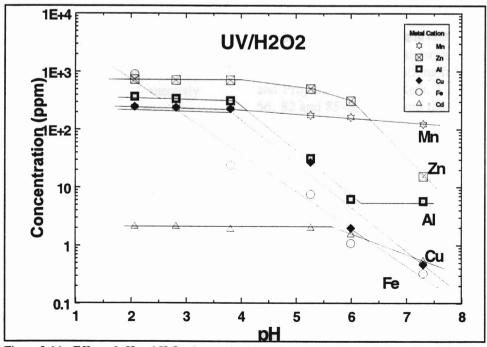


Figure 2.14. Effect of pH and H_2O_2 photo-oxidation on heavy-metal remediation of Berkeley Pit water.

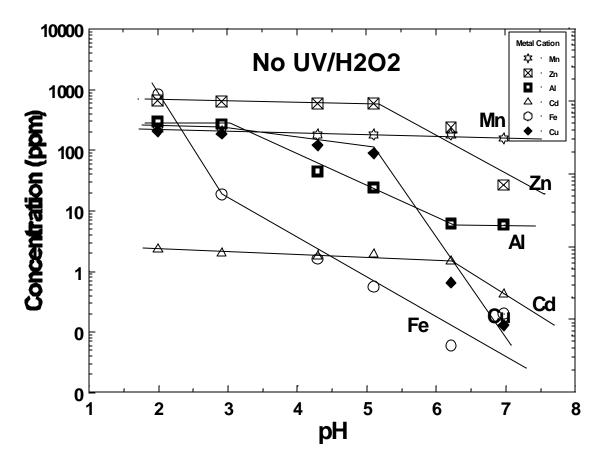


Figure 2.15. Effect of pH and H₂O₂ oxidation on heavy metal remediation of Berkeley Pitlake water.

3. TREATABILITY

Experimental procedures were the same in this study as for the photooxidation experiments of free cyanide and metal-complexed cyanide and photo-reduction experiments of nitrate conducted in the previous MWTP studies (Ref. 1,2). A major difference was how the mobile toxic constituents were detected and quantified. In this regard, an inductively-coupled plasma (ICP) spectrophotometer was used.

3.1 General Test Procedures

For this project, a 5-gallon sample of water from the Berkeley Pitlake was collected and transported to the ELC Building at Montana Tech by the Montana Bureau of Mines and Geology. The water was obtained from the 200-foot depth (i.e., deep Berkeley Pitlake water) and stored in a refrigerator to help maintain freshness (see Section 6 - Field Samples). Aliquats measuring 150 milliliters (ml) were taken from this sample for each experiment and placed in standard 250 ml Pyrex beakers (Fisher) as reaction vessels. The aliquats were magnetically stirred using the experimental setup shown in Figure 3.1. The experimental set-up shows the pyrex beaker being illuminated by a UV source from above while simutaneously being sparged by a gas and stirred magnetically with a magnetic stirrer and Teflon-coated stirbar (VWR). The magnetic stirrer was operated at approximately 2-speed.

Experiments were conducted in the absence and presence of both UV radiation and photochemicals. The UV sources (Rayonet) had rated intensities of 16000 FW/cm² and emitted radiation with peak intensities at wavelengths of 185, 254 or 365 nm. Photochemicals included hydrogen peroxide (J.T. Baker), hydrazine hydrate (J.T. Baker), sodium formate (Fischer), and anatase (Degussa P25). Deionized/distilled water was used for the dissolution of photochemicals prior to their addition, and the dilution of acid (H_2SO_4 or HNO_3 , J.T. Baker) and base (NaOH, Fischer) for pH control. All reagents were reagent grade and obtained from the indicated commercial manufacturers. Most photo-oxidation experiments involving iron, arsenic and manganese remediation were conducted at pH 3. All photoreduction experiments involving sulfate were continuously sparged with argon gas (General Distributing Co.) to maximize reducing conditions and were conducted at pH 6. Gas flow rates were measured with an in-line flow meter. Experiments were conducted for 1.5 hours. Non-irradiated tests would help ascertain the applicability of photolysis.

QA/QC was conducted at all times (see Ref. 4 as well as Section 4 - Quality Assurance/Quality Control; and Section 6 - QA/QC Activities). Experimental conditions for the 11 photo-oxidation, 5 photoreduction, and 5 non-irradiated QA/QC experiments are listed in Tables 3.1-3.3, respectively. These experiments were found to be the most desirable after determining that the most appropriate photolytic technologies involved dissolved photosensitizers and solid photocatalysts as suggested by resulting publications and presentations from this project and Projects 3 and 3A (Ref. 1,2,38,53,55,56,82,85-87). During the course of this study, it became apparent that two experiments needed to be conducted as well (see Section 3- Results and Discussion and Section 6 - QA/QC Activities). These new experiments were designated 3A and 17A in Appendix A as well as in the tables below. This included the thesis work of a Metallurgical Engineering Masters graduate student who recently graduated (Ref. 82).

Iron, arsenic and manganese concentrations were measured at the start and conclusion of each photooxidation experiment using a Varian Liberty 110 Inductively-Coupled Plasma (ICP) spectrophotometer in accordance with EPA Method 6010A, Inductively Coupled Plasma-Atomic Emission Spectroscopy (Ref. 88). Sulfate concentrations were measured at the start and conclusion of each photo-reduction experiment using a Dionex DX-100 Model DX 1-03 ion chromatograph (IC) equipped with an IONPAC® AS4A analytical column (P/N 37041), an IONPAC® AG4A guard column (P/N 30742), and an ion self suppressor (P/N 43189). This was in accordance with EPA Method 300.0, The Determination of Inorganic Anions in Water by Ion Chromatography (Ref. 89). ICP and IC measurements were conducted outside the reaction vessel by taking appropriate sample volumes with syringe filters and diluting as necessary with appropriate matrix solutions. Plastic vials (VWR) were used for temporary storage of samples until analyses could be made. Arsenic and manganese concentration measurements were deemed as non-critical (see Section 6 - QA/QC Activities) whereas iron and sulfate concentration measurements were deemed as critical (Ref. 4). The pH conditions were measured in-situ at the start and conclusion of each test as well as at least twice during the progress of the experiments using an Orion combination pH electrode (Model 81-02) coupled to an Orion pH meter (Model 920A) in accordance with EPA Method number 4500, Electrometric Measurement (Ref. 90).

3.2 Experimental Results

In this section, the results of iron photo-oxidation and sulfate photo-reduction are further discussed to delineate the effect of UV radiation. Experiments were conducted in the absence and presence of both UV radiation and photochemicals. UV wavelengths were varied among 365 nm, 254 nm and 185 nm. Photochemicals included hydrogen peroxide and anatase for the iron photo-oxidation experiments and hydrazine hydrate, sodium formate, and anatase for the sulfate photo-reduction experiments. Results listed in Appendix A as % Fe and % SO_4^{2-} remediation were determined from the QA/QC data presented in Appendix B. Results in Appendix A are grouped into appropriate figures and tables in order to discuss the effects of certain parameters such as pH and wavelength on remediation.

3.2.1 Iron Photo-Oxidation

Fifteen experiments on iron oxidation were conducted to determine the effect a number of parameters: photochemical type and amount, wavelength, presence of UV, oxygen, and kinetics.

3.2.1.1 Anatase

Iron remediation by photo-oxidation was examined as a function of anatase addition in the presence of 254 nm UV radiation and oxygen. Results after 1.5 hours of equilibration are listed in Table 3.4. In the absence of anatase (i.e., direct photolysis), only 3.1% remediation was observed. By comprison, Table 3.4 clearly show that iron remediation can be improved using solid photocatalysis with anatase. Unfortunately, the level of remediation is low, barely in excess of 6%. The results also indicate that there is an upper level of anatase amount to add, perhaps near 0.2 g/l, such that the addition of more anatase does not lead to more remediation. This behavior can be attributed to the design of the reactor (see Figure 3.1) which is simple in nature but does not take into account the shallow depth of UV penetration through water. To remedy this, other more appropriate designs could have been used but were too expensive to consider for this evluation study (Ref. 91,92).

3.2.1.2 Hydrogen Peroxide

Iron removal was also examined as a function of the amount of H_2O_2 added in the presence of 254 nm UV radiation and oxygen. Results after 1.5 hours of equilibration are listed in Table 3.5 and indicate that, as the amount of H_2O_2 is increased, the amount of iron remediation is also increased. However, like the anatase, the amount of remediation increases drastically initially but higher dosages due not increase the amount of remediation significantly. In this case, increasing the dosage of H_2O_2 from 0.25 ml to 1.25 ml increases iron remediation from 28.8% to 32.2%, a mere 3.4%. Although 100% Fe remediation would have been preferred to observe, an examination of Figures 2.14 and 2.15 shows that these results concur with the preliminary investigations. According to solubility diagrams of ferrihydrite and other similar iron compounds, had higher pH values been tested, Fe remediation percentages would have been improved (see Figure 3.2).

3.2.1.3 Wavelength

Experiments were conducted on Berkeley Pitlake water to examine the effects of wavelength on iron removal using H_2O_2 and O_2 -sparging. After conducting the experiments for 1.5 hours, results show that shorter wavelengths are more efficient (see Table 3.6). Because photolysis cannot occur unless the UV radiation is absorbed, the improved performance at lower wavelengths is attributed to improved UV absorbance. UV-vis absorbance spectrum of H_2O_2 at low pH in Figure 3.3 show that strong absorbance at low wavelengths do indeed occur.

3.2.1.4 Direct Photolysis

Experiments were conducted on Berkeley Pitlake water to examine the effects of UV radiation in the absence of photochemical reagents and without O_2 -sparging. After conducting the experiments for 1.5 hours, results in Table 3.7 show that direct photolysis appears to occur but is rather slow with less than 1% Fe remediation being observed. Furthermore, the process appears to be dependent on wavelength with the longer wavelength yielding higher remediation: 254nm yielded 0.66% remediation and 185nm yielded 0.16% remediation. The results are insignificant except to illustrate that photolytic processes may be occuring naturally in the Berkeley Pitlake. This an important conclusion for future studies (Ref. 6).

3.2.1.5 Oxygen

The effect of oxygen was investigated for both the TiO₂ and H_2O_2 photolytic systems using 254 nm UV radiation. Results that were obtained after 1.5 hours of equilibrating are presented in Table 3.8. Interestingly, iron remediation is observed to decrease when O_2 is present. For TiO₂, iron remediation decreased from 8.1% to 6.2% and, for H_2O_2 , it decreased from 31.8% to 28.8%. These differences are attributed to O_2 lowering the oxidation potentials of the valence band holes of TiO₂ and hydroxyl radicals from H_2O_2 . In other words, because the OH^c/H_2O_2 redox couple is higher than the H_2O_2/O_2 redox couple, ferrous-to-ferric oxidation is more complete in the absence of oxygen. This "mixed-potential" result suggests that oxygen should not be used in these photolytic systems. It is interesting to note that the preliminary experiments conducted by Cashin and Young (Ref. 81) were conducted in this manner. Consequently, it can be concluded this is why MnO₂ precipitation was not observed in this study.

In order to examine the effect of O₂ further, experiments were conducted in the absence of UV

radiation. Results presented in Table 3.9 illustrate that the presence of O_2 is deleterious to H_2O_2 oxidation even in the absence of UV radiation. This can be attributed to the "mixed-potential" phenomenon mentioned above, thereby suggesting that oxygen should not be used in these systems either.

3.2.1.6 UV Radiation

The effect of 254nm UV radiation on Fe can be determined by comparing the results of experiments 3 and 17, 5 and 18, and 6 and 19. Experiments 3 and 17 were conducted with H_2O_2 and without O_2 , Experiments 5 and 18 were conducted without H_2O_2 and with O_2 and, Experiments 7 and 19 were conducted with H_2O_2 and with O_2 . In each case, Fe remediation decreases significantly upon UV irradiation. The decrease is minimal when H_2O_2 is present: 34.7% to 31.8% without O_2 and 30.6% to 28.8% with O_2 ; however, the decrease is significant when H_2O_2 is absent: 12.2% to 0.31%. Surprisingly, these results suggest that the use of UV radiation for the remediation of acid-mine drainage is inappropriate. In defense of this conclusion, it is important to note (1) that these results were obtained with a one-time addition of H_2O_2 at the start of the experiments as opposed to staged or continuous addition which would likely be the case in an industrial setting, and (2) that non-QA/QC data presented in Figures 2.14 and 2.15 indicate that UV radiation may prevent adsorption of some metal cations at the surface of precipitates due to photocatalytic activities.

3.2.1.7 Kinetics

In order to further understand the effect of UV, experiments 3 and 17 were reconducted as specified (i.e., in the absence of oxygen but with and without 254nm UV radiation, respectively). However, in this case, samples were taken periodically so results could be analyzed kinetically. These experiments, designated as 3A and 17A in Appendix A, were conducted according to QA/QC procedures but were determined to be important enough to include even though the QAPP did not require them (see Section 6 - QA/QC Activities). Results are presented in Figure 3.4. Results show Fe remediation was 32.8% in the absence of UV radiation and 30.2% in the presence of UV radiation. These results are quite comparable to the QA/QC results of 34.7% and 31.8% obtained for the original experiments and consequently confirm that Fe remediation with H₂O₂ is best in the absence of UV. However, it is critical to note that the reaction profiles in Figure 3.4 clearly show that H₂O₂ photolysis is the better process in the first ten minutes; and this reaction profile would likely have progressed had the H₂O₂ been added continuously or in stages as opposed to only at the start of the test.

In lieu of these comments, the data was replotted using time as a logarithmic scale (see Figure 3.5). The resulting profile for the non-irradiated sample shows at least one plateau indicating that there is an initial slow reaction which must first be overcome before Fe oxidation actually occurs. This behavior can be attributed to the oxidation of another species, most likely organic in nature. The lack of plateaus for the irradiated sample suggests the reaction of hydroxyl radicals with the suspected organic is significantly faster due to resulting higher oxidation potentials and therefore a stronger driving force to react. At pH 7, the H_2O_2/H_2O couple has a reversible potential near 1.3 volts vs SHE and the OH^*/H_2O couple is near 2.1 volts vs. SHE (Ref. 18-20,60,93). Consequently, under non-irradiated conditions, H_2O_2 has a longer lifetime (which explains why pharmaceutical H_2O_2 is stored in brown bottles) and is more efficient at reacting on a molar basis. It can thus be concluded that, under irradiated conditions, H_2O_2 should be added continuously or, at least, in stages to overcome this

problem and, in this regard, UV irradiation would likely prove to be better than non-irradiated systems. Clearly, though, more research is needed.

3.2.2 Sulfate Photo-Reduction

Seven experiments on sulfate reduction were conducted to see if sulfide could be produced using several photochemicals either individually or in combination and in the absence or presence of 254nm UV radiation. Argon gas was continually sparged to help remove dissolved oxygen and thereby maximize reducing conditions.

3.2.2.1 Photochemicals

Sulfate photo-reduction experiments were conducted with Na-formate, hydrazine, and anatase. Because the literature concludes that a combination of dissolved photochemicals works better in the presence of a solid photocatalyst (Ref. 22-25), experiments were also conducted using formate/anatase and hydrazine/anatase combinations. Results presented in Table 3.11 show the best remediation of 9.2% was obtained with hydrazine alone followed by 6.7% remediation with formate alone. When anatase was used in combination with hydrazine and formate, sulfate remediation worsened to 5.4% and 2.9%, respectively. These results clearly show that, in the case of remediating acid-mine waters, the combination of photochemicals is detrimental. This has been observed previously for hydrogen peroxide/anatase and was attributed to the formation of a titanium complex (Ref. 59,86). Such a conclusion could be reached here but would be speculation at best. Finally, results obtained with anatase alone was the worst at 2.3% sulfate remediation.

3.2.2.2 UV Radiation

In order to insure that sulfate photoreduction is fact, Experiments 12 and 13 were repeated in the absence of UV radiation and designated as Experiments 20 and 21. The results of these four experiments are listed in Table 3.12. Unlike Fe photo-oxidation results, Table 3.12 indicates that sulfate remediation is best in the presence of UV. Due to the redox nature of the photochemicals tested, it can also be concluded that sulfate photo-reduction improves with increased reducing power and that power improves upon UV irradiation. $E_{\rm H}$ measurements conducted simultaneously to the process showed that the potentials were not low enough to reduce the sulfate to the desired sulfide (see Figure 2.7).

In general, it is intriguing that sulfate concentrations were observed to decrease in all of these experiments. Unfortunately, sulfide formation was never observed and, as a result, sulfide precipitation for selective recovery of copper, zinc and cadmium could not be tested. It can therefore be concluded that further research is needed to find a way to achieve this photolytic goal.

3.3 Summary

Photo-oxidation experiments of Berkeley Pitlake water were conducted to remediate ferrous (Fe²⁺), manganous (Mn²⁺) and arsenate (AsO₄³⁻) ions with anatase (titanium dioxide, TiO₂) and hydrogen peroxide (H₂O₂). Ferrous and manganous ions were expected to be removed by their oxidation to ferric and manganese(IV) and subsequent precipitation as ferrihydrite and pyrolusite, respectively. On the other hand, arsenate remediation was expected to occur via adsorption at the surface of the precitated ferrihydrite. In addition, photo-reduction experiments for sulfate remediation were conducted using strong reducing agents of sodium formate (NaCOOH) and hydrazine (H₄N₂) in the

absence and presence of the anatase (TiO_2) in hopes of producing sulfide (S^{2-}) for the additional remediation of additional mobile toxic constituents such cupric (Cu^{2+}) , zincic (Zn^{2+}) , and cadmous (Cd^{2+}) cations via their precipitation as sulfide compounds. Reaction efficiencies were calculated and compared as remediation percentages for all experiments.

Results showed that sulfate photo-reduction worked but, under the conditions examined, was not 100% effective. Photo-reduction the dissolved photochemicals proved to work best with hydrazine and formate yielding 9.2% and 6.7% remediation, respectively. When hydrazine and formate were used simultaneously with anatase, remediation percentages decreased to 5.4% and 2.9%, respectively. Anatase, by itself, only yielded 2.3% remediation. Consequently, it is concluded that the presence of anatase, as a solid photocatalyst, with either hydrazine or formate, as dissolved photochemicals, is detrimental to the homogeneous photolysis processes. Although sulfide formation was never observed, it is clear that photo-reduction of sulfate is possible with both homogeneous photolysis and heterogeneous photocatalysis.

By comparison, ferrous photo-oxidation could be 100% effective but was found to be dependent on the conditions applied, especially pH. Results indicated that homogeneous photolysis with hydrogen peroxide worked better than heterogeneous photocatalysis with anatase yielding 28.8% remediation versus 6.1% remediation. Higher dosages of either photochemical yielded only marginal improvement in remediation. Further experiments showed that photolysis with hydrogen peroxide improved with decreasing wavelegth, but was actually best in the absence of UV radiation. This surprising result was attributed to bubbling in oxygen during the experiments as well as to not adding the photochemical continuously and observing a side reaction for only the UV-assisted experiments. The side reaction was further attributed to photo-oxidation of organic species. Oxygen bubbling was believed to have created a mixed potential which lowered the solution potential (E_H) in the experiments below the potential required for manganous oxidation to occur. In this regard, manganous concentrations were not observed to change and its measurement was therefore removed from the critical list. Unfortunately, the selected pH condition of 3 was too low to observe adequate ferrous remediation. Iron concentrations in solution therefore remained high and interfered with the arsenic concentration measurement by ICP. In this regard, arsenic concentrations were unable to be determined and its measurement was also removed from the critical list.

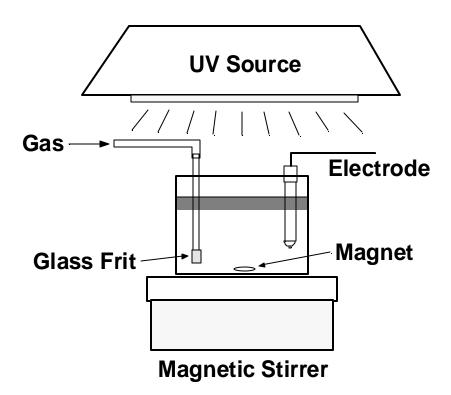


Figure 3.1. Experimental setup for QA/QC work in MWTP Activity IV, Project 3B.

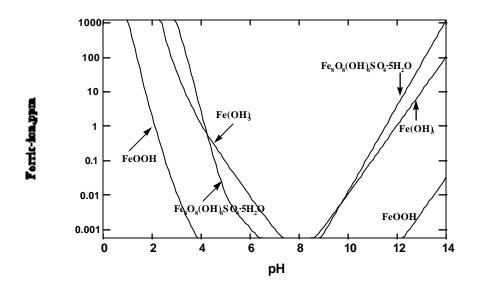


Figure 3.2. Solubilities of ferrihydrite, $Fe(OH)_3$; schwertmannite, $Fe_8O_8(OH)_6SO_4$, SH_2O ; and goethite, FeOOH in concentration of iron (III) as a function of pH.

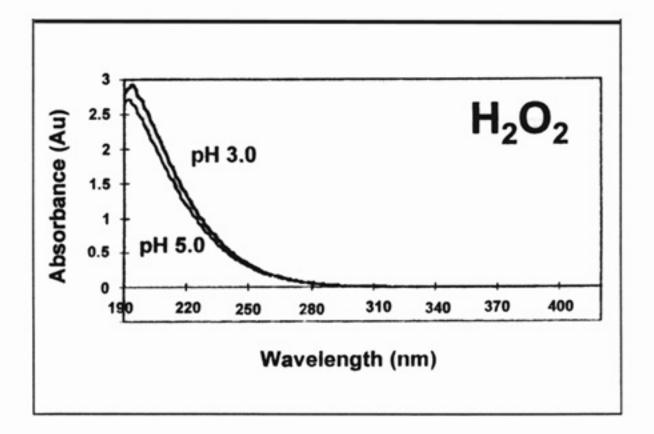


Figure 3.3. UV-vis absorbance spectra of hydrogen peroxide at pH 3 and 5.

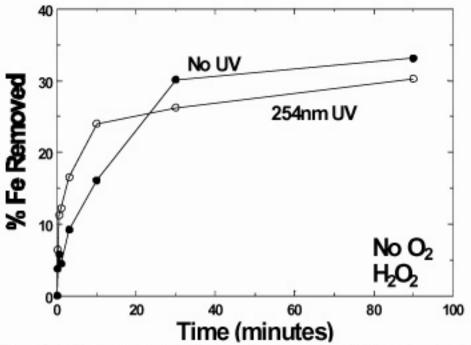


Figure 3.4. Plot to compare the Fe remediation kinetics of UV irradiated and non-irradiated samples of Berkeley Pitlake water with H₂O₂ in the absence of O₂.

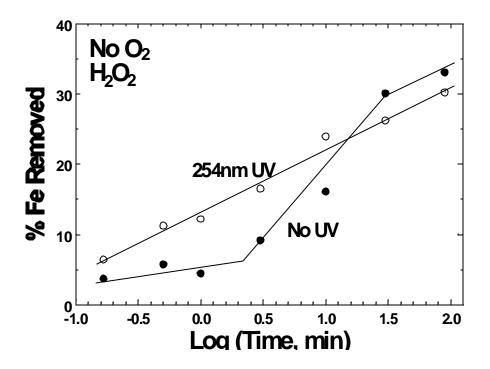


Figure 3.5. Semi-logarithmic plot to compare the Fe remediation kinetics of UV irradiated and non-irradiated samples of Berkeley Pitlake water with H_2O_2 in the absence of O_2 .

Experiment No.	UV Wavelength	Photolytic Reagent Concentration or Amount	Sparging Gas
1	185nm	None	None
2	254nm	None	None
3	254nm	30% H ₂ O ₂ (0.25 ml)	None
3A	254nm	30% H ₂ O ₂ (0.25 ml)	None
4	254nm	TiO ₂ (2.0 g/l)	None
5	254nm	None	O_2
6	185nm	30% H ₂ O ₂ (0.25 ml)	O ₂
7	254nm	30% H ₂ O ₂ (0.25 ml)	O ₂
8	254nm	30% H ₂ O ₂ (1.25 ml)	O ₂
9	365nm	30% H ₂ O ₂ (0.25 ml)	O ₂
10	254nm	TiO ₂ (0.2 g/l)	O ₂
11	254nm	TiO ₂ (2.0 g/l)	O ₂

 Table 3.1
 Photo-oxidation Test Conditions and Reagent Schedules for Project 3B.

Table 3.2. Photo-reduction Test Conditions and Reagent Schedules for Project 3B.

Experiment No.	UV Wavelength	Photolytic Reagent Concentration or Amount	Sparging Gas
12	254nm	Na-Formate (0.5 M)	Ar
13	254nm	Hydrazine (0.5 M)	Ar
14	254nm	TiO ₂ (2.0 g/l)	Ar
15	254nm	TiO ₂ (2.0 g/l) Na-Formate (0.5 M)	Ar
16	254nm	TiO ₂ (2.0 g/l) Hydrazine (0.5 M)	Ar

Experiment No.	Sample Test	Photolytic Reagent Concentration or Amount	Sparging Gas
17	Oxidation	30% H ₂ O ₂ (0.25 ml)	None
17A	Oxidation	30% H ₂ O ₂ (0.25 ml)	None
18	Oxidation	None	O ₂
19	Oxidation	30% H ₂ O ₂ (0.25 ml)	O_2
20	Reduction	Na-Formate (0.5 M)	Ar
21	Reduction	Hydrazine (0.5 M)	Ar

Table 3.3. Non-Irradiated Test Conditions and Reagent Schedules for Project 3B.

Table 3.4. Effect of Anatase on Iron Remediation using 254 nm UV radiation and O₂.

Experiment No.	TiO ₂ Amount	% Fe Remediation	
5	0 g/l	0.31	
10	0.2 g/l	6.10	
11	2.0 g/l	6.24	

Table 3.5. Effect of H_2O_2 on Iron Remediation using 254 nm UV radiation and O_2 .

Experiment No.	H ₂ O ₂ Amount	% Fe Remediation	
5	0 ml	0.31	
7	0.25 ml	28.8	
8	1.25 ml	32.2	

Table 3.6. Effect of UV wavelength on Iron Remediation using 0.25 ml H_2O_2 and O_2 .

Experiment No.	UV Wavelength	% Fe Remediation	
6	185 nm	32.0	
7	254 nm	28.8	
9	365 nm	23.0	

Table 3.7.	Effect of UV	Wavelength on	Iron Rem	ediation [•]	without	Chemical Addition.	

Experiment No.	UV Wavelength	% Fe Remediation	
1 185 nm		0.16	
2	254 nm	0.66	

Experiment No.	Reagent	Condition	% Fe Remediation
3	H_2O_2	No O_2	31.8
7	H_2O_2	O_2	28.8
4	TiO ₂	No O_2	8.05
10	TiO ₂	O_2	6.10

Table 3.8. Effect of O_2 on Iron Remediation using 254nm UV radiation and H_2O_2 or TiO₂.

Table 3.9. Effect of O_2 on Iron Remediation using H_2O_2 in the Absence of UV Radiation.

Experiment No.	Condition	% Fe Remediation	
17	No O_2	34.7	
19	O ₂	30.6	

Table 3.10. Effect of 254nm UV on Iron Remediation under Different Conditions.

Experiment No.	Conditions		% Fe Remediation
3	H_2O_2	UV	31.8
17	no O ₂	no UV	34.7
5	no H_2O_2	UV	0.31
18	no H_2O_2 O_2	no UV	12.2
7	H_2O_2	UV	28.8
19	$\begin{array}{c} H_2O_2\\O_2\end{array}$	no UV	30.6

Table 3.11.	Effect of Differen	t Photochemicals on	SO ₄ ²⁻ Remediation	with Ar-Sparging.
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Experiment No.	Conditions	% SO ₄ ²⁻ Remediation
12	0.5 M Formate	6.7
13	0.5 M Hydrazine	9.2
14	2 g/l Anatase	2.3
15	0.5 M Formate 2 g/l Anatase	2.9
16	0.5 M Hydrazine 2 g/l Anatase	5.4

Experiment No.		litions	% SO_4^{2-} Remediation
12	Estimate	UV	6.7
20	Formate	no UV	0.34
13	TT 1 '	UV	9.2
21	Hydrazine	no UV	0.52

Table 3.12. Effect of 254nm UV on SO₄²⁻ Remediation with Ar-Sparging.

4. QUALITY ASSURANCE/QUALITY CONTROL

The major purposes of this MWTP project were identifying photolytic processes that could be used for the remediation of acid mine drainage waters and evaluating the processes to assess their scientific feasibility via determining reaction efficiencies so that recommendations could be made to continue this research effort. The programmatic and regulatory setting in which the project quality assurance was conducted was Category IV as outlined in MWTP Activity IV, Project 3B QAPP (Ref. 4). Projects are designated Category IV when they are used to produce results for the purpose of assessing suppositions. Existing background data presented in Section 2 - Photochemistry was not required to conform to any criteria. This information is considered common knowledge since it was predominantly the foundation to the workplan (Ref. 3).

4.1 QA/QC Objectives

The Quality Assurance/Quality Control (QA/QC) objectives outlined for the project were specified to generate acceptable data. The MWTP Activity IV, Project 3B QAPP (Ref. 4) was provided to insure:

- C measurements were appropriate for achieving project objectives,
- C quality control procedures were sufficient for obtaining data of known and adequate quality, and
- C such data would be defensible if technically challenged.

Ultimately, it would be desirable to show that the selected photolytic technologies for the remediation of acid mine drainage waters yielded concentrations below the U.S. EPA Drinking Water Standards. However, as noted in Section 2.3 - Experimental Results, pH control was conducted at too low of a pH for adequate precipitation of the iron thereby causing interference problems for the detection and quantification of arsenic concentrations (see Section 6 - QA/QC activities). Furthermore, the use of oxygen gas appeared to cause a mixed potential to develop which prevented the high redox potential of hydroxyl radicals from being reached. This was used to explain why manganese remediation was not observed in this investigation as opposed to a preliminary study (see Ref. 81 and Section 6 - QA/QC Activities). Nevertheless, project objectives were to identify and then evaluate appropriate photolytic processes that remediate the wastewater, not necessarily achieve the Drinking Water Standard. This task would be reserved for future studies and accordingly recommended if such concentrations were obtained.

4.2 Analyses

Berkely Pitlake test solutions were monitored for iron, manganese, arsenic and sulfate concentrations as well as for pH conditions. Only U.S. EPA-approved methods were employed.

4.2.1 Procedures

U.S. EPA-approved methods (Ref. 88-90) included Electrometric Measurement (Method No. 4500) pH, Determination of Inorganic Anions in Water by Ion Chromatography (Method No. 300.0) for sulfate concentration measurements, and inductively coupled plasma spectroscopy (Method No. 6010A) for iron, manganese and arsenic concentration measurements. Electrometric measurements for pH were conducted in the reaction vessel every hour. The pH was controlled at pH 3 for photo-oxidation experiments using drops from NaOH or H_2SO_4 solutions, as needed. However, for photo-reduction experiments, the pH was controlled at pH 6 using drops from NaOH or HNO₃ solutions, as needed. Sulfate concentrations were determined by first diluting a sample with a matrix of

deionized/distilled water (usually 1:20) and then taking and injecting a 1-ml aliquot sample into the ion chromatograph. Because the photoreduction experiments were conducted at pH 6, the deionized/distilled water had no effect on the sample. Samples may have been stored temporarily in 20 ml plastic vials between measurements. Equipment manufacturers and types are specified in Section 3 - Treatability.

4.2.2 Calibrations

pH meter. For photo-oxidation experiments, buffer solutions at pH 1.0 and 4.0 were used in the standard two-point calibration of the pH meter. For photo-reduction experiments, buffer solutions at pH 4.0 and 7.0 were used. The buffer pH values bracketed the pH control that was required. The pH meter was recalibrated after every 20 measurements and at the conclusion of every test. Percent slopes were consistently found to be $100\% \pm 5\%$. Measurements of pH were non-critical to all tests. **Ion chromatograph.** Before every photo-reduction test, a blank and sulfate standards were used to establish working curves between 0 and 1000 ppm. This calibration range bracketed all sulfate concentrations measured but required aliquots to be diluted by at least a factor of 10; normally, a diluition ratio of 1:20 was used. Calibration curves were analyzed by PeakSimple data software (SRI Instruments) using R²-correlation coefficients. In this regard, R²-values typically measured 0.97 which was consistently greater than the 0.90 acceptance criterium. Although never encountered, the ion chromatograph was to be recalibrated if a standard, upon being checked after every 20 measurements, was outside 75-125% linear range. Sulfate measurements were critical to all photo-reduction tests but were non-critical to the photo-oxidation tests.

ICP Spectrophotometer. Before every photo-oxidation test, arsenic, manganese and iron standards of 0.1, 1.0, 10 and 50 ppm were used to establish working curves. This calibration range bracketed all concentrations measured but required samples to be diluted with a 5% HNO_3 matrix by a typical factor of 10 depending on which element was being analyzed. Instrument detection limits (IDL) were determined to be 0.052, 0.162 and 0.003 ppm for As, Fe and Mn, respectively. This met acceptable criteria. These concentration measurements were critical to all photo-oxidation tests.

5. FIELD SAMPLES

Berkeley Pitlake water measuring 5 gallons was collected and transported to the ELC Building at Montana Tech by the Montana Bureau of Mines and Geology. The water was obtained from the 200-foot depth (i.e., deep Berkeley Pitlake water) and stored in a refrigerator to help maintain freshness throughout the duration of the QA/QC work. Aliquats measuring 150 milliliters (ml) were taken from this sample for each of the 21 experiments. All experiments were conducted with reagent grade chemicals named earlier with the industrial supplier (see Section 3 - Treatability).

6. QA/QC CHECK PROCEDURES AND ACTIVITIES

6.1 Check Procedures

Numerous procedures were in place to assure that quality data was reported. These check procedures included

- recalibrating the various instruments used through the course of the tests as described in Section
 4 Quality Assurance/Quality Control,
- C analyzing calibration standards periodically to assure the various instruments were functioning properly as also described in Section 4 Quality Assurance/Quality Control,
- C measuring reagent blanks periodically to make sure the various instruments were not contaminated thereby giving false readings,
- c running a duplicate sample to assure the data was reproducible,
- c running a second duplicate sample in the dark to verify effects of UV radiation,
- C matrix-spiking a test to to assure the various instruments were functioning properly thereby yielding results within 75-125% recovery,
- C using laboratory fortified blanks for determining acceptable performance of the ion chromatograph,
- C establishing proficiency on the ion chromatograph by measuring 4 equally prepared aliquots, calculating average % recoveries, standard deviations, and upper and lower control limits, and by comparing results to values found in the accuracy and precision table found in Determination of Inorganic Anions in Water by Ion Chromatography (Method No. 300.0), and

C verifying inter-element interference and background correction factors for the ICP. Only two of these QA/QC check procedures were found to fail. Corrective actions were taken and are described in the ensuing section.

6.2 Activities

During the course of the QA/QC experiments, only two problems were observed which required QA/QC activities. These activities involved ICP procedures:

- C Early on, photo-oxidation experiments were conducted and all QA/QC criteria would pass except one; recovery calulations following the analysis of matrix spike solutions would be <20%. Because acceptable criteria is 75-125%, a matrix effect was suspected. It was found that 2% HNO₃ standards were being used while samples were being prepared with 5% HNO₃. Standards at the higher acid concentration were then obtained and the problem was remedied, and
- C Throughout, photo-oxidation experiments showed arsenic concentrations to be zero at the start and finish. Inter-elemnt interference with iron was suspected due to the high concentration of iron in the initial and final solutions. Because this problem could not be overcome, a request was written to and accepted by EPA to remove arsenic from the critical measurement list. Nevertheless, arsenic concentrations were non-critically measured through the all of the QA/QC work. At the same time, a request to EPA was made and accepted to also remove manganese from the critical measurement list. This activity was needed because manganese concentrations, unlike in the preliminary studies, was not being remediated and goals were thus not being obtained. Reason for this behavior was attributed to oxygen (i.e., samples were bubbled with oxygen) causing a lower-than-desired potential to develop between oxygen and water. Presumably, hydroxyl radicals, with water and in the absence of oxygen, should

produce a higher potential and cause manganous cations to oxidize and precipitate as pyrolusite.

In addition to solving these two problems, QA/QC activities were taken to develop a better understanding of what happens when photochemical reactions are induced in Berkeley Pitlake water, especially since early conclusions were being drawn that suggested not to use photolysis for its remediation. In this regard, it became apparent that two experiments needed to be conducted, one in the absence and the other in the presence of UV radiation, for kinetic analysis. These two experiments were conducted using QA/QC protocol but are not listed in the QAPP (Ref. 4). Appendix A and various tables in Section 3 show these experiments to be Experiments 3A and 17A.

7. CONCLUSIONS

7.1 Summary

Photo-oxidation experiments of Berkeley Pitlake water were conducted to remediate ferrous (Fe²⁺), manganous (Mn²⁺) and arsenate (AsO₄³⁻) ions with anatase (titanium dioxide, TiO₂) and hydrogen peroxide (H₂O₂). Ferrous and manganous ions were expected to be removed by their oxidation to ferric and manganese(IV) and subsequent precipitation as ferrihydrite and pyrolusite, respectively. On the other hand, arsenate remediation was expected to occur via adsorption at the surface of the precitated ferrihydrite. In addition, photo-reduction experiments for sulfate remediation were conducted using strong reducing agents of sodium formate (NaCOOH) and hydrazine (H₄N₂) in the absence and presence of the anatase (TiO₂) in hopes of producing sulfide (S²⁻) for the additional remediation of additional mobile toxic constituents such cupric (Cu²⁺), zincic (Zn²⁺), and cadmous (Cd²⁺) cations via their precipitation as sulfide compounds. Reaction efficiencies were calculated and compared as remediation percentages for all experiments.

Results showed that sulfate photo-reduction worked but, under the conditions examined, was not 100% effective. Photo-reduction the dissolved photochemicals proved to work best with hydrazine and formate yielding 9.2% and 6.7% remediation, respectively. When hydrazine and formate were used simultaneously with anatase, remediation percentages decreased to 5.4% and 2.9%, respectively. Anatase, by itself, only yielded 2.3% remediation. Consequently, it is concluded that the presence of anatase, as a solid photocatalyst, with either hydrazine or formate, as dissolved photochemicals, is detrimental to the homogeneous photolysis processes. Although sulfide formation was never observed, it is clear that photo-reduction of sulfate is possible with both homogeneous photolysis and heterogeneous photocatalysis.

By comparison, ferrous photo-oxidation could be 100% effective but was found to be dependent on the conditions applied, especially pH. Results indicated that homogeneous photolysis with hydrogen peroxide worked better than heterogeneous photocatalysis with anatase yielding 28.8% remediation versus 6.1% remediation. Higher dosages of either photochemical yielded only marginal improvement in remediation. Further experiments showed that photolysis with hydrogen peroxide improved with decreasing wavelegth, but was actually best in the absence of UV radiation. This surprising result was attributed to bubbling in oxygen during the experiments as well as to not adding the photochemical continuously and observing a side reaction for only the UV-assisted experiments. The side reaction was further attributed to photo-oxidation of organic species. Oxygen bubbling was believed to have created a mixed potential which lowered the solution potential (E_H) in the experiments below the potential required for manganous oxidation to occur. In this regard, manganous concentrations were not observed to change and its measurement was therefore removed from the critical list. Unfortunately, the selected pH condition of 3 was too low to observe adequate ferrous remediation. Iron concentrations in solution therefore remained high and interfered with the arsenic concentration measurement by ICP. In this regard, arsenic concentrations were unable to be determined and its measurement was also removed from the critical list.

7.2 Recommendations

Sulfate photo-reduction was shown to occur but only yielded a maximum of approximately 10% remediation. Ferrous photo-oxidation was also shown to occur but, due to the low pH conditions

studied, yielded no better than 35% remediation. Clearly, both of these processes are promising but require further investigation to improve upon reaction efficiencies as well as rates.

The sulfate photo-reduction process is appealing because it represents an opportunity to produce sulfide and there by induce the remediation of numerous heavy metal cations via their precipitation as sulfide compounds. On the other hand, the ferrous photo-oxidation process is appealing because it can simultaneouly remediate manganous and arsenate species. The remediation of manganese via this technique would establish a process where the pH does not have to be adjusted to pH 11 as required by the two-stage lime addition process which, at this time, is the best-determined available technology (BDAT) for remediating Berkeley Pitlake water (Ref. 7). In this regard, this technique could eliminate the second stage and yield substantial savings of lime.

This would require determining the effect of, for examples, pH, oxygen, continuous photochemical addition, and wavelength on the two processes. Different research areas would also include examining other solid photocatalysts, dissolved photosensitizers, other mine waste waters, concentrations of mobile toxic constituents, sparging gases, temperatures, and UV intensities. ZnO, WO₃, CdS, SiC, Fe_2O_3 , and certain zeolites, for examples, would be great photocatalysts to study. Humic acid and oxalate could be interesting photosensitizers for examining. CH₄, CO, H₂, O₃, and CO₂ are excellent candidates for changing atmospheric conditions. Temperatures ranging from near-freezing to nearboiling should be examined to mimic changing conditions observed in cold and hot climates. Finally, UV intensities could be adjusted, for example, from the 600 FW/cm² used in previous studies (Ref. 1,2) to the 16,000 FW/cm² used in this study. Other intensities (and wavelengths) could be obtained from a variety of different sources including lamps, arcs and lasers. All of these options should be examined and are therefore recommended for further studies.

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Appendix A

Remediation Percentages

Experiment No.	UV Wavelength	Photolytic Reagent Concentration or Amount	Sparging Gas	% Fe Remediation
1	185nm	None	None	0.16
2	254nm	None	None	0.66
3	254nm	30% H ₂ O ₂ (0.25 ml)	None	31.8
3A	254nm	30% H ₂ O ₂ (0.25 ml)	None	30.2
4	254nm	TiO ₂ (2.0 g/l)	None	8.05
5	254nm	None	O_2	0.31
6	185nm	30% H ₂ O ₂ (0.25 ml)	O ₂	32.0
7	254nm	30% H ₂ O ₂ (0.25 ml)	O ₂	28.8
8	254nm	30% H ₂ O ₂ (1.25 ml)	O ₂	32.2
9	365nm	30% H ₂ O ₂ (0.25 ml)	O ₂	23.0
10	254nm	TiO ₂ (0.2 g/l)	O ₂	6.10
11	254nm	TiO ₂ (2.0 g/l)	O ₂	6.24
17	None	30% H ₂ O ₂ (0.25 ml)	None	34.7
17A	None	30% H ₂ O ₂ (0.25 ml)	None	32.8
18	None	None	O ₂	12.2
19	None	30% H ₂ O ₂ (0.25 ml)	O ₂	30.6

 Table A.1
 % Fe Remediation Determined by Photo-Oxidation Experiments.

Experiment No.	UV Wavelength	Photolytic Reagent Concentration or Amount	Sparging Gas	% SO ₄ ²⁻ Remediation
12	254nm	Na-Formate (0.5 M)	Ar	6.7
13	254nm	Hydrazine (0.5 M)	Ar	9.2
14	254nm	TiO ₂ (2.0 g/l)	Ar	2.3
15	254nm	TiO ₂ (2.0 g/l) Na-Formate (0.5 M)	Ar	2.9
16	254 nm	TiO ₂ (2.0 g/l) Hydrazine (0.5 M)	Ar	5.4
20	None	Na-Formate (0.5 M)	Ar	0.34
21	None	Hydrazine (0.5 M)	Ar	0.52

 Table A.2
 % SO₄²⁻ Remediation Determined by Photo-Reduction Experiments.

Appendix B

QA/QC Data

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Analyze calibration standard (ICV) Acceptable Criteria measured cone. true v As 1.039 Al 18.87 Min 1.604		the second			2.0.6 11011220				
cptable (on standard	(ICV)			Matrix spikes	Kcs			
	ia	10%			Recovery	15% - 125%		%R = 100 * (S-U)/C	U/C
	measured conc.	true value		0/0		Hnewitz (11)	Calle / CV		i i
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	+001	LUC I		0.72	Mn	0.05184	0.07215	0.0194	101
2	0/ C A			4,19	Lc	0.2076	0.2735	0.036	77
2W	505.2			0.87	Mg	B.D.L.	B.D.L.		
5	496.5	500.002 ppm		-0.70	Ca	B.D.I.	B.D.L.		
Section 8.3,					Section 8-1				
Method blank					Analytical duplicates	dublicates			
Acceptable Criteria	ia	N/A			RPD	<= 20%		RPD = 100 * (C1-C2)/(C1+C2)/C2	CJ+1J)//CJ-1
-									1
	measured conc.	CRD.L.				CI	C2	RPD %	
As	B.D.L.	0.01 ppm	1		AN	B.D.L.	B.D.L.		
AI	11060.0	0.20 ppm	LI LI		AI	0.08282	0.05605		
Mn	B.D.L.	0.015 ppm			Mn	0.05184	0.05159	0.48	
10	18650.0	0.10 ppm			Fe	0.2076	0.2061	0 73	
3IN	B.D.L.	5.00 ppm	n		Mg	B.D.L.	BDL.		
Ca	B.D.L.	5.00 ppm	=		Ca	B.D.L.	BDL.		
Section 8 6 1 1									
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Control of Carl					Calibration	Calibration blank (CCB)			
		10%0		-	Acceptable Criteria	Criteria			
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1	44 Method Blank 1	/1.5	1\$3.096	7.106		B.D.L.	ppm	2/ 2/97	15.27.1
1	44 Method Blank 1	Al	396.152	14940		0 19014	pren	5/14/97	15:07.3
1	44 Method Blank 1	Ma	257.61	H(17		BEL	pj.en	2/14/95	15-28-1
1	44 Methoc Blanc 1	Fe	239.94	2132		0.03981	ippus .	2/14/971	15 28 4
1	44 Method Band 1	Mg	279.679	906.8	-	BUL	ppre	2/14/9/2	17.29.1
1	44 Method 3 and 1	Ca	317.933	4676		BUL.	plum	2/ 14/9 /	10.20-1
E	10 LCS (CCV)	Fa	193.695	173.1		41,4542	ទព្វព	2/14/97	12.513
1	10 LCS (CCV)	AJ	396.152	149200		9.62	ppm	2/14/97	12:114
1	10 LCS (CCV)	Nin	257.01	64270		0.76.34	liten	214.97	12.0
1	10 LC5 (CCV)	Ге	259.94	\$9660		5.007	ppan	2/14/97	12.03
1	10 LCS (CCV)	Mg	279 079	23-209	1000	248.4	blaa	21429	12:10
1 10	10 LCS (CCV)	Ca	317 933	2590000		233.5	jqar.	21437	12.33
	1 254ma 30%H2C2 5k		193 696	23.80		R.D.L.	t but	2'14'57	12.34:3
	1/254wa 30%iH2C2 5K	A ferror of the second se	395 152	14830		0.08282	the second s	21457	12:35:-
	1 254am 304(1)2C2 5K	statements of the local data and the	257,61	5698	-	C.03184	Ebu.	2'14'57	12:36:0
	1 254am 30%d 12C2 5K	Committee of the other discovery	259,94	2094		0.2075	t.bu,	2'14'57	12:36:2
	1 254am 30%11202.5K		279.079	1030		the second s	Ebai	the second se	
	1 254am 30%41202 5K		317.933	5429		F.DL.	ורכן:ן	2'14'97	12:30:+
1.5.4	2 254mm 30%d 1202 5K	Contraction of the second s	193,676	2429		B.DL.	libar	2.14.97	12:371
	2 254nm 3044 202 5k		396.152	14450		F.DL.	lilsai	2.14.971	12.58.5
	2 254nm 3056H202 5K	A CONTRACTOR OF A CONTRACTOR OFTA CONTRACTOR O	257.5	5676		0.05605	[i]+n	2.14.97	12.39.3
	2 254nm 3054 12:02 51		259.94	and the second se		0.05159	<u>likus</u>	2.14.97	12.392.5
	2 254nm 3054 12:02 51		and the second se	5057		0.2051	, inclut	\$14.97	12 40:2
1	2 254nm 30%4 1202 5K		279.079	977.0	_	H.D.L.	ppna	2.14.97	12 40.3
1	3 254nm 30%H2O2 5K		317.935	5272:		H.D.L.	incici	2:14:97	12 40 5
1	the state of a fillent of the stration of the first or the last of the		103,696	25.33	20	B.D.I.+	19501	2/14/97	12 42 4
1	2 25 4rm 30%H2O2 5K		306,152	14590		0.005351	1000	2.14.97	12 43 2
1	3 254mi 30%H2O2 5K		257.61	7505		0.07215	Titom	2.14.97	12.43.4
- 1	3 254nm 30%H2O2 5K		259.94	6203		0.2735	91000	2/14/97	12.44 1
1	2 254nm 30%H2O2 5K		279,075	944.8		B.D.L.	12 103	2/14.97	12:44.3
1	3 254 nm 30%H2O2 5%		317.933	4465	1.1.1.1	B.D.L	12.008	2/14/97	12.44.5
1	4 254mm 30%212O2 5%		193.596	22.77	4X 3	B.D.L	- Eau	2.14.97	12.46.30
1	4 254nm 30%H2O2 5%		396.152	13540	4X	B.D.L	lister	2.14.97	12.47.13
1	4 254mm 30% 12O2 5%		257.61	2201	4X.	0.01279	labor .	2:14/97	12.47.43
1	4 254mm 30%H2O2 51		256.94	2436	4X	0.05704	japer	2/14/97	12.48.03
1	4 254mn 30%112O2 5K		279.070	\$39.9	4X	B.D.L	open.	2/14/97	12:44:2
1	4 254nm 30%H2O2 5K		317.053	3524	4X	BD.L.	spra	2/14/27	12.48.43
1	5 real spike cone.	A	193.696	-0.33(0)		13 D.1	opita	214.27	12.50.2
1	5 real spike cone.	Al	396,152	62980		5.491	opin	21-17.	12.5.11
1	5 real spike cone.	Fe	259.94	153900		\$.664	ppm.	2/1-/27	12.5 .5
1	5 reat spike conc	Mg	275.079	700 1		0.01865	ppen	21+97	12:52:17
1	5 real spike cose	Co	317.933	\$260		0.05929	րրու	2114-07	12:52:34
1	S real sp ke conc.	1.4n	257.61	42530	4X	0.4859	1.944 ppm	2/14/07	2:55:53
1	10 CCV1	As	193.656	173.1		0.5157		2/ 4/97	2:57:51
1	10 CCVI	A	396.152	139700		9.818	PI-1%	2/ 4/97	2:58.34
1	10 CCV1	Ma	257.61	59430	_	0.7724	ppm	20 4/97	2.58.58
1	10 CCV1	Fe	250 04	77810		4.756	ppm	2: 1/07	12:39:20
1	10 CCV1	Mz	279.670	214100		21).2	bbur	21197	12:59:40
	III CCVI	Ca	717.933	2430600		237.4	6.0	21407	12:50:50
I.	I CCBI	AS	.93.696	17 8]		B.D.L.	[film	2/14/97	13:01:4-
1	1 CCBI	AI	396 152	1.680		B.D.L.	EL.D.		
1	LICCRI	Ma	257.61	1242		the second se	bhu	21147	13:02:27
	I CCBI	Fe	252.94			R.D.L.	Link	211/07	12.02.51
1	110080	the second se	279.079	1613		R.D.L.	Lbo.	2.11.97	13:03:14
1	I CCB1	Mg	the state of the s			B.D.L.	11.66.	21197	13:03:33
		Ca	517533	4082		B.D.L.	[13ao:	2 11-97	13:03:32
1	6 254nm 30%412O2 90n		193 695	1411		4 411	1.000	214.97	15:13:01
1	6 254 nm 30% 412O2 90n		.96 152	4284001		252.8	"Islaut	2/14/17	13,13,14
1	6 254am 30%d120/2 90n			1.68107	4 1 A	226.4	Jilan	2 14 17	15 14.08
1	6/254nm 30%d12C/2 90n			1.141-+017		58 .4	Librar	2 14 07	15 14 - 8
1	0/254nm 30%d12C2 90m	and the second s	279.079	\$0.5400		469.2	(pp.us		15 15.37
1	6 204nm 30%H2C2 90m		317.933	427.8400		455.5	0000		15 Brox
1	0-254nm 30%812C/2 50m		259.94	70400	10JX	8 305	\$30 S ppm		15 19:50
1	5 254nm 30%d (2C2 50m	the second se	257.61	15210	539X	0.5310	255 9 ppm	and a second	15 2315
1	7 Berkeley Pi: Water	As	193.696	2211		6.81.5	140.00		15 25 1 1
1	7 Barkeley Pi. Water	AJ	395.132	3\$82000		235.6	ppm	2.11.47	15 25 44
1	7 Berkeley Pi, Water	Ms	279.079	40.5400		427.6	เกิดกา		15.77 17

1	7 Barkeley Fit Water	C ₄	217.933	4909000		410.8	ppia	214 97	15 28:1
1	7 Berkeley Fit Water	Fe	257.94	2-9000	100X	12.17	1217 ppm	2.148.7	13 31 3
1	7 Berkeley Fit Water	Min	257.61	20500	50ELX	0.4847	241.6 jpp.t/	2/14/57	15.35.0
11	8 185/254cm 90min	135	193 696	2130		G 819	ppin	×142.7	15 37 0
1	8 185/254rm 90min	Al	-96 157	39800001		242.2	ta t	214-57	15 37 4
1	8 185/254cm 90min	Mg	279 079	492900		456	pesia	2/14/57	15.39.3
1	8 185/254cm 90mm	(Ca	317 933	4071090	S. 1	430.6	12.200	2/14/57	15 10 1
1	8 185/254cm 90mm	Fe	252.94	2546-90	100X	12.44	1244 prom	2/14/57	15 43 5
1	8 185-254rm Wimin	Min	257.61	54060	500X	1.52	250 pom	2/14/57	15 47 0
1	9 254mn 90min	1.0	193 695	212.		6.635	poni	21457	15 49 0
1	9 254nm 99min	A	396.152	38030-00		230.4	inc.dl	2/14/97	11 49 4
1	9 254nm 90min	Mg	279.079	467700	-	431	prairi	2/1+/07	15 31 7
1	9 254nm 90min	Ca	317.933	3972000		418.4	point	2/14/97	15 32 1
1	9 254nm 90mm	Fe	252.94	2-7500	100X	12.09	1209 (pom	2/14/97	15 55 5
1	9 254nm 90mm	Mn	257.61	52410	500X	0.5034	256 [200	2/14/97	15.59.0
1	10 254am 1iO2 90min	41	193 695	205		6.448	10.00	2/14/07	16.01.0
	10 254 am Ti O2 90 min	1	266 152	\$ 76 50.10		277 N	12:001	2.14.97	46-01 4
11	10 254nm TiO2 90min	Mg	279.079	475630		438.1	(pana)	2/14/04	In US 4
-	10 254am TiO2 90mia	G	517.933	49374110	0.0	420.2	11101	2/14/97	16304-1
1	1012 \$4am TiO2 9(mi.)	7.	259,94	229230	1003	11.10	1119 pom	2/14/97	10:07.5
1	10/254am TiO2 90mia	Mn	257.61	30059	500X	C. 4787	239.4 (100)	2/14/97	16:11 0
1	46 Mathoy Blank 3	45	103.695	26.11		B.IAL	10,000	2/14/97	10.131
1	46 Methoc Blank 3	01	356.152	4740		B.D.L.	(apart	271.107	10:14:4
1	46 Mathos Blank 3	Mn	257.61	1158	111111	RDL	pper	21:4/95	16:14:1
1	46 Methoc Blask 5	Fe	259.94	1477		B.D.L.	ppm	21,4,95	he fit 5
1	46 Mathine Blank 3	Mg	170.079	869.2		RDL.	(1) (1)	204.95	Me.14.5
1	46 Method Blank 3	Ca	317,533	3202		B.D.L.	pystri	2/ 3/97	10:13:1
1	10 CCV2	As	15.3.696	167.5	Description of	1.4566	Idsur	2/14/97	16:16:5
1	10 CCV2	Al	356,152	136000	20.00	9,536	(your	2/ 4/97	10,17,-
i	10 CCV2	Mn	217.61	\$7730	Contraction of the	0.549	Disur	2/ 4/97	16:18:0
1	10 CCV2	l'e	259.94	75'270	1	4.85	ppm	2/14:97	16:18:2
1	10 CCV2	Vg	279.079	205500		233.7	pipina	j 27 J/97	Re 18.4
-	10 CCV2	105	317.033	2172000	-	235.5	ppun	2/ 4/97	16, 193
1	LCCB2	As	193,096	13.50	1.1.1.1.4	8.D.L.	ppm	X 4.97	16,200
	1/CCB2	AJ	196 152	1440		8.D.L.	ppns.	1 2/ 1/07	16.21:2
1	1 CCB2	Ma	257.61	1139		B.D.L.	רחרען	2/ 4.97	16.21.3
1	1 (CCB2	Fe	259.94	1471		BDL.	ppm	2/ 107	16.22
1	1 CCB2	Mg	270.079	876.1		BDL	ppn	2/ 4.97	16.22
1	100032	Ca	317.933	3231		B.D.L.	ppm	2.49	16 53 1

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Section 7.4				Section 8.5.2.	2			
Analyze ca	Analyze calibration standard (ICV)	(ICV)		Matrix spikes	8			
Acceptable Criteria	: Criteria	10%		Recovery	75% - 125%		%aR = 100 * (S-U)/C	-0//C
	measured cone.	true value	1%		Illueniba (II)	Calborer	1	14 14
As	1.60.1	1 004 ppm	9 26		101 muldeuro	(0) 29140	ACTUAL COTIC	K 74
N	20:45	20.035 ppm	1.0	19	1.0.0	1		
Mn	1.567	1.503 ppm	VC T	Ndra	100100			100 million 100 mi
Fe	10.07	0 035 000	31.0	IIINI	100+0'0	C76000		109
Mo	6162	Ind care	27.0	FC	0.1818		0.085	
12	7.400		0.66	Mg	B.D.L.	BDI.		
5	537.8	500 002 ppm	7.56	Ca	B.D.L.			
Section 8.3.				0				
Method blank	and			200000				
				Analytical duplicates	uplicates			
Acceptible 1.nicria	LINCON	NIA		RPD	<- 20%		RPD - 100 + (RPD - 100 + (CI-C2)/(C1+C2)/2
	measured conc	CRDI						
40					CI	C2	RPD %	
11	0.01.00	uidd 10.0		As	A D.L.	B.D.L.		
	ACTION I	0.20 ppm		AI	0.07102	0.05728		
	B.U.L.	udd cioro		Min	0.04801	16210.0	0.151	
140	0+01010	0.10 ppm		L'r	0.1818	0.1786		
SIN .	0.00.723	5.00 ppm		Mg	BD1.	B.D.L.		-
Y	52200.0	uidd b0.5		E.	B.D.L.	B.D.L.		
Control 8 / 1					-			
CONTRACTO ON			1	Section 8.6.1.2.	12.			
Check standard	dard			Calibration I	Calibration Library of CON			
Acceptable Criteria	Criteria	10%		Acceptable Criteria	interia			-
-	measured cone. (true value	10					
1	10007-0	0 21.3			Incasured conc	C. H. D.L.		
. Iv	1386.0	HILE FROM	- 17.7.	As	BD.L.	mqc 10.0	mdc	
Min		HIGH CHARLE	V+ 1-	IVI	BDI	0.20 ppm	unde	
1.0	10000	uidd 7. 7 ii	806	Mn	BD.L.	0.015 ppm	bpm	
		udd on c	-5 08	FIC.	3D1.	0.10 ppm	under 1	
80	1.877	250.41 ppm	16.8-	Mg	3 D.L.	A OULDER	1	
	10 20	Territor and					and a start of the	

Page 1

esults expo	orted from Varian LIBERTY				-			-
esult File	TA.CAQC215					1	4	
ulpul Fort	and the second state of th							
latch Samp								
and the second se		-						
latch Prog		-				10000		
latch Elem	and the second se					1	1	
ate and Th						1	3	
eport Mad	e ALL DATA	-				1	u.	
eport Mad	e = ALL DATA, Date and Time = YE	S			Cone Dilate Co	. It was	Daty 1	ine
ack#	Tube" Samp.Lab.	E.	and the second s	Litens			215.97	19.28
1	1 ELANK	As	193.696	.0.01	0	para	the second se	
1		Al	396.152	7884	0	(para	3'15'9'	19.2%
1		Min	257.61	603.7	0	para	215.97	19 29
1	1 ELANK	Fe	259.94	927.5	0	para	215.97	10.29
	and the second se	Mg	279.079	424.6	0	para	2'15.97	19.29
1		Ca	317.933	1666	0	para	2/15/91	19.30
1		the second se	93.696	40.87	0.1	[DDF]	2/15/97	19.51
1	2 STANDARD I	As		48500	2	ppro	2/15.91	19.32
1	2 STANDARD I	Al	J96.152	and a local data of the second s		the second second	2/15/97	19.32
1	2 STANDARD 1	Mn	257.61	16900	0.15	ppri	2/15/97	19.33
1	2 STANDARD 1	F:	259.94	23710	1.311	bbea	and the second sec	19.33
]		Mg	279,079	61340	49.95	bbu	2/15/97	
1	2 STANDARD 1	Ca	\$17,933	481300	49.97	ррия	2.15.07	19.34
	3 STANDARD 2	10	1\$3.696	166.3	0.5	pom	2 15/97	19.35
	3 STANDARD2	Al	356.152	151800	9,999	ppus	2/15/97	19.3
	and an international and a second sec	Mn	257.61	75950	0,7495	ppus	3 15/97	19.4
	3 STANDARD 2	Fe	259.94	106500	3.05	145003	1.15.97	19.33
1	3 STANDARO 2		- transformer and the second state of the local second sec	289800	2.98		2/15.97	19.3
1	3 STANDARD 2	Mg	379.079	the second se	and the second sec	ppin	2.15.97	9:3
1	3 STANDARD 2	Ca	317.933	2266000	2-9.9	Dous	- A Local Control of State	9:5
1	4 STANDARD 3	As	193.696	299.1		Dun	215,97	
	4 STANDARD 3	AI	356.152	347300	20	Filmo	2.15.97	9:1
-	4 STANDARD 3	Ma	257.61	143060	1 1 1 0 0	000	2/15/97	9:4.
	4 STANDARD 3	Fe	259.94	194600	10.11	16000	2 15.97	4.4
	the second se	Mg	279 079	544500	499.5	130401	2:15.97	V.4
	4 STANDARD 3	and the second se	317 933	4145000	499.7	[ijan)	2:15.97	16.4
1.10	4 STANDARD 3	Ca	396 152	7261000	501.7	រកុទ្ធន	215.97	9.4
10	5 STANDARD 4	Al			the second s		2/15 97	14
	5 STANDARD 4	Fe	259.94	3965000	195,8	Tibut	2 15.97	24
	6 STANDARD 5	A3	193 696	15\$10	541	[tbur	2 15 97	.9.4
	7 107	As	193 696	5.58 5	1.877	¹ I:Date		
) K.V	1	396.152	3790001	20.45	(Ppm)	2/15/97	19_4
	1 3 ICV	Mr	257.51	1-7700	1.557	(fbm	2 15 97	19:4
		Fe	259.94	208900	10.071	(ppm)	2/15/97	19.4
		Mg	279.075	577600	554.2	il:faur	2115:97	19:5
	and the second se	Ca	317.933	1399000	\$37.8	(rpm)	215.97	19:5
	I I KIV		193.696	18.92	8.D1	irpm	2 15 97	19:5
	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	1/15			B.D.L.		2/15/97	19:5
	1 1 ICB	14	396.152	8161	the second se	T.Dui	215.97	19:5
21	1 1 ICB	Min	257.61	6.34.5	B.D.L.	Lbu	and the second s	15:5
	1 1 108	Fe	259.94	1102	B.D.L	tba	21.5.97	
1.	1 1 ICB	Mg	279.079	506	B.D.L	1.641	2/15/97	19:5
10	1 1 ICB	Ca	317.933	2181	B.D.L	(pa)	10 5997	19:5
		As	193.696	the second se	B.D.L	ppm	2 5-97	15:5
	Contraction of the second s	Al	396.152	the second	B.D.L	plan	2/ 5/97	15:5
	1 3 CRH	Mn	257.61	and a rest of the second se	0.03572	ppn	1/ 5/97	15:5
	1 1 CRII	and the second se			0.01862	10.0	2 5.97	15.5
	1 1 C30	Fe	259.9-	and the second se	B.D.L.	+ + . · · · · · · · · ·	1 2' 597	15.5
1	1 \$ 2311	Mg	279.079	Contraction and a second se	the second	libin	1 5.97	14.4
	1 1 10.001	Ca	317.933		B.D.L.	(J-D-ar	2 5 97	21.1
	1 S ICSAI	AR	193.696		11.09%5	a dd	2 5 97	203
	I SICSAI	Al	396.152		510.5	- libu		
	1 5 ICSAI	Ma	257.61	1696	0.01001	ippn	2 597	200
	I SICSAI	Fc	259.94	386800K)	105	[hhan	2'15'97	20st
-	I S ICSAI	Mg	275.079	53-40000	\$40.7	ippm	215.97	260
	1 ilCSAJ	Ca	317.93)		524.4	ppan	2 15 97	2set
	A Design of York	As	193.696	the set of	B. H.	htm	2 1 5 97	260
_	1 9 [CSAB1	1. P.	376.152	CARLON OF STREET, STRE	385.8	ppan	31597	200
	1 9 ICSAB1	Al	and the second se	and the second sec	9.4416		21597	2010
	1 9 ICSABI	Mn	217.6	46830	and the second sec	21911	215.97	20 (
	1 FICSABL	Fe	259.94	and the second data in the second	19.6	_blan	1401 (Section 4.1.1)	20.5
	1 9 ICSABI	Mg	279.079	and the second sec	530.9	ppu	21547	1
	1 FICSABI	Ca	317.533	277030	510.5	, ppan	21557	20.0
	1 44 Me hod Blank 1	1.15	193.696	15.55	B D.I.	ppm	21547	20.1
		AJ	396.152		0.06159	plan	215.57	20.1
	1 44 Method Blank I	100		575.6	B.D.1.	(p) (i)	217.57	20.1

1	44 Method Blank I	Fe	259.94	1250	11-11-11-11-11-11-11-11-11-11-11-11-11-	B.D.L.		(III)	2/15/97	2/13.
1	44 Method Blank 1	Mg	279.079	507.6		B.D.L.		1910.1	2/13/97	2014.
1	44 Method Blank 1	Ca	317 931	2742		B D1		in and a second	2/15/97	20.14:
1	10 LCS (CCV)	As	193.696	168		0.5261		pm	2/15/97	2116:
	10 LCS (CCV)	AJ	356.152	189800		9.578		1000	2/15/97	2017:
	10 LCS (CCV)	Mn	257.6:	72800		0.7055		alour	2/15/97	2017.
the second se	10 LCS (CCV)	Fe	259.94	102900		4 939			2.15.97	3118
	a sugar such as a such asuch as a such as a su	- Brown	279 (179	271(000)		Provide the second second		ann	2/15/97	3118
	16 LCS (CCV)	Mg				239		ppm		1.400.000
	10 LCS (CCV)	C;	317 933	2143(000		235.3		opm	2/15-97	3118
1	1 234nm H2O2 1.25 5K	As	153 096	-8.31		0.0 L.		abur	2.13.97	20.20.
1	1 254nm H202 1.25 5K	Al	356 152	\$271		107302		alaut	2/15/97	30.5
1	1 254nm 112:02 1.25 SK	Mn	257.61	5825		3.0+8013	1	alaan	2/15/97	30.5 -
1	1 254nm H2O2 1.25 5K	Fe	259.94	4755		0.1848	1	1941	2/15-97	20.2 :
11	1 254nm H2O2 1.25 5K	Ma	279 079	597.1		BDL		1000	2/13/97	20.22.
1	1 234nm 1/2/02 1.25 5K	Ci	317 933	1086		BDL		ipm	2/13/971	20:22
1	21254nm H2:02 1.25 5K D	As	153 696	11.77		B.D.L		าวกา	2/15/971	20:24
	2 254nm H2O2 1.25 5K D	AJ	196 152	9027		0.05728		11/1	2/15/97	20:25
1			257.61	5817					A	20.25
1	2 234nm H202 1.25 5K D	Ma	And and a second second second	the second se		0,04794		1.16.1	2/15/971	A. (1997) 107 (1997)
1	2 254nm F(202 1 25 5K D	Fe	259.94	4627		0 1786		1963	2/14/97	20.25
1	2 254nm 112:32 1.25 5K D	Mg	279 (179	572,4		B.D.1.	1	on	2/15/3/7	20:26
1	2 254mm 1-202 1.25 SK D	Ca	317 933	2896		B.D.L	1	1111	2/15/97	23:26
1	5 254nm Fi2:02 1.25 5K S	As	193.696	12.8		B.D.L	1	23123	2/15:57	21.28
1	3 254nan H2O2 1.25 SK S	AJ	396.152	9529		0 1985	1	1.11.5	2.14.57	21-28
1	3 254mm 1:202 1:25 5K S	2.13	257.51	8120		0.16925		ant.	21557	21:29
1	3 254nm 1 202 1.25 5K S	Fe	259,94	6430		C.268	110	and and a second	211557	2129
1	3 254mm 1:202 1:25 5K S	Mg	279.075	371.3		D.D.L		(MR)	211257	21,30
	3 254nm 1:202 1:25 5K S	Ca	\$17 931	3132	-	B.D.L		and the selection of th	2/ 1157	23.10
1	to be and a strange of the barry of the barr		193.690	5 599				iyan)	3: 5/57:	2132
1	4 254nm E2O2 1.25 5K L	AS			iv	1.D.G	0.0753	pm		
1	4 254nm E2O2 1.25 SK L	Al	396.152	1094	4X	0.006325	0.0253 p		27.5497	20:32
1	4 254nm H2O2 1.25 5K L	Mn	257.51	1921	4X	0.91211	0.04843 (2/ 5/97	20.35
1	4 254nm H2O2 1.25 SK L	Fe	259 94	1897	4X	0.04651	11186		2' 1671	20.31
1	4 254nm H2O2 1.25 5K L	Mg	279.079	470.2	4X,	0.03625	0.1478		2' 5.97	20:33:
1	4 254nm H2O2 1.25 5K L	Ca	317.933	2195	4X	0.05435	0.2194	pm	2/ 5/97	20:34
	10 CCV1	AS	.93.676	167.2		6.5237		prn	2/ 5/97	20:36
	10 CCV1	Al	196.152	185500		9.052		ipin	1 5317	20.36
	10 CCV1	Ma	257.61	73640		6.7147		pro	1: 5.97	20.35.
	10 CCVI	Fe	259.94	104000		4.987			1: 5:97	20.35
		Mg	179,079	281.700		241.5		pm	2: 5.97	20:37:
	10 CCV1		117.933	21123000		and a second second second second		pre	2.15.97	20:33
	10 CCV:	Ca	A ADD TO THE PARTY OF THE PARTY OF		*****	210		pin		
1	CCB1	As	93.696	12.76		3.D.I.		pm	215.97	20.35
1	CCBI	Al	196.152	7994		b.D.L	E	pin	21597	20.40
1	CCBI	Ma	257.61	6027		0.D.L ;	, P	pia	2.15.97	20.43
1	CCBI	Fe	259.94	975.6	-	I.D.L	P	pitt	215.07	20.11
1	CCBI	Mg	279.079	457.4		F.D.I.		ptit	2/15/97	20.41
1	CCB1	Ca	317.933	1909		E.D.L.	- AG	pau	21597	20.12
1	5 254nm 112()2 1.25ml ()2	As	193.696	1561		5.106	10	pm	2/15/97	20.43
	5 254nm H2O2 1.25mL O2	the second se	305.152	456-1000		282.7		pm	3/15/97	20:44
	the state of the second state of the state o		279.079	529400		Contraction of the local division of the loc			2 15 97	20:46
1	5 254nm H2O2 1.25mL O2					483.5		pru	 	
1	5 254nm H2O2 1 25mL O2	and strange over the strange of the	017.933	4008000	1000	479.3		pru	2/15/97	20:46
1	5 (254nm H2O2 1.25mL O2		259.941	172200	100X	8.287	828.7 0		21597	20:56
1	5 254nm H2O2 1.25mL O2	Ma	257.61	52740	500X	LL 1005 i	210.015	pp.	2-15-47	20:53
1	6 254nm H2O2 0.25mL O2	45	193,696	1522	and the second of	5.037]		pru	2:15:97	20:55
1	6 254nm H2O2 0.25mL O2	AJ	395.152	431 50001	1013	265		prai	2/15/97	20:56
1	6 254nm 11202 0.25mL 02		279.019	515200		469.2		pth	÷15.97	20:58
1	6 254nm H2O2 0.25mL O2		317.033	3970000	1000	173,7		(m)	2/15:47	20:58
1	612:4mm H2O2 0.25mL O2		259.94	180000	100%	8,668	866,1 0		3/15 97	21:02
1	6 254nm H2O2 3.25mL O2		257.61	545-0	503%	0.5.8	255 p		2/15/97	21.05
the second se	the state of the second s	· Production and the second seco	193,595	1486		the second rest of the second sector is a second	and the second se		2 15 97	21.07
1	7 185/254mm H2C/2 0.25m	As		4134000		4.9.9		<u>pn:</u>		
1	7) 185/254nm H3C2 0.25m	Al	305.152			252.31		hu .	215.07	21 08
1	? 1\$5'254nm H2C2 0.25m	Mg	279.079	509500		463.4		kas.	2/15/97	21: 10
1	1 185/254mm H2C2 0.25m	Ca	317.933	3788000		476.4	10	Lu.	2/15/97	21. 33
1	7 185/254mm H2C2 U.25m	te	259.94	154100	100%	B.53.5	838.3 ip	Lat.	2 15 97	21: 4
1	7 185/25 inm H2C2 0.25 m	Ma	251.61	52870	500X	0.5012	251.Cip		2/15/07	21- 7-
1	\$ 254nm O2	As	193.596	2252		7.449		rn:	2/15/97	31: 9:
1	\$ 254nm ()2	Al	196.152	4)17:00		244.2		rn .	2 15 97	21.202
il	\$ 254nm 02	Mg	179.129	507100		4008			2 15 97	21:22;
	the property of the state of th	the second se	and the second se	38(4)(0		to some other shares a second second part of		<u>[]</u>		21.22
1	8 254nm O2	Ca	317.903		(032	1(2.7		liu;	2 15 47	
1	\$ 254nm ()2	Fe	259.94	251900	100X	12.16	12161p		2 15 97	21:26:
1	# 254nm C/2	Min	257.61	\$3710	500X	0 5196	254.8 p	pn:	2 15 97	21:29:
		As	193.596	4.188		B.D.		pre	2 15 97	21040

1	\$ICRI2	\J	326.152	1225	B.D.L.	ppni	2:15:97	21:32:34
1	\$ CR12	Ma	257.61	:645	C.84G35	labup	2:15:07	21:32:55
1	\$ CR12	Fe	259.54	2620	0.08161	ppni	2/15/97	21:33:24
1	8 CR12	Mg	279.079	458.2	B.D.L	ppna	2/15/97	21:35:44
1	\$ CR12	Ca	317.933	2423	B.D.L	ppm	2/15/97	21.31:33
1	5 ICSA2	As	123.656	52.94	0,1405	ppna	2/15/97	21:15:44
1	5 ICSA2	AI.	396.122	6557000	439.2	ppm	2/15/97	21:36:27
1	SICSA2	Ma	257.61	2319	0.01573	ppm	2/15/971	21:37:09
1	5 ICSA2	Fc	259.54	3634000	115.7	ppm	3/15/97	21:37:41
1	SICSAZ	Mg	279.079	541700	503.8	ppm	2/15/97	21:34:00
1	S ICSA2	Ca	317.933	4252000	5 5.1	րրու	2115/97	21:38-15
1	9 ICSAE2	1.8	193.656	-4.1.36	H.D.L.	[][n]	2 15 97	21.40.93
1	9 ICSAE2	AL	336 142	6530000	417.1	10041	0/15/57	21:40:41
1	9 ICSAE2	Ma	257.61	45860	0.431	рраз	2/15/57	21:41:25
i	9 ICSAE2	re	239.54	3053000	124.6	ppen	2/15/57	21 42:31
1	9 ICSA52	Mg	279.079	516600	501.7	Eding)	2/15/97	21:42:21
1	90CSAE2	Ca	317.933	4157000	503	ppm	2/15/57	21 42:40
1	50 MethoJ Blank 7	As	103.656	15.46	11.D.L.	ppm	0/15/57	22:03:50
	50 Method Blank 7	Al	396.152	7752	B.D.L.	ppn	2/15/57	22:04:3.
	50 Method Blank ?	Ma	257.61	754.1	0.301458	ripat	21.557	22.04.5
	50 Method Blank ?	Fe	259.54	957.9	ILD.L.	und	21557	22 (15:11
-	50 Method Blank 7	Mg	279.079	416.8	ILDL	tus at	2/15/57	22105:3
	50 Method Blank 1	Ca	51 1.933	1731	B.D.L	lids at	2/15/57	22 115-5
1	10 CCV2	1.5	133.656	157.5	0,4939	ppn	2:557	22 107:4
N	10 CCV2	/J	396.152	177200	9.265	ido ar	2/15/57	22115:2
11	10 CCV2	Ma	257.61	70690	0.6817	1:1> 41	01447	22.08-5
1	10 CCV2	Fe	259.94	29(140)	4.744	ppar	1 557	2210/1
1	10 CCV2	Mg	279.079	256100	228.1	pp n	2/ 557	22/11/ 3
1	10 CCV2	Ca	317.973	2113000	231.7	1:12.31	2 597	22112.5
1	LICCB2	1.5	193.696	11.64	E.D.L.	(ppa)	2 5 57	22 11 3
1	10032	24	396.132	*631	f.D.L.	Libar.	2 847	22 12:1
1	I CCB2	Mn	257.61	639.3	E.DL.	11(22)	2/ \$\$7	22 12-4
1	1 CCB2	Fe	255.94	977.9	E.D.L.	ppm	2 5/971	22 1 5 11
1	1 CCB2	Mg	279.079	409.1	U.D.L.	rgn	2/ 5/5/7	22 13:2
1	1 CCB2	Ca	317,933	904	E.D.L.	(FD3)	2/ 5/971	22 13:4

					Section 8.5.2.	2.			
Analyze ca	Analyze calibration standard (ICV)	-			Matrix spikes	Kes			
Acceptable Criteria	Criteria	10%			Recovery	75% - 125%		%R - 100 * (S-U)/C	-1/1/
	measured conc.	true value		%		Unsnike (11)	Shike (C)	Actual acres	D. 07
As	1.131	1.004	undq	12.65	As	RDI	B LL I	COUNT COLLC.	K 70
AI	20.01	20.055	bpm	-0.22	Al	0.03418	17/0/0		
Mn	1.581	1.503	pprn	5.19	Min	19650.0	0.0756	0.0101	011
Fe	9,903	9.995	ppm	-0.92	E E	0.1868			211
Mg	514,4	500.828	ppm	2.71	Me	BDT		0000	701
5	510	500.002	ppm	2.00	Ca	B.D.L			
Section 8.3.					Continu 0 1				
Method blank	nk				And History	distant in a second			
Acceptable Criteria	Criteria	NIA			Analytical duplicates	uupiicates			
						0/07		0) * 001 = 0.01	RUD = 100 * (C1-C2)/[(C1+C2)/2]
	measured conc.	C.R.D.L.				CI	C2	RPD %.	
AS	B.D.L.	0.01 ppm	bpm		As	B.D.L.	B.D.L.		
ALC: NAME	19640.0	0.20 ppm	mdd		IN	0.07102	0.05728		
Ea	B.D.L.	0.015 ppm	unde		Mn	0.05264	0.05235	0.55	
	B.D.L.	0.10 ppm	uido		Fe	0.1868	0.185		
Sile.	B.U.L.	00.0	uido		Mg	D.D.L.	B D1.		
3	B.D.L.	5.00 ppm	mqc		B	B.D.L.	B.DL		
Section 8.6.1.1.					0				
Check standard	lard				Section 8.6.1.2.	1.2.			
Acceptable Criteria	Criteria	10%			Calibration	Calibration blank (CCB)			
					Acceptable Cinteria	(, riteria			
	measured conc. (true value				measured on	CDDI		
AS	0.4596	0.502 ppm	md	-8.45	As	B.D.L	0.01 nnm	nom	
AI .	9.465	10.03 ppm	mdi	-5.61	AI	BDI	0.20 ppm	nom	
IN III	F617.0	0.752 ppm	uid	-1.31	Mn	B.D.L.	0.015 ppm	DDDI	
Mu	1076 H	indd 00's	Ind	-1,46	Fc	B.D.L.	0 10 ppm	mdd	
	1	uidd 14'0c7	hu	-5.16	Ma	B.D.L.	5:00 ppm	mdd	
	71767	udd: nn: ncz	und	-7.12	;Ca	B.D.L.	5 00 ppm	mum	···· · · · · · · · · · ·

esul. File	from Varian LIBERTY TAIQAQC215						1	1.11
utput Formal	DIF							
atch Sample La	and the second se			200			-	
atch Program								
atch Elements								- 55
ate and Time	YES							
spon Mode	ALLDATA							
Contractor and the second s	LL DATA Date and Tane	- VPg						
ekf Tube	and the second se	El	W.L	Intens	Conc	Dilute Con Units	Data	ine
1	1 BLANK	As	193.696	22.12	Conc C	protection in the second appropriate the second	2'16'97	18 (0)
1	BLANK	Al	396.152	10230	0	ppm	2/16/57	18 (11
1	BLANK	Ma	257.61	836	G	្រាំក្រា	2/16/97	18.01
1	1 BLANK	Fe	259.94	1140	0	pjan	and the second s	18.02
1	BLANK	Mg	279.079	618.7	0	pçau	2/16/57	18.02
1	IBLANK	Ca	317.933	2203	0	ppm	2/16/97	
	2 STANDARD I	As	193.696	41.16		bbui	2'16'97	18:02
1		AJ	395.152	35230	01	pj:m	2/16/97	
1	2 STANDARD I			and the second se	2	pj:m	and the second se	18:05
1	2 STANDARD I	Ma	257,51	13980	0.15	pl.u.	2'16'97	18:05
1	2 STANDARD I	Fe	259.94	18210	1.011	ppm	2:16:97	18:00
1	2 STANDARD 1	Mg	279.079	44320	49.95	Plux	2:16:97	18:05
1	2 STANDARD 1	Ca	317.933	424660	49.97	biu.	2'16'97	18:05
1	2 STANDARD 2	44	193 696	152.5	0.5	(blaz,	2 16 97	18114
1	3 STANDARD 2	٨l	396.152	121100	9.959	litan.	2'16.97	13:05
1	2 ISTANDARD 2	Ma	257.51	57460	0.7495	1000	2.16.97	15,09
1	3 STANDARD 2	I'e	259.94	80630	5.05	l bbas	2.16.97	15-10
1	3 STANDARE 2	Mg	279.379	209760	249.8	ippro	2/16-97	13:30
1	3 STANDARE 2	Ca	317,933	1968000	249.9	indd	2.16-97	13:10
1	4 STANDARE 3	As	193.596	277.9	1	[pm]	2:16:97	13:12
÷.	4 STANDARE 3	AJ	396.132	219900	20	1 Jan	2:16:97	18:13
4	4 STANDARD 3	Ma	257.61	113100	1,499	Ebus	2/15/97	18:13
1	4 STANDARD 3	Γc	259.94	150400	10.11	Flan	2.15.97	18.13
1	4 STANDARD 3	Mg	279.079	405900	400.5	Ebur	215.07	12:14:
2	4 STANDARD 3	Ca	317.917	3787000	499.7	[:pm	2/15/97	12-14
2	5 STANDARD 4	AJ	396.152	4783000	501.7	rpn	215.97	18:16:
2	5 STANDARD 4	Fe	255.94	3003000	199.8	[pn	2:15:97	15:16:
	6 STANDARD 5	As	193.696	13520	50	rpai	2/15/97	15:18:
5	7 ICV	As	193.696	301.6	1 131	րրու	2/16/97	13:20
1	7 KW	AL	396.152	231000	20.01	Idxn	2/16/97	13:2.
1	7 KW	Mr	237.61	114500	1 581	ррен	2/16/97	18:2
1	/IKV	Fe	259.94	150200	9.503	interna international internat	2/16.97	13:22
1	7 ICV	Ma	279.079	410500	514.4	רחיקנן	1/10/97	18:22
1	7 KW	Ca	317.903	3830000	512	1990	2/16/97	18.25
1	1 108	As	195.696	18 41	B.D.L.		2/16/97	18.2
	1 109	Al	396.152	10340	B.D.I.		2/16:37	18.25
	1 10.15	Mn	217.61		the second se	[9]sur		15.74.
	the second se	F2	219.94	857.6	E.D.L.		2/16/07	
1	1 ICB		279.079		B.D.L.	ppm	2/16/97	18:20;
	1 108	Mg	317.923	663.2	B.D.L.	ppan	2/16/97	18:26
1	1 109	La Ar	193.696	2525	F.D.L.	ppan	2/16/97	18:20;
1	8 CRII	As		23.62	F.DL.	מויק	216.97	\$:22:
1	8 CRII	Al .	396.152	10370	E.D1.	լթու	\$16.97	8.25
1	8 CR11	Mn	257.01	3721	(1,03548	med	2/16/97	5:10
1	8 CRII	Fe	259.94	:372	1º.D1	ib om	116.27	\$50
1	8 CRII	Mg	270,479	649.1	F.D.1.	lasur	2/16/97	\$ 161.
1	8 CRH	Ca	3 7,0331	2763	E.D.1.	рэн	246.97	_ 8 G;
1	51CSA1	As	193 656	69.15	0 1943	pont	14.97	8:2:
1	SICSAL	Al	396.152	476(00)	500.5		3.16.95	873
1	5 ICSAI	Ma	257 61	1590	0.009247		2.16.95	18:33.
1	5 ICSAI	Fe	259 94	3036000	202,3	1000	2/16:97	18:14:
1	5 ICSAI	∨g	279.079	433600	537.3	ppen	2 16 95	18:14:
1	5 ICSA1	Ca	317.933	3905000	521.5	pra	2/16/97	18:74
1	9 ICSAB1	As	193.696	103.6	0.3332	рга	2/ 6/97	18.360
1	9 ICSAB1	AJ	396, 152	4752000	498.7	opra	2 6.97	18.371
1	9 IC3AB1	Man	257.61	38290	0,4766	opra	2: 6/97	18:37:
1	9 ICSADI	Fe	259.94	3121030	208.2	labis	2 6.97	18.77
1	9 ICSAB1	Mg	279.079	4:2330	549	ppm	21.6497	18: 18:
1	9 ICSAB1	Ca	117 533	3025000	\$25.2	ppin	2/16/97	18:38:3
1	43 Method Blank	43	193.696	17.72	BD1.	Tabut	2: 6.97	18:40
1	43 Method Blank	AI	396.152	11380	0.08594	npin	2 6 97	18.41:0

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1	43 Mothod Blank	Mn	257.61	\$51.9		11.D.L.	ppm	2/16/27	18:13
1	43 Method Blank	Fe	259.94	1601		6,02657	ppna	2/16/07	18:41
1	43 Method Blank	Mg	279.070	713		B.D.L.	נחיים	2/16/07	18:42
1	43 Method Blank	ICa	317.933	2815		B.D.L.	ppm	2/16/07	8.17
1	44 Method Blank 1	As	193 696	16.87	_	R.D.L.	ppm	2/16/07	\$ 11
1	44 Method Blask 1	Al	396. 32	10980		6.04957	[ppns	2/16/97	8-44
1	44 Methne Blank 1	Min	257.61	841.9		B.D.I.	[ppn]	2/16/97	8:45
1	44 Methoc Blank 1	Fe	259.94	1373	101	B.D.L.	incici	2/16/97	8.+5
1	44 Methoc Blank 1	Mg	275.079	669	9.000	B.D.L.	ilabur	2/16/97	86
1	44 Methoc Blank 1	Ca	3 7.933	2529		B.D.L.	1915B1	2/16/97	8:-6
1	10 LCS (CCV)	As	193.696	154		0.5364	ppm	2/16/97	8:-3
1	10 LCS (CCV)	AJ	396.152	123000		10.13	ppan	2/16/97	18:->
1	10 LCS (CCV)	Vin	257.61	57910		0.7414	poan	2/16/971	18:-4
1	10 LCS (CCV)	Fe	259.94	31170		5.106	poin	2/16/97	18:-9
i	10 LCS (CCV)	Mg	275.079	210500		249.1	pan	2/16/97	18:49
1	10 LCS (CCV)	Ci	3:7.933	1956000		244.1	12283	2/16/97	18:50
1	1 365nm H2O2 .25 5K	15	193.696	11.49		E.D.L.	10.000	2/16/95	18.5
1	1 365nm H2O2 .25 5K	AJ	396.152	10810		0.03418	ancol (1997)	2/16/97	18:12
1	1 365nm H2O2 .25 5K	Mn	257.61	5111		0.05264	40.01	2/16/97	18.5
1	1 365nm H202.23 3K	70	259.54	4114		0 1858	ant of	2/10/97	18:2.
1	1 365nm H2O2 .25 3K	Mg	279.079	755.4		E.D.L.		2/10/97	18.2.
1	and a second	Ca		3380		the second se	10.201	the second s	18.2
1	1.365nm H2O2.25.5K		317.933			E.D.L.	in sm	2/16/97	18:23
1	2 365nm H2O2.22 5K D	A.:		10.83		E.D.L	pom	2/16/95	18.2
1	2 365am H202.21 5K D	A	396.152	10783		0.13182	ppm	2/16.97	-
1	2 365nm H2:02 .25 5K D	Ma	257 61	5087		0.05235	- baor	2/16/97	18.50
1	2 365nm H2:02 .25 5K D	Fe	259 94	4085		0.185		2/ 6.97	18.5
1	2 365m a H2D2 .25 5K D	Mg	279.079	735.5		H.D.L.	(dao)	2 6.97	18:5
1	2 365m (112:02.25 5K D	Ca	317.533	3285		11.D.L.	Tubua	2 (197)	121; 51
1	3 365nm H2D2 .25 5E S	As	193.696	5.927		B.D.L.	abe,	2 6.07	18:50
1	3 365nm H2O2 .25 5K S	A	396.152	11330		0.08129	inter	2/ 6/97	10:01
1	3 365 nrs H2(02,25 5K 5	kān	257.GL	6964		0.0756	inter a la contra contr	2 6.97	10-01
1	3 365nrs H2O2 .25 5K S	Fe	259.94	486	_	0.2743	1.100	2/ 6/97	10.01
1	3 365nm H2O2.25 SK S	Mg	279.079	734.1	_	B.D.1	201	2/ 6/97	19 (1)
1	3 365nm HDO2 .25 5K S	Ca	317.533	3256		RD1.	inde l	2/:6/97	19:01
1	4 365am H2O2 .25 5K L	As	193.696	21.61	4X	RDL.	inge	2/16/97	19:03
1	4 365 nm H2O2.25 5K L	M	396.152	(280	4X	BDL	pm	2/16/97	1911
1	4 365nm H2O2.25 5K L	Min	257.61	1890	4.5	0 01 294	0.05174 ppm	2/16/97	1916
1	4 365nm H2O2.25 5K L	Fe	259.94	1890	4.5	0.04502	0.1801 ppm	2/16/97	19 05
1	4 365am H2O2.25 5K L	Mg	279.079	658.2	4N	B.D.L.	ppm	2'16'97	19 05
1	4 365am 11202.25 5K 1.	Ca	317.933	2630	4N	H.D.L.	ppm	2/16/97	19 05
1	1) CCV1	As	\$3.696	156.3		1.5458	ppm	2/16/97	19.07
1	1) CCV1	Al	396.152	122200		6.11	ppm	2/16/97	19.08
1	10 CCV1	Min	257.61	:8740).7529	ppro	2/16/57	19.68
1	10 CCV1	Fe	259.94	81310		5.115	րրո	2.16/57	19.05
1	1D CCV1	Mg	279.079	210100		248.2	ppm	2'16'57	19.05
1	1) CCV1	Ca	317 933	19660030		244.6	ppin	2/16/97	19.06
1	1 CCB1	N	193 696	12.87		B.D.L	ippina i	2'16'57	19.11
1	1 CCB1	AI	396 152	10120	-	B.D.L		2'16'97	19:12
	1 CCB1	Ma	257.01	\$41.6	_	BUL	Pin	2'10'57	19:12
1	10081	Fe	239.94	1123		B.D.L	plus	2 10 97	19:12
1	the book of the second s	Mg	279 079	626.2		BDL	ppm -	2 10 97	19:12
the second se	1 CCB1	Ca	317 933	2255		the second s	p(m)	2.10.97	12:13
1	1 ICCB1 5 365am (1202.25ml, 02		193 695	1229	-	B D.L. 834	ppm.	2:16:97	19:15
1			The second second second second			the second se	. 6Lui	2/16/97	12,15
1	5 365mm (1202, 25ml, 02		296 152	2810000		274		42. 1000002.004	
1	5 365am 11202.25ml. 02		279 079	358100		-89.7	htan	2.16.97	12:17 12:18
1	5 365am (1202.25ml, 02		317 933		1.10.17	-6/2,1	[]Fith	And the second s	
1	5 365am H2O2.25nd. O2	and the second sec	250.01	38400	100X	k.767	876-7 ppm	2 16:07	10-22
1	5 365am H2O2 .25mL O2		257.61	123 80	\$68X	0.5308	265 Appro-	2 16 07	11.25
1	6 254am T O2 2g/1 O2	As	193 695	-113.4		3 D	Harry	2 16 97	10.27
1	5 254am T O2 2g/1 O2	Al	396 152	2746000		267.2		2 16 97	19.24
1	5 25km T (17 7g/11)7	Mg	279.079	399400		4913		2 16 927	12.29
1	6 254nm T:O2 2p/102	Ca	317.933	3459000		454.3	ppn	2.16.97	12.30
	6 254nm T:O2 2g/102	Fe	259.94	179700	100X	11.41	1 41 ppn	2 16-97	12:34
1	5 254nm TiO2 29/102	Ma	257.51	42810	500X	0.5366	268.3 ppn	2 16 97	19:37
1	V BUT THEN Y	1.8.4	193.696	-617.2		3.E.L.	Linn	2/16/97	10:30
	7 254nm TiO2 .2g/ O2	As	122.0201	and the second se				2.17.07	19:40
1	and a second statement and a second statement of the second statement of the second statement of the	A	396.152	2698000	1. 2	262 1	L'ant.	2:16.97	
1	7 254nm TiO2 .2g/ O2					262 1	1400. Litali,	246.97	19:41
1	7 254nm TiO2 .2g/ O2 7 254nm TiO2 .2g/ O2	Al	396.152	2698000			ldur 1441 Ltak	 Construction and 	

11	7 254nm TiO2 28/1 07	Min	257.61	42690 59CX	0.5549	207.4 jppm	2'16-97	19.49.22
1	& CRIZ	As	193.696	26 92	B.D.L.	jppm.	2'16-97	19 51 19
1	8 CR12	A	396.152	132,30	[3.D.L.	pper	2'16/97	19:52:0
-	& CRIZ	Ma	257.61	4236	0.04154	blan.	2'16.97	19:52 2
i	21571 8	Fe	259.94	1911	0.64637	ppm.	2,16.97	19:52 4:
1	8 CR12	Mg	275.079	608.3	B.D.L.	ppm.	2'16/97	19:53:07
1	8 CR12	Ca	3 7.935	24 18	B.D.L.	hear	2'16-97	19:53-20
1	5 CSA2	AJ	193.696	76.55	B.D.L.	ppm.	2.16/97	19:55 12
il	1 CSA2	Al	396.152	4.395000	424.6	թյու	2:16:27	19:55 55
1	5 C3A2	Mn	257 61	1001	011118	pp0	2:16:97	19:56:18
1	5 CSA2	re	259.94	2867000	150.5	ppa	2.16.97	16:56:11
	3 1CSA2	Mg	275.079	410900	516.8	ppn.	2/16/97	19:57:01
1	SUCSA2	Ci	3 . 1.935	3098000	450.1	ppo	2/16:07	(C: 57: P
1	9 ICSAB2	A	193.696	-7.638	HDL.	ppm	2(16.97	5:29:00
1	9 ICSAB2	AI	396.152	4456000	461.9	ppm	2/16.07	S. 598-48
1	9 ICSAB2	Mn	257 61	36570	0.4538.	nje	2:10:97	26.10:12
1	9/ICSAB2	re	219.94	2890000	192.2	spin	2.16.07	2010.33
	9 ICSAB2	Mg	270 070	409600	505.1	opm	2/16/97	201005
1	9 ICSAB2	Ci	317.933	3064000	485	121510	2/16.97	20.11.12
	51 Method Blank 8	As	192.696	3.82	F.D.	inite i	2/16.97	20.20(1)
	51 Method Blank 8	AI	396.152	9766	P.D.L.	apan	2'16.97	20:27:0
	51 Method Blank 8	Mn	217.61	\$98.8	E.D	37.03	210 97	20:27:2
	31 Method Blank 8	F¢	219.94	1052	1.D	ingen	2 16 37	71 17 44
1	\$1 Method Blank \$	Mg	279 079	190.2	E.D.S.	ותיור	2/16:97	21 (28/0)
	51 Method Blank 8	Ca	317.933	2058	E.D	in the second	2/16/97	21:38:25
	10 CCV2	As	193.696	34.9	0.4596	in je	2/16/97	20.50.10
	10 CCV2	AI	396.152	115100	9.165	altan	2:16:97	20:00:57
	10 CCV2	Mn	257.61	563 10	0.7194	aban	2:16:97	20.31.10
	10 CCV2	Fe	259.54	78340	4.925	орти	2:16/97	20.31.3
	10 CCV2	Mg	279.079	201400	237.3	ap n i	2/16/97	20.54:51
	10 CCV2	Cu	317.933	1866000	232.3	pipate	2/16/97	20:32:13
-	1 CCB2	As	193.656	15.77	B.D.L	and a	2/16:97	20.34.0
-	1 CCB2	Al	396.152	9600	B.D.L.	ppre	2/16/97	20:54:40
-	I CCB2	Ma	257.61	832 7	B.D.L	(a)ria	2/16:97	20.35:10
+	and the second se	Fr	259.94	1105	I.D.L	ppm	2/16/97	20:35:37
1	1 CCB2 1 CCB2	Mg	279.059	582	E.D.L	ppm	2/16/97	20.05:5
1	1 CCB2	Ca	317,033	2192	B.D.L	ppm	2/16/97	20:56:1

Section 7.4.			Site and state		Section 8.5.2	5.2			
Analyze call	Analyze calibration standard (ICV)	-			Matrix spikes	kcs			
Acceptable Critcria	Critcria	10%			Recovery	75% - 125%		%eR = 100 * (S-U)/C	:-uyc
	measured conc.	true value		%		Unspike (U)	Shike (S)	Actual con-	Dec
As	0.9399	1.004	mad	-6.38	As	10U	I L B L I	THIN THINK	N VI
M	19,44	20.055 ppm	mdd	-3.07	AI	0.02279	0.06703		
Mu	1 468		bpm	-2.33	Ma	0.04519	0.06585	F6100	106
Fe	9,401		bpm	-5.94	Fe	0.1688	0.2594		165
Mg	500.1	500.828	mqq	-0.15	Mg	B.D.L	BDL.		
Ca	496.3	500.002	шф	-0.74	Ca	B.D.L.	B.D.L.		
Section 8.3.					Castion 0.4				
Method blank	ık				Analytical	Analytical dunicates			
Accentable Criteria	Criteria	MIN			unit unit	1			
Annulana	CHICKING	Y M			KFU	<= 20%		RPD - 100 * ((C1-C2)/[(C1+C2)/2]
	measured conc.	CRD1.				CI	0	RPD %	
As	B.D.L.	10'0	ppm		As	RDI	RDI		
AI	B.D.L.		ppm		IV	0 02275	0.02032		
Mn	B.D.L.	0	bpm		Mn	0.04519	0.04492	0.60	
Fc	D.D.L.		ppm		Fe	0.1688	0.1701	22.0-	
Mg	B.D.L.		ppm		Me	BDL	RDI	1.10	
Ca	B.D.L.		ррт		Ca	B.D.L.	B.D.L.		
Section 8.6.1.1.	1.1.								
Check standard	ard				Colibration	Colibration March (COD)			
Acceptable Criteria	Criteria	10%			Accentable Criteria	· Criteria			
	measured conc.	true value		0%		measured conc.	CRDL		
As	0.4718		ppm	-6.02	As	BDL	0.01 000		
AI	9.874	10.03 ppm	bpm	-1.54	AI	8DL	0 20 mm	num	
Mn	0.6942		bpm	-7.69	Ma	B.D.L.	0.015 0000	unu -	
Fe	4.769	5.00	ppm	4.58	Fe	BDL	0.10 00m	mud	
Mg	235.6		ppm	-5.91	Mg	B.D.L.	5.00	000	
Ca	233.8		ppm	-6.48	Ca	B.D.L.	5.00 ppm	ppm	

QC Procedures

	ted from Vanan LIBERTY								-
cesul: File	TAIQAQC306					-		-	
Aatch Sample	and the second se					-	1		
Aatch Sample	the second s						1	The second	
Antch Eleme									
ate and Time	and the second se	_						1	
Leport Mode		-					11		
epon Mode	- ALL DATA, Date and Time - 1	VES						10.000	
	Fuhe# Samp.Lab.	EJ	W/	Intens	Conc	Dilute Con	Units	Date	Time
1	I BLANK	As	193.696		0		ppm	3/6/97	19:59
1	I BLANK	Al	396.152	and the second sec	0		ppen	3/6/97	20:00
1	1 BLANK	Mb	257.61	1223	0		ppm	3/6/97	20:00
1	1 BLANK	Fe	259.94		0	Concession and an a strength of the strength o	ppm	3/6/97	20:00
1	1 BLANK	Ma	279.079		0		ppm	50/97	20:01
1	1 BLANK	Ca	317.933	2867	0		opm.	3/6/97	20-01
1	2 STANDARD 1	As	193.696	the second se	0.1		ppm	3/6/97	20:03
1	2 STANDARD 1	AI	396.152	5	2		ppm	3/6/97	20:03
1	2 STANDARD I	Mn	257.61	16080	0.15		ppca.	3/6/97	20:04
1	2 STANDARD 1	Fe	259.94		1.011		ppm	3/6/97	20:04
	2 STANDARD 1	Mg	279.079		49.95	1.1.1.1.1.1.1.1	ppm	3/6/97	20:05
1	2 STANDARD 1	Ca	317.933		49.97		ppm	3/6/97	20:05
	3 STANDALD 2	Aa	193,696		05		rem	3/6/97	20.07
1		Al	396.152	a second and a second as a	5.999		ppm	3/6/97	20:07
1	3 STANDARD 2	Ma	257.61	73460	0 7495		ppm	3/6/97	20:03
1	3 STANDARD 2	and the second second second	257.01		3.05		and the second se	36/97	20:08
1	3 STANDARD 2	Fe	and the second se		249.8		ppm	3/6/97	20:08
1	3 STANDARD 2	Mg	279.079	3258300	2498		ppm	3/6/97	20:09
1	3 STANDARD 2	Ca	317.933	2/5.4	2499	-	ppm	3/6/97	20:09
1	4 STANDARD 3	As	and the second se				ppm	3/6/97	20:10
1	4 STANDARD 3	LA I	306.152	125400	20		ppm	3/6/97	20:11
1	4 STANDARD 3	Min	257.61	:35200	1.499		ppm	3/6/97	20:12
1	4 STANDARD 3	Fe	2:9.94	77300	10.11		ppm	3/6/97	20.12
1	4 STANDARD 3	Mg	279.079	\$14300	499.5		Phun -	and the second sec	and the second se
1	4 STANDARD 3	Ca	317.933	5930000	499.7		ppm	3/6/97	20:13
1	5 STANDARD 4	AJ	396.152	6439000	501.7		ppm	3/6/97	20:14
1	5 STANDARD 4	Fe	259.94	3585000	199.8		ppm	3/6/97	20.15
1	6 STANDARD 5	Aa	193.695	the second s	50		ppm	3//5/97	20.17
1	7 ICV	As	193.695		0.9399		ppm	3/6/97	20:19
1	7 KV	AI	396.152	341300	19.44		ppm	3/6/97	20:23
1	7 10 1	Mn	257.61	133200	1.468		ppm	3/6/97	20:20
1	7 10	Fe	219.94	76100	5,401	0	ppm	3/6/97	20:21
1	7 ICV	Mg	279.079	515300	500.1		ppm	3/6/97	20:21
i	7 ICV	Ca	317.933	5900000	49/6.3		ppm	3/6/97	20.21
1	1 ICB	مد	193.696	11.42	B.D.L.		ppm	3/6/97	20:23
1	1 108	A	396.152	15040	B.D.L.		ppen	3/6/97	20:24
1	1 1/CB	Min	257.61	1222	B.D.L.	1 1	ppm	3/6/97	20:24
1	1 1/08	Fe	2:9.94	1423	D.D.L.		ppm	3/6/97	20:25
1	1 1/08	Mg	279.077	879.4	B.D.L.	1.	ppen	3/6/97	20:25
	1)/CB	Ca	317.933	3146	B.D.L.	1	ppm	3'6/97	20:25
1	8 (CR)1	As	193.695	18.69	B.D.L.		pren	3.6/57	20.27
	8 CR11	AI	396.152	15100	B.D.L.		ppm	3'6/97	20:23
1	8 CR11	Mn	257.61	4690	3.03494		ppm	3'6/97	20:23
1		Fe	2:9.94		0.01535		ppm	3'6/97	20:29
1	8 CR11		279.079		B.D.L.		ppm	3'6/57	20.29
1	8 CKJI	Mg	317.933	3407	B.D.L.		ppm	3'6/97	20.29
1	R CRJI	Сл		147.1	0.4404	S	1.	3'6/97	20.31
1	5 ICSA1	As	193.695		503.7	the second se	ppm	3'6/57	20.32
1	51)CSA1	AJ	217.61	2082	0.001654		ppm	3'6/97	20:32
1	5 XCSA1	Mn		and the second se	194.2		prm	3'6/97	20:33
1	5 ICSA1	Fe	259.94		533.4		prm	3'6/57	21:55
1	5 ICSA1	Mg	275.079	6:10000	519.8		prm	3/6/57	20:34
1	5 ICSA1	Ca	and the second se		B.D.L		PEm	3/6/57	20:35
1	9 CSABI	As	193.696		the second s		btu	3'6/57	20:36
1	9 ICSABI	Al	396.152	and the second se	523.7		ppm	3/6/57	20.37
1	9 ICSABI	Mn	257.61	A CONTRACTOR OF A CONTRACTOR OFTA CONT	0.4792		bbu	and the second sec	20:37
1	9 ICSABI	Fe	259 94	A REAL PROPERTY AND	200	5 F	<u>b</u> Lm	3/6/57	20:31
1	9 ICSABI	Mg	275.079	and the second se	546.4		ppm	3/6/57	20:34
1	9 ICSABI	Ca	317.933	the second s	559.1		ppm	3/6/57	
1	43 Method Blank	As	192.696	and the second se	B.D.L.		ppm	3/6/57	73 41
1	43 Method Blank	Al	396.152		B.D.1		ppm	3.6/57	23 44
1	43 Method Blank	Ma	217.61	1 42	B.D.1.	1000	ppm	3/6/97	23 44
1	43 Method Blank	Fe	239.94	1336	B.D.L.		blau	3/6/97	23 45
1	43 Method Blank	Mg	275.079	875.6	BDI		ppm	3.6/97	23:45
1	43 Method Blank	Ca	317.933	3658	B.D.L.		ppm	3/6/97	23.45
1	44 Method Blank 1	As	193.696	CONTRACTOR OF THE OWNER WATER OF THE OWNER OF	B.D.L.		ppm	3/6/97	2J:43

1	44 Method Blaak 1	Al	396.152	15350		B.D.L.		ppm	3/0/91	20,48
1	-44 Method Blaak 1	tin	257.61	1124		B.D.L.		ppm	7/6/97	20:48
1	44 Method Blaak 1	Fe	255.94	1296		B.D.L.		ppm	3/6/97	20:49
1	44 Method Blank 1	Mg	279.079	859.5		B.D.L.		ppm	3/6/91	20:49
11	44 Method Blaak 1	Ca	317.933	3846		B.D.L.		ppm	3/6/97	20 49
1	10 LCS (CCV)	As	193.696	162.4	_	0.4913		ppm	3/6/97	20.51
11	10 LCS (CCV)	Al	396.152	173500		9.366		ppm	3/6/97	20:52
1	10 LCS (CCV)	Mn	257.61	00000	_	0.6/57		ppm	3/6/97	20:52
1	10 LCS (CCV)	Fe	250.94	\$9070		4.712		bbu	3/6/07	21-53
1	10/LCS (CCV)	Mg	279.079	249700	_	230.6	_	ppm	3/6/97	20:53
1	10 LCS (CCV)	Ca	317.933	2968000		226.3 D.D.L.		ppm	3/6/97	20.55
1	1 No-UV H2C2 C2 SK	As	193.696	19.93		0.02279	-	ppra	3/6/97	20:56
1	1 No.17V H2C2 02 5K	Al Mn	326.152	5737		0.04519		ppm	3/6/97	20:56
1	1 No-UV H2C2 02 5K	Fe	259.94	4509		0.1688		ppes	3/6/97	20:51
1	1 No-UV H2C2 02 5K	Mg	279.079	956		BDL		ppes mpes	3/6/97	20:57
1	1 No-UV H2C2 02 5K	Ca	317.933	4429	_	B.D.L.		ppm	3/6/97	20:57
1	2 No-UV H2C2 02 5K D	As	173.696	16.43		B.D.L.		ppm	3/6/97	20:55
1	2 No-UV H2C2 02 SK D	Al	396. 52	5950		0.02032		labera .	3/6/97	21:00
il	2 No-UV H2C2 02 5K D	Mn	257.61	5630		0.04492		ppen	3/6/97	21:00
1	2 No-UV H2C2 O2 5K D	Fe	259.94	4595	-	3.1701		ppes	3/6/97	21:00
i	2 No-UV H2C2 02 1K D	Mg	279.079	936.8	0.000	B.D.L.		ppm	3/6/97	21.01
1	2 No UV H2C2 02 SK D	Cn	317 933	4328		B.D.L.		ppm	3/6/97	21:01
1	3 No-UV H2C2 O2 5K S	As	193.696	8.252		B.D.L.		ppm	3/6/97	21:03
i	3 No-UV H2C2 O2 5K 5	Al	396.152	6740		0.06703		ppm	3/6/97	21.03
1	3 No-UV H2C2 02 5K 8	Ma	257.61	7754		0.06585		ppm	3/6/97	21:04
1	3 No-UV H2C2 02 5K S	Te	259.94	6257		3.2594		ppm	3/6/97	21:04
1	3 No-UV H2C2 02 5K S	Mg	279.079	950.4	_	3.D.L.		ppm	3/6/97	21:05
1	3 No-UV H2C2 O2 5K 5	Ca	317.933	4581		B.D.L		ppm	3/6/97	21 0:
1	4 No UV H2C2 02 SK L	As	193 696	12 33	4X	B.D.L.		ppm	3/6/97	21:07
13	4 No-UV H2C2 02 SK L	AI	396. 52	15230	4X	3.D.L.	0.04145	ppm	3/6/97	21:07
1	4 No-UV H2C2 02 5K L	Mn	257.61	2252	4X 4X	001036	0.04145	production and the second s	3/6/97	21.08
1	4 No-UV H2C2 02 4K L	Гс	259.94	2183	4X 4X	3.D.L.	0.1612	and a second	3/6/97	21:08
11	4 No-UV H2C2 02 5K L	Mg	279.079	3552	4X	3.DL		abu	3/6/97	21:05
1	4 No-UV H2C2 O2 5K L	Ca	193.696	166.2	40	0.5943		ndd abw	3/6/97	21.11
1	10 CCV1 10 CCV1	AL	396 152	182100	-	9177		nere	3/6/91	21:11
1	10/CCVI	Mn	257.61	68650		0.6972		opm	3/6/97	21:12
1	10/CCVI	Fe	259.94	92630		4.905		opm	3/6/97	21:12
1	10 CCV	Mg	279.079	262500		242.8		open	3/6/97	21:13
1	10 CCV1	Ca	317.933	3072000		234.8		open	3/6/97	21:13
1	1 CCB1	As	193.696	21.18		3.D.L.		opm	3/6/97	21:14
11	I CCB1	AI	396.152	14850	1	3.E.L.	0.011-01	pen	3/6/97	21.15
1	I CCB!	Min	25761	1182		B.E.L.		open	3/6/97	21:16
1	1 CCB!	Fe	259.94	13\$5		B.E.L.	1	open	3/6/97	21:16
il	1 CCB!	Mg	279.079	855.2		B.D.L.		ppn	3/6/97	21:10
1	1ICCB1	Ca	317.933	2930		3.D.L.		2pm	3/6/97	21:17
1	5 No-UV 30%H2O2 O2(19)	los	193.696	1237		4.088		ppn	3/6/97	21.18
1	5 No-UV 30%H2O2 O2(19)	AJ	396.152	3691000	Sec. 1	245.8		ppm	3/6/97	21.15
1	5 No-UV 30%H2O2 O2(19)	Mg.	279.079	477900		459.6		ppm	3/0/97	21.21
1	5 No UV 30%4H2O2 O2(19)	Ca	3 7 933	5114000	10.011	421.6		ppm	3/6/97	21.21
1	5 No-UV 30%H2O2 O2(19)		259.94	156100	100X	8.521	\$321		3/6/97	21.25
1	5 No-UV 30%(1202 D2(19)		25761	(0500	400X	0.6097	243.9	the second s	3/0/97	21 28
t	6 No-UV 02 (sample 18)	As	193.696	1658		5.503		up and a	3/6/97	21 31
1	6 No-UV O2 (sample 18)	AJ	396.152	37(6000		248		ppm	3/6/97	21 31
1	6 No-UV 02 (sample 18)	Mg	279.079	464200		445.1		ppm	3/6/97	21 33
1	6 No-UV 02 (sample 18)	Ca	3 7.933	3271000	100X	10.69	1069	ррев	3/6/97	21 37
1	6 No UV 02 (cample 18)	Fe Mn	25761	57390	400X	0.5766	230.6		3/6/97	21 40
1	6 No-UV 02 (sample 18)	As	193.696	1196	-NUA	3.952	250.0	ppm	3/6/97	21 42
1	7 No-UV 30%H2O2 (s 17) 7 No-UV 30%H2O2 (s 17)	AJ	396.152	3775000		253.4		ppm	3/6/97	21 43
1		Mg	279.079	470900		452.2		ppm	3/6/97	21 45
1	7 No-UV 30%(1202 (s 17)	Ca	3:7.533	5370000		44).1		ppm	3/6/97	21 46
1	the second se	Fe	259 94	149200	100X	7.551	795.1		3/6/97	21 49
1	7 No-UV 30%44202 (* 17)	Mn	25761	58630	400X	0.5897	235.9		3/6/97	21 52
1	8 CR12	As	193.696	16.19		B.D.L.		1pm	3/6/97	21 54
i	8 CR12	A	396.152	15090		B.L.L.		7pm	3/6/97	21.33
1	B CR12	Mn	25761	4465		0.03267		Shu.	3/6/97	21 56
1	8 CR12	Fe	259.94	1686		0.01391		ppm	3/6/97	21.56
i	8 CR12	Mg	279.079	8294		B.D.L.		ppm.	3/6/97	21:56
1	8 CK12	Ca	317.533	3470		B.D.L.		ppm.	3/6/97	21:57
1	5 ICSA2	As	193 696	1.91		B.D.L.		ppm	3/6/97	21:58
1	5 ICSA2	Al	396.152	16860		0.07413		pper:	3/6/97	21:59
		Mn	257.61	1184		BDL		PTMT:	3/0/97	21.59.

1	5 ICSA2	Fe	259.94	1342	BDL	ppen	3/6/97	22:00
1	5 ICSA2	Mg	279.079	230500	2123	ppen	3/6/97	22:00
1	5 ICSA2	Ca	317.933	6256000	536.2	ppes	3/6/97	22:00 :
1	9 ICSAB2	As	193.696	-1128	BD.L.	ppm	3/6/97	22.32)
1	9 ICSAB2	AI	396.152	6205000	4765	ppen	3/6/97	22.03.
1	9 ICSAB2	Mn	257.61	45190	0.4484	ppm	3/6/97	22.04
1	9 ICSAB2	Fe	259.94	3291000	183.3	ppcs	3/6/97	22:04
1	9 ICSAB2	Mg	279.079	529900	5161	ppm	3/6/97	22:04:
1	9 ICSAB2	Ca	317.933	6362000	5145	ppm	3/6/97	22:05
1	45 Method Blank 2	As	193.696	14.22	BD1	ppta	3/6/97	22:07:0
i	45 Method Blank 2	AI	396.152	15470	BD1.	ppm	3/6/97	22:37:
1	45 Method Blank 2	Min	257.6	1265	BD.L.	abury	3/6/97	22.38.
1	45 Method Blank 2	Fe	259.94	1447	B.D.L.	and a	3/6/97	22:38.
1	45 Method Blank 2	Mg	279.079	848.5	BD.L.	ippra.	3/6/97	22:38:
1	45 Method Blank 2	Ca	317931	3395	B.D.L.	ppm	3/6/97	22:39.
1	46 Method Blank 3	As	193,696	18.11	B.D.1.	ppra	3/6/97	22:10
1	46 Method Blank 3	Al	396.152	14850	B.D.L.	рртя	3/6/97	22:11
1	46 Method Blank 3	Min	257.6	1201	B.D.L.	ppm	3/6/97	22:12:
4	46 Method Blank 3	Fe	259.94	1302	B.D.L.	ppm	3/6/97	22.12:
	and the second se	Ng	279.079	822.5	B.D.L.	ppra	3/6/97	22:12:
1	46 Method Blank 3 46 Method Blank 3	Ca	317931	3082	B.D.L.	ppm	3/6/97	22:13:
1	and the second se		193.696	15.74	BD.L.		3/6/97	22:14:
1	47 Method Blank 4	As	396.152	14743	BD.L.	ppm	3/6/97	22:15:
1	47 Method Blank 4	Al		1190		ppm	3/6/97	22.15
1	47 Method Blank 4	Min	257.6		B.D.L.	ppm	3/6/97	22.16:
1	47 Method Blank 4	Fe	259.94	1301	B.D.L.	ppm	3/6/97	22:16:
1	47 Method Blank 4	Ng	279.079	816.4	B.D.L.	ppm		22:16:
1	47 Method Blank 4	Ci	317933	1025	B.D.L.	ррти	3/6/97	22:18:
1	48 Method Blank 5	As	193.696	15.91	B.D.L.	ppm	3/6/97	2219
1	48 Method Blank 5	AJ	396.152	14730	B.D.L.	ppm	3/6/97	
1	48 Method Blank 5	Min	257.61	1131	B.D.L.	ppm	3/6/97	12 19:
1	48 Method Blank 5	Fe	259.94	1309	B.D.L.	ppm	3/6/97	22 20:
1	48 Method Blank 5	Ng	279.079	823.4	B.D.L.	ppm	3/6/97	12:20:
1	48 Method Blank 5	Ci	317933	3207	B.D.L.	ppm	3/6/97	22:20:
1	49 Method Blank 6	As	193.696	1 502	B.D.L.	laben	3/6/97	22:22
1	49 Method Blank 6	A	396.152	1472)	B.D.L.	ppm	3/6/97	22:23
1	49 Method Blank 5	Mn	257.61	1141	B.D.L.	ppm	3/6/97	22.23
1	49 Method Blank 6	Fe	259.94	1273	B.D.L.	ppm	3/6/97	22:24
1	49 Method Blank 5	Ng	279.079	820.3	B.D.L.	ppm	3/6/97	22.24
1	49 Method Blank 6	Ca	317.933	2914	B.D.L.	ppm	3/6/97	22 24
1	50 Method Blank 7	As	193.696	13.11	B.D.L.	ppen	3/6/97	22:26
1	50 Method Blank 7	Al	396.152	1470)	B.D.L.	ppm	3'6/97	22:27
1	50 Method Blank 7	Mn	257.61	1152	B.D.L.	ppm	3/6/97	22:27
1	50 Method Blank 7	Fe	259.94	1259	B.D.L.	ppm	3/6/97	32:27
1	50 Method Blank 7	Mg	279.079	808.2	B.D.L.	ppm	3/6/97	22:28
1	50 Method Blank 7	Ca	317.933	3971	B.D.L.	ppm	3'6/97	22:28
1	51 Method Blank 3	As	193.696	12.32	B.D.L.	ppm	3/6/97	22:30
1	51 Method Blank 3	A	396.152	16530	B.D.L.	Taur	3/6/97	22:31:
1	51 Method Blank 3	Mn	257.61	1139	B.D.L.	ppm	3/6/97	22:31
1	5] Method Blank 3	Fe	259.94	1212	B.D.L	tom	3/6/97	22:31
and the second se	51 Method Blank 3	Mg	279.079	821.3	B.D.L.	tpm	3/6/97	22:32
1	51 Method Black 3	Ca	317.933	2981	B.D.L.	ppm.	3/6/97	22:32
1	state in the second state of the second state	As	193,596	156.5	0.4718	rpm.	3/6/97	12:34
1	10 CCV2	Al	396.152	182000	9.874	and the second	3/6/97	12:34
1	10 CCV2	Mn	257.61	68370	0.6942	tbu	3/6/97	12:35
1	10 CCV2	and relative	259.94	9(130)	4.769		3/6/97	22.35
1	10 CCV2	Fe	279.079		and the second s	Ebur	3/6/97	12:36
1	10 CCV2	Mg	and the second s	254900	235.6	Ebus	3/6/97	12:36
1	10 CCV2	Ci	317.933	3061000	233.8	Ebus.	3/6/97	22.30
1	1 CCB2	As	193.696	14.04	B.D.L.	Ebus	3/6/97	22.38
1	1 CCB2	Ai	396.152	14520	B.D.1.	Ebus	3/6/97	22.39
1	1 CCB2	Mn	257.61	1199	B.D.1.	Ebus		22:39
1	1 CCB2	Fe	259.94	1355	B.D.L.	Ebus	3/6/97	
1	1 CCB2	Mg	279.079	892.2	B.D.1.	Ebus	3/6/97	22:39:
	1 CCB2	Ca	317.933	2891	B.D.1.	(pn:	3/6/97	22:40:

Sheet1

Section 9.3					
Reagent B					
Acceptable	c Criteria	< 5 ppm			
	measured conc.		-		
sulfate		ppm			1000
Section 9.3	3.2.				
Lab Fortili			1		
Recovery	90% - 110%				- Anna
		% R = 100 *	(S-U)/C		
	Unspike (U)	Spike (S)	Actual cone.	R %	1 Annu I
sulfate	1905			97.225187	
			0.16		
Section 9.3					
	Performance Ches	and the second			
Acceptable	Criteria	10%			
	measured conc.	true value	12 2015	58	
sulfate	1066	1000	ppm	6.60	104
Section 9.3	.4.				
Calibration					
Acceptable		< 5 ppm			1000
1	measured conc.				1
sulfate	2.27	ppm			
Section 9.4	7			9.0	ALC: NO
Field Dupli					
RPD	<= 20%		RPD = 100 * ((C1-C2)/[(C1	+C2)/2]
	C1	C2	RPD %		
sulfate	6923	7348	5.96		

	Destantas Ditista		
	Berkeley Pitlake water		0/10
		sulfate (ppm)	%R
11	unspike conc. (U)	8624	91.3
	spike conc. (S)	9437	
	actual conc. (C)	1000	
	Sample 12 (UV 254n	m, Na-Formate)	
		sulfate (ppm)	%R
	unspike conc. (U)	8512	79.0
	spike conc. (S)	9308	
	actual conc. (C)	1000	
	Sample 13 (UV 254 r		
		sulfate (ppm)	%R
	unspike conc. (U)	7750	97.7
-3	spike conc. (S)	8727	
	actual conc. (C)	1000	
	Sample 14 (UV 254 n	T(02)	
	Sample IT (OV LOTI	suffate (ppm)	%B
	unspike conc. (U)	8110	106.9
	spike conc. (S)	9179	100.5
	actual conc. (C)	1000	
	Sample 15 (UV 254 n	m, TiO2 & Na-Format	
		sulfate (ppm)	%R
	unspike conc. (U)	8066	76.8
	spike conc. (S)	8823	
	actual conc. (C)	1000	
	Sample 16 (UV 254 n	m, TiO2 & Hydrazine)	
		sulfate (ppm)	%R
	unspike conc. (U)	69701	79.76331
	spike conc. (S)	7644	
	actual conc. (C)	845	
	Sample 20 (no-UV. N	a Eormate)	
	Jampie 20 (10-01.14	sulfate (ppm)	%R
	unspike conc. (U)	8113	81.89349
	spike conc. (S)	8805	01.00045
	actual conc. (C)	846	1
	actuar conc. (C)	0-10	-
	Sample 21 (no-UV, H	(drazine)	
		sulfate (ppm)	%R
1	unspike conc. (U)	6923	117.4746
	spike conc. (S)	7965	
	actual conc. (C)	887	